

Impact of Fluidized Bed Hydrodynamics on the Distribution of Liquid Sprayed into the Bed

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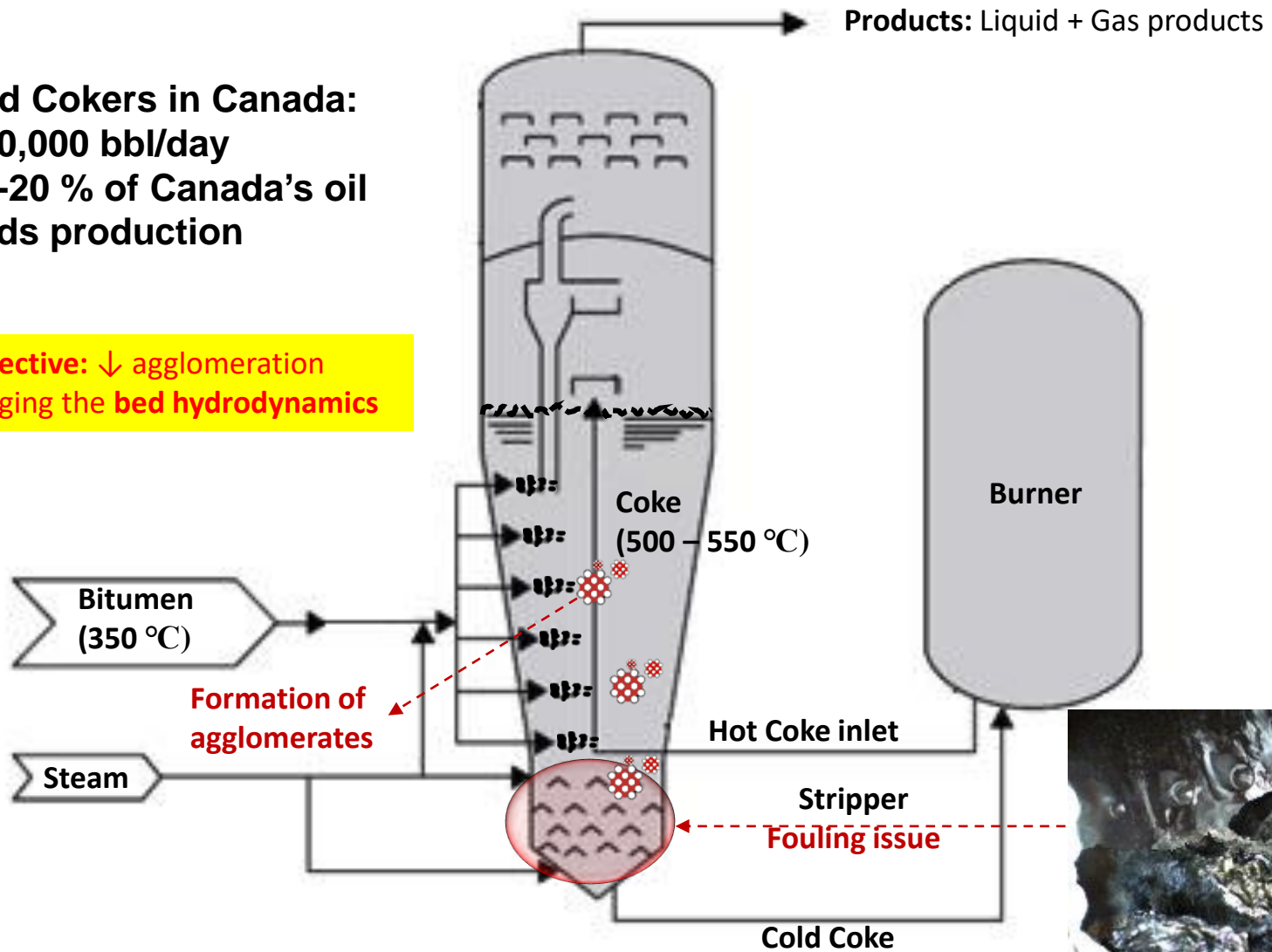
Introduction

Fluid Coking™ technology

Fluid Cokers in Canada:

