

# Achieve Test Run Objectives with Advance Preparation and Real Time Reports

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Charles D. Herzog, PE  
Consulting (Retired) Chemical Engineer  
Herzog Process Services, PLLC  
AIChE South Texas Section, Jan 2019



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# Types of Test Runs

- Performance guarantee
- Root cause analysis
- Scope identification for revamp project
- Others?



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# Test Run Preparation

- **Confirm material balance envelope**
- Prepare Excel calcs and reports in advance
- Obtain or create a simulation of the system
- Verify DCS data acquisition / migration to Excel
- Synchronize lab data with DCS data
- **Make a plan to reconcile data into a balance**

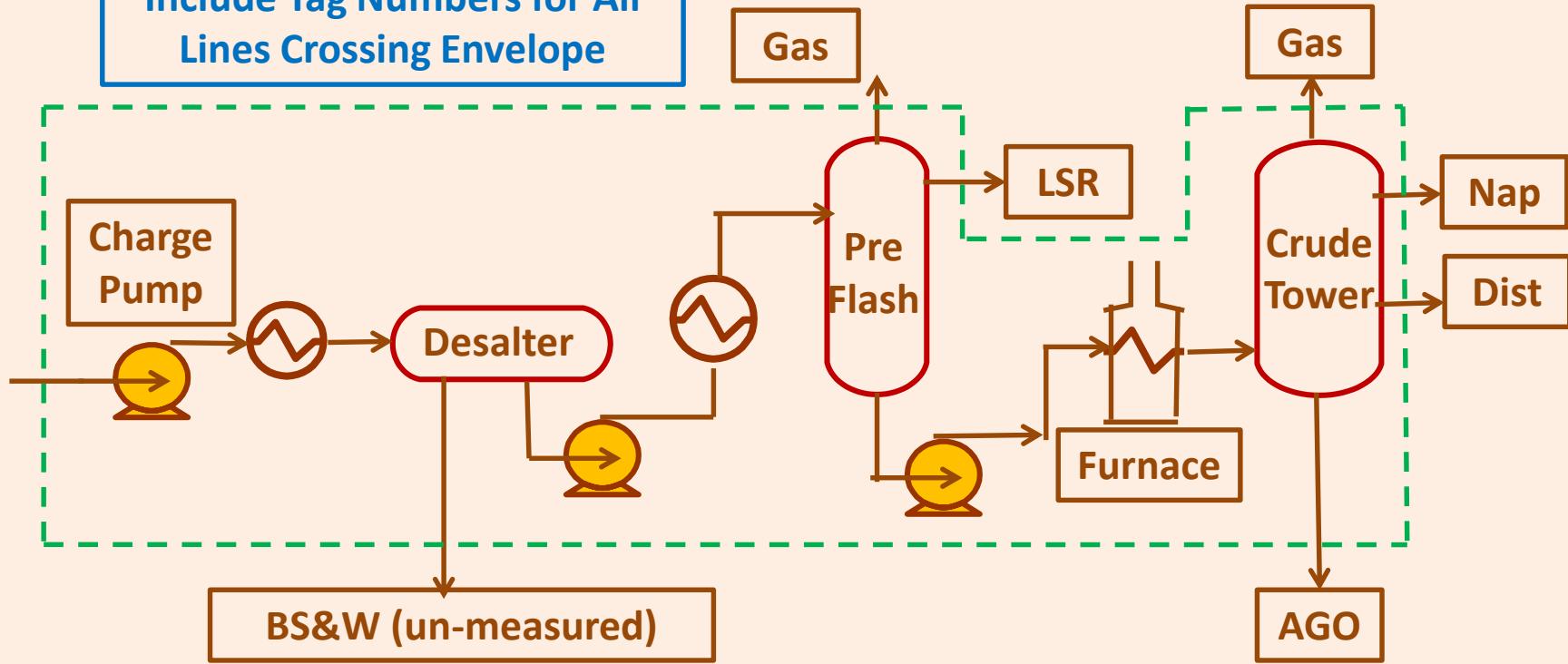


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# Material Balance Envelope for Crude Oil Unit

Include Tag Numbers for All Lines Crossing Envelope



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# Confirm Material Balance Envelope