- 400,000 bbl/day
- 15-20 % of Canada's oil sands production

Objective: ↓ agglomeration by changing the **bed hydrodynamics**



Objectives

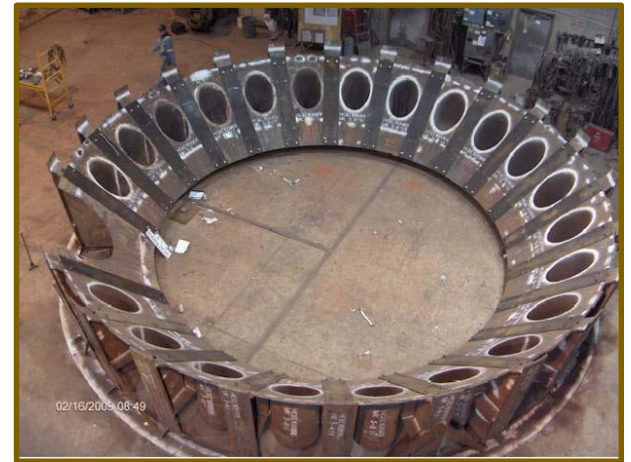
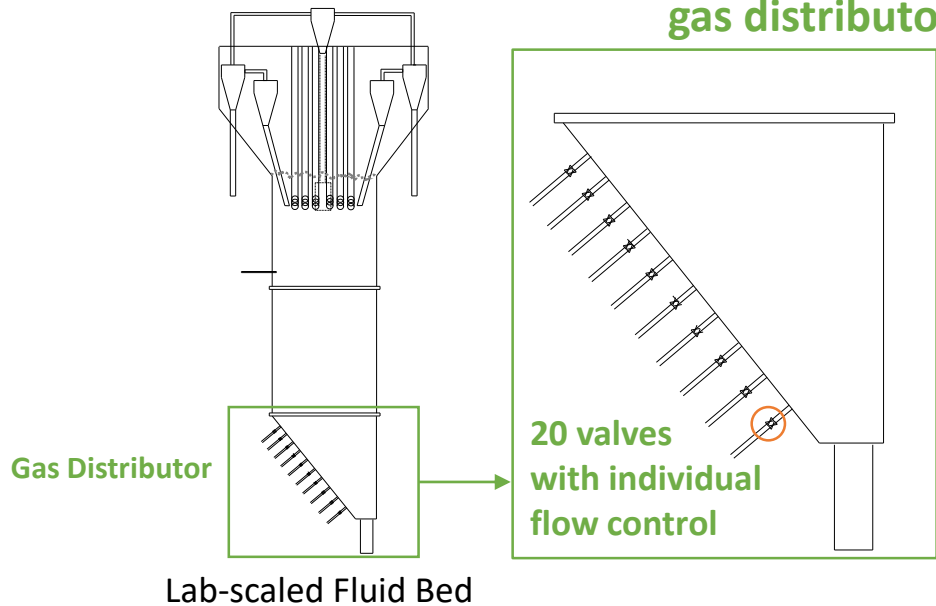
Bed Hydrodynamics

Increase superficial gas velocity

Modify gas distribution

By changing the
gas distributor

By using **internals**,
e.g. **baffle**

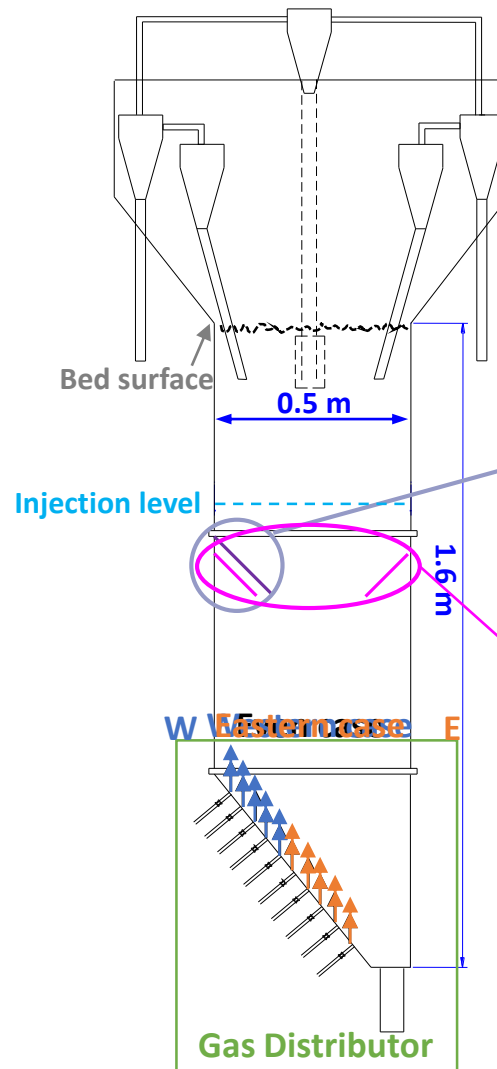


Picture from: ExxonMobil, 11th International BBTC Conference

Equipment & method

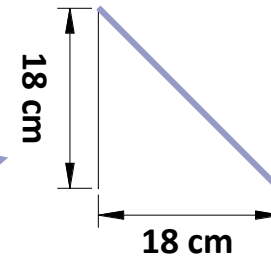
Approaches to modify gas bubble distribution

Approach 1:
Change the initial inlet gas distribution configuration

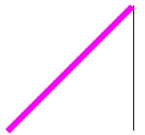
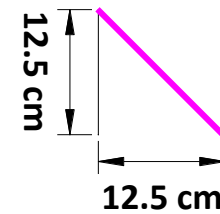


Approach 2: Baffle

a. Single baffle



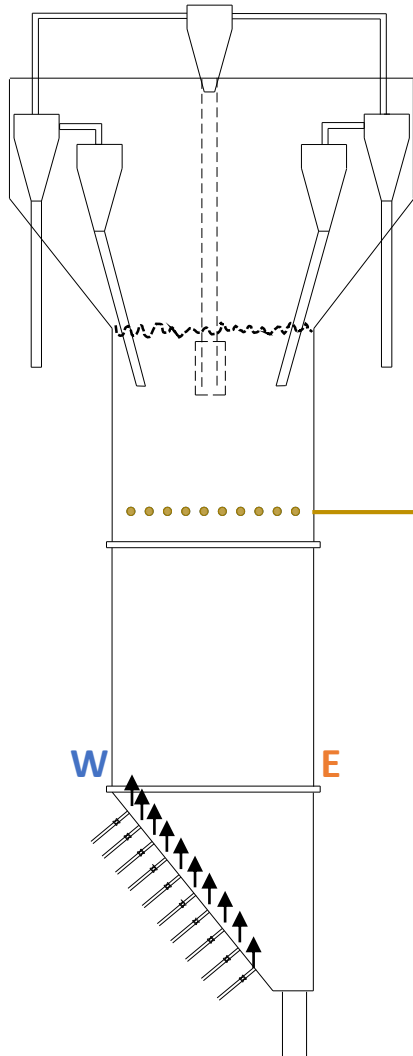
b. Symmetrical baffles



Lab-scaled Fluid Bed

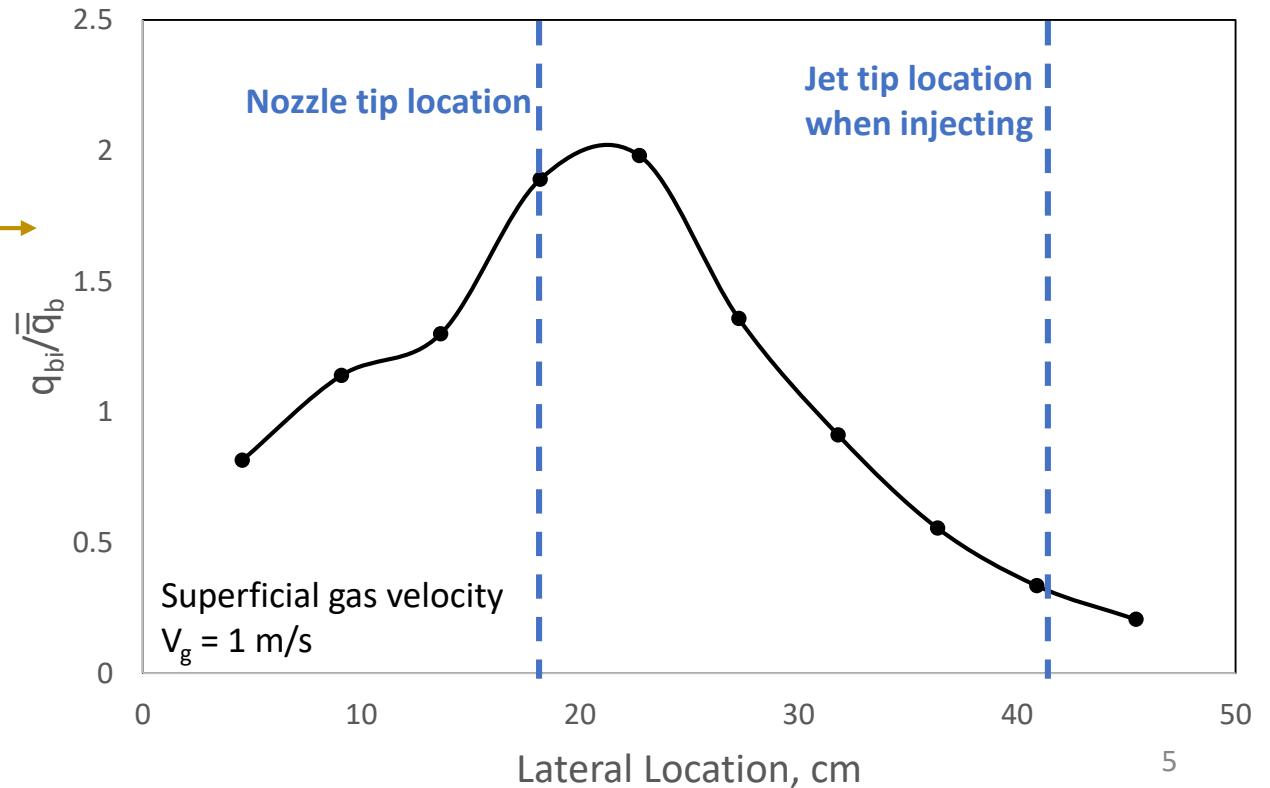
Equipment & tribo-probe method

Gas bubble distribution profile



$$\frac{\text{Local bubble volumetric flux}}{\text{cross - section average bubble flux}}$$

Typical profile example: even case before injection

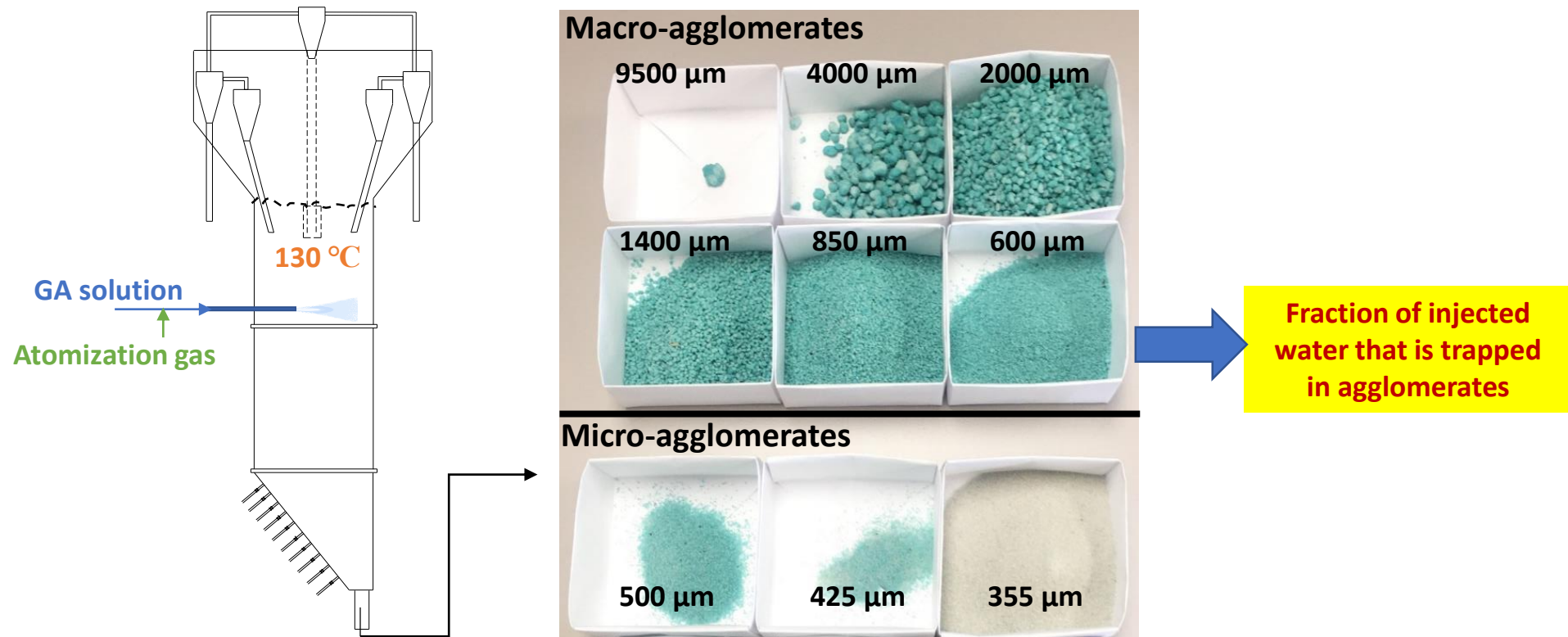


Equipment & Gum Arabic method

Simulate fluid coking agglomeration

Gum Arabic (GA) Solution: (200 g)

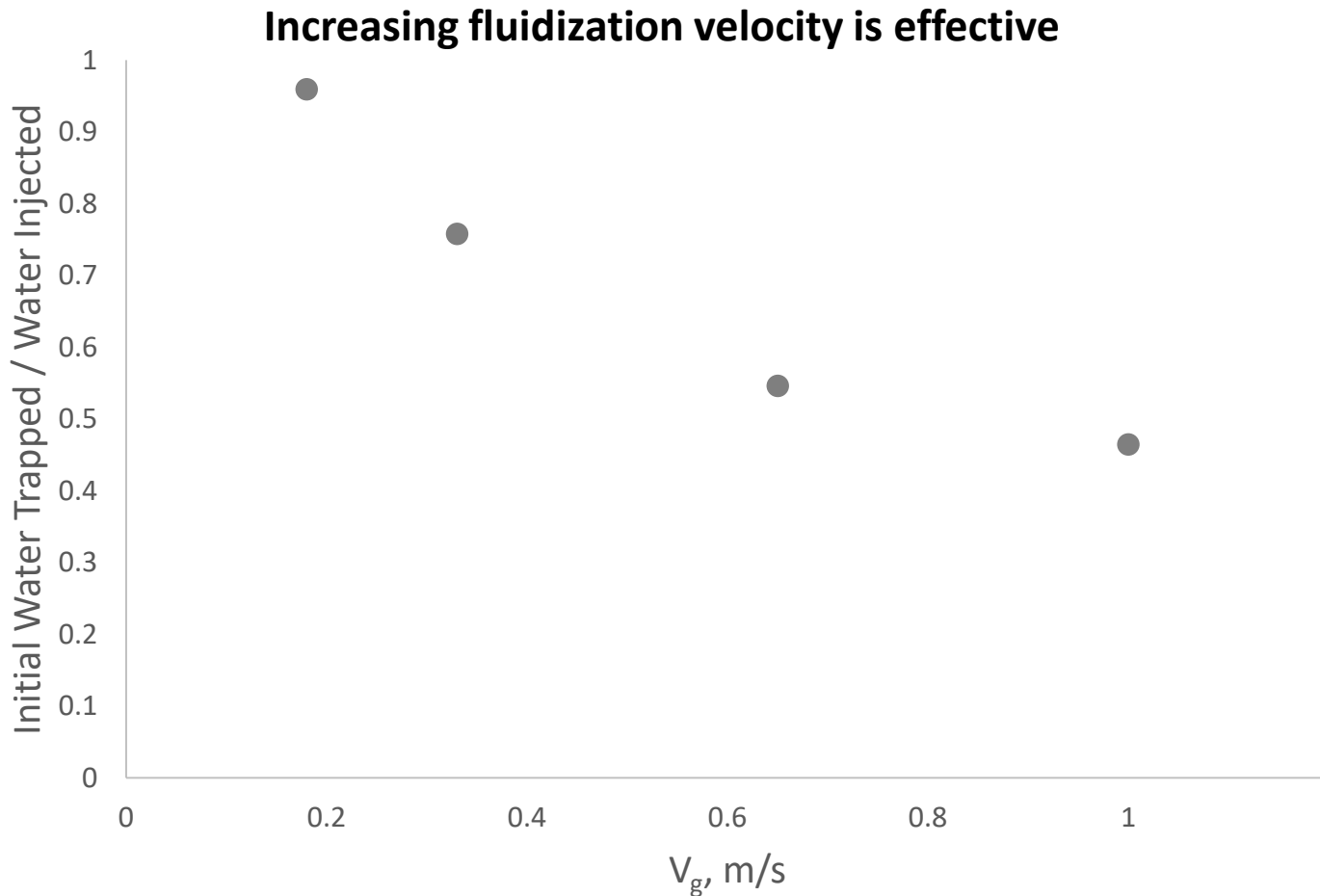
92 wt% water + 6 wt% gum Arabic + 2 wt% blue dye; pH: 3.0



Increase of V_g in the Coker

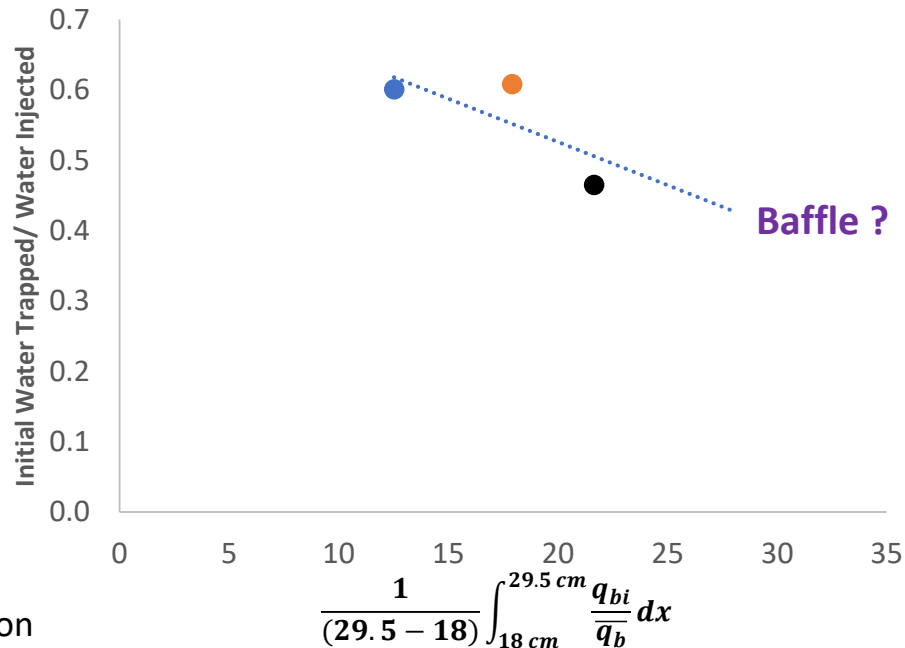
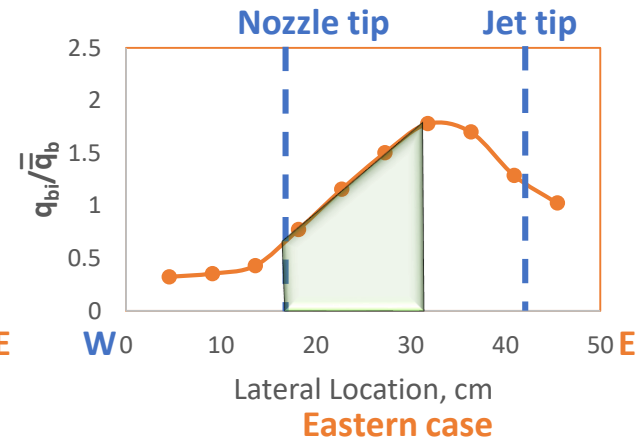
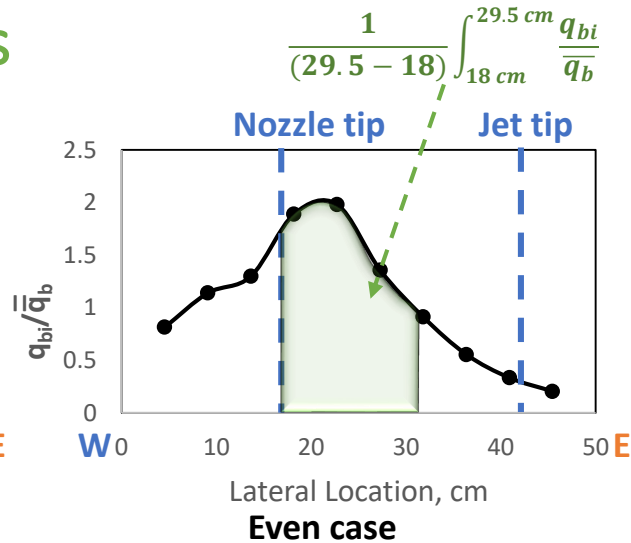
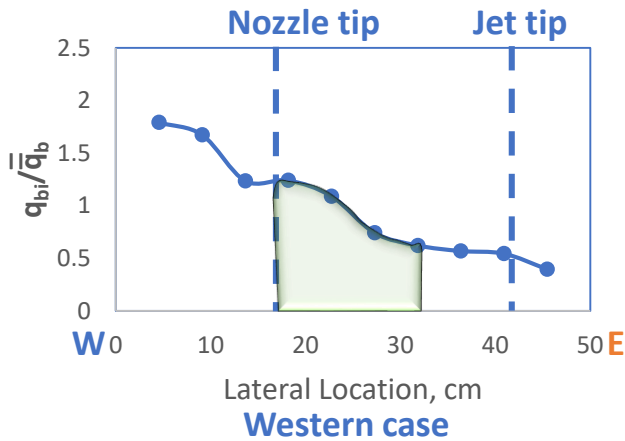
↓ agglomeration

Even Gas Distribution, No Baffle, Slumped after injection



Impact of gas distribution

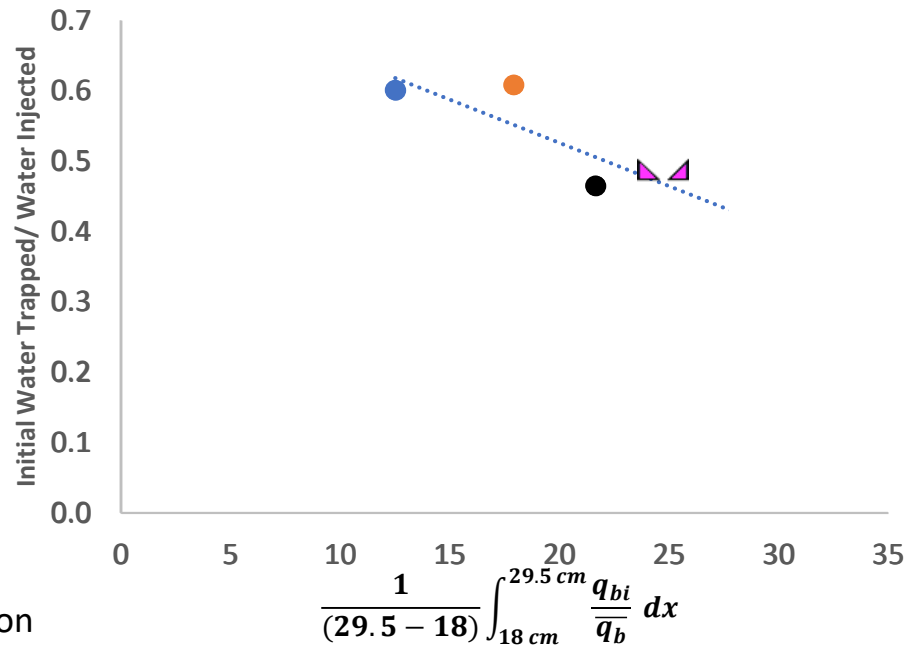
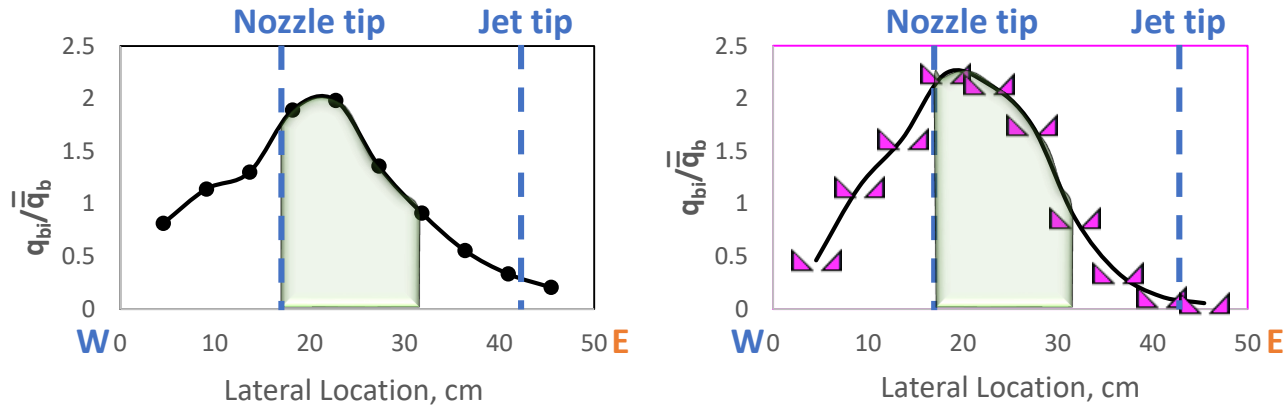
3 gas distributions



$V_g = 1 \text{ m/s}$, slumped after injection

Impact of gas distribution

Symmetrical baffles (even case)

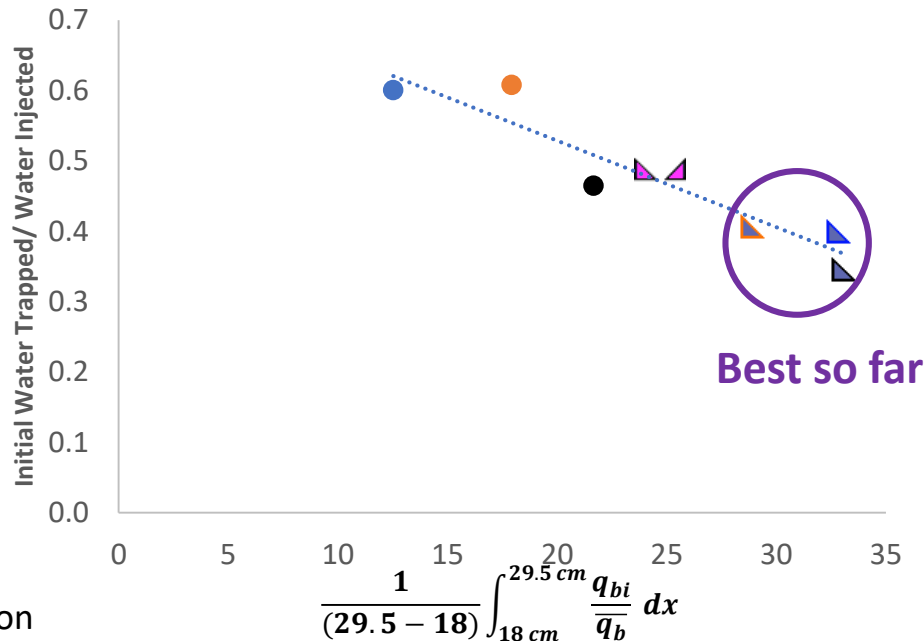
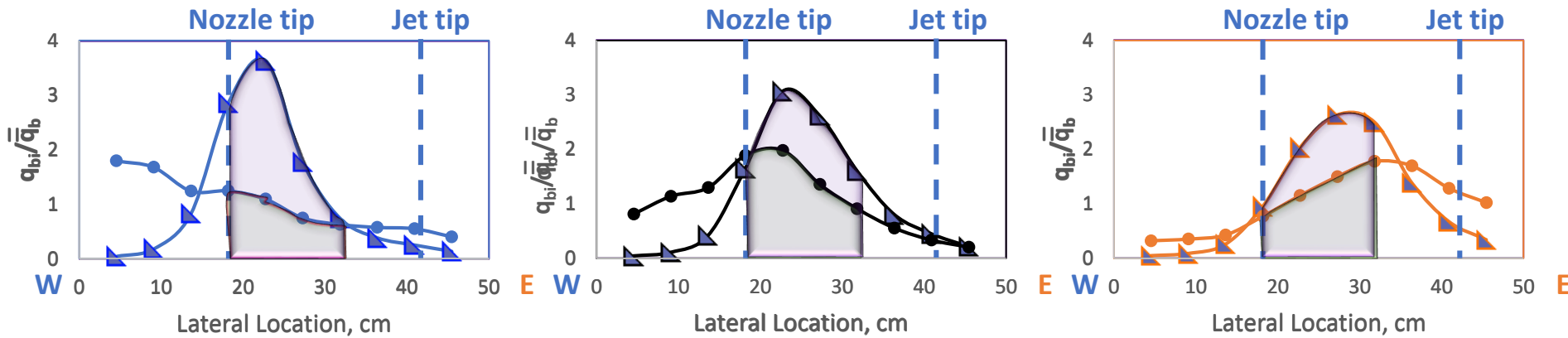


$V_g = 1$ m/s, slumped after injection

$$\frac{1}{(29.5 - 18)} \int_{18 \text{ cm}}^{29.5 \text{ cm}} \frac{q_{bi}}{\bar{q}_b} dx$$

Impact of gas distribution

3 gas distributions + single baffle



$V_g = 1$ m/s, slumped after injection

Conclusion

To reduce agglomeration:

1) Increase fluidization gas velocity

2) More efficient:

- **Move the nozzle**, so 1st half of jet cavity exposed to high bubble flow
- **Move the gas** to 1st half of jet cavity, with internals

Acknowledgments

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**NSERC
CRSNG**

ExxonMobil

Syncrude



References

Li, Lingchao, "Effect of Local Bed Hydrodynamics on the Distribution of Liquid in a Fluidized Bed" (2016). *Electronic Thesis and Dissertation Repository*. 4120.

Jahanmiri, Majid, "Effect of a baffle on gas bubbles flow patterns and the distribution of liquid injected into gas-solid fluidized beds" (in press).

Ariyapadi, S., Berruti, F., Briens, C., Griffith, P., & Hulet, C. (2003). Modeling the Injection of Gas Liquid Jets into Fluidized Beds of Fine Particles, 81(August), 891–899.

Appendices

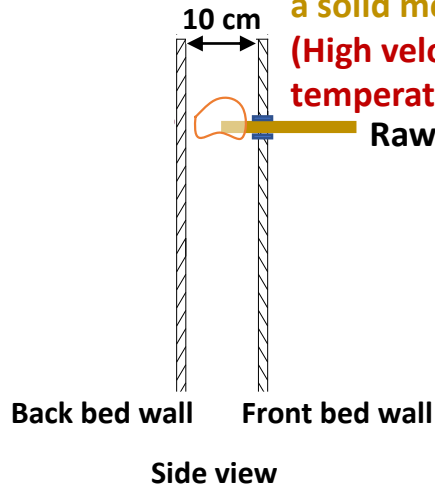
Equipment & Tribo-Probe Method

Gas Bubble Distribution Map

Tribo-probe:

a solid metal probe
(High velocity & temperature friendly)

Raw signal: $V = I \cdot R$



Principle:

Triboelectric current produced by collisions with fluidized particles in bubble wakes

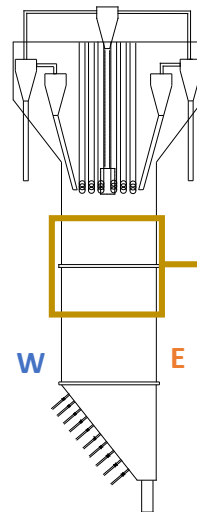
Cycle amplitude is applied to calculate local volumetric flux (q_{local})

$\frac{q_{local}}{q_{average}}$ shows the **bubble profile**

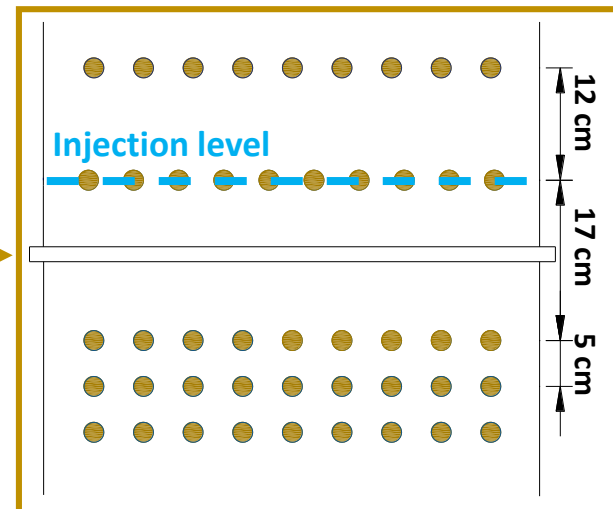
Poster session at

More about Tribo-probe Applications:

- Bubble profile
- Slugging check
- Bubble velocity
- Bubble evolution pattern
- Jet penetration
- ...



Locations



Tribo-electric Method

Principle:

The triboelectric current is produced by the collisions with fluidized particles in bubble wakes

Correlation:

$$q_{bi} = \alpha \textit{Amplitude}_{cycle}^{\beta}$$

where the q_{bi} is the volumetric flux, Cycle amplitude is applied for calibration

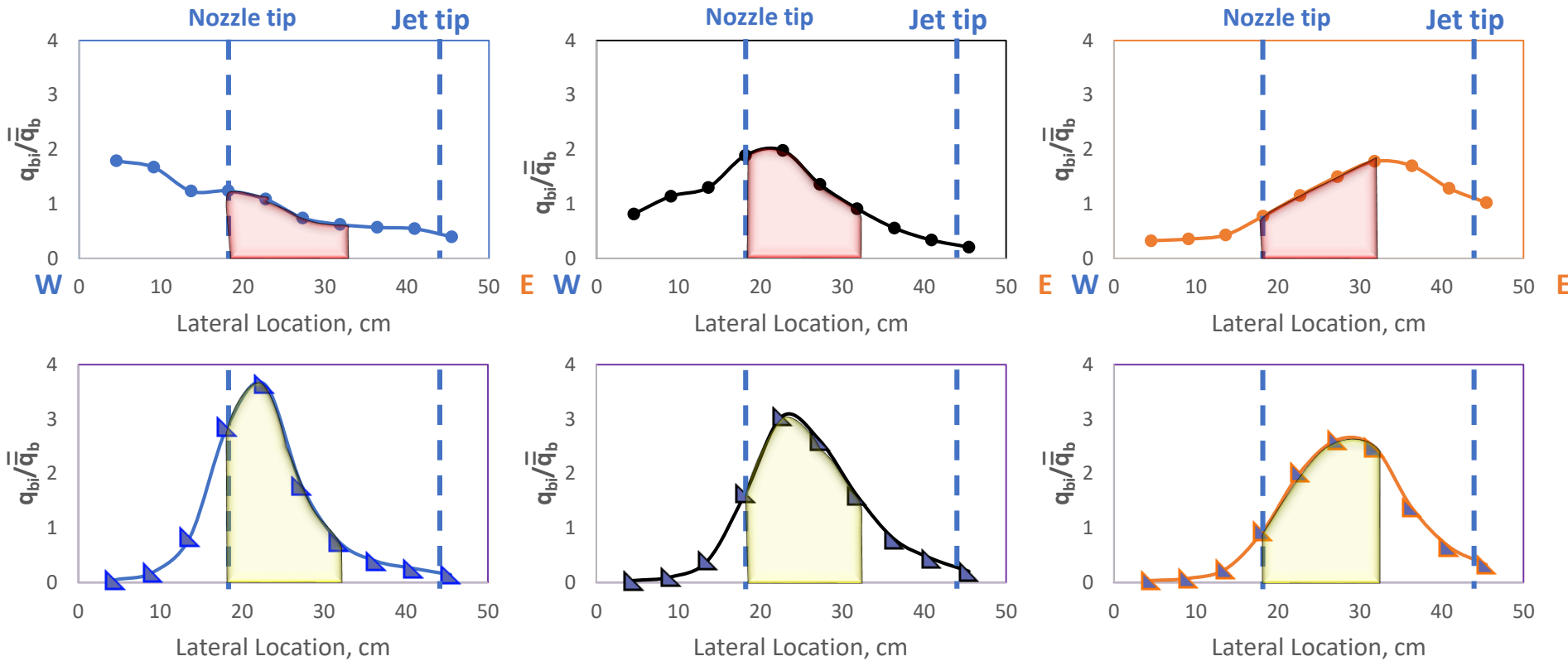
To get the bubble profile along the bed length:

$$\frac{q_{bi}}{q_b} = \frac{\textit{Amplitude}_{cycle}^{\beta}}{\frac{1}{\sum \lambda_i} \left[\sum \lambda_i \textit{Amplitude}_{cycle}^{\beta} \right]}$$

where λ_i = cross-sectional area associated with position
(Yuan & Jahanmiri et al., 2019)

Impact of gas distribution

3 gas distributions + baffle



Baffle successfully concentrate gas bubbles to 1st half of jet cavity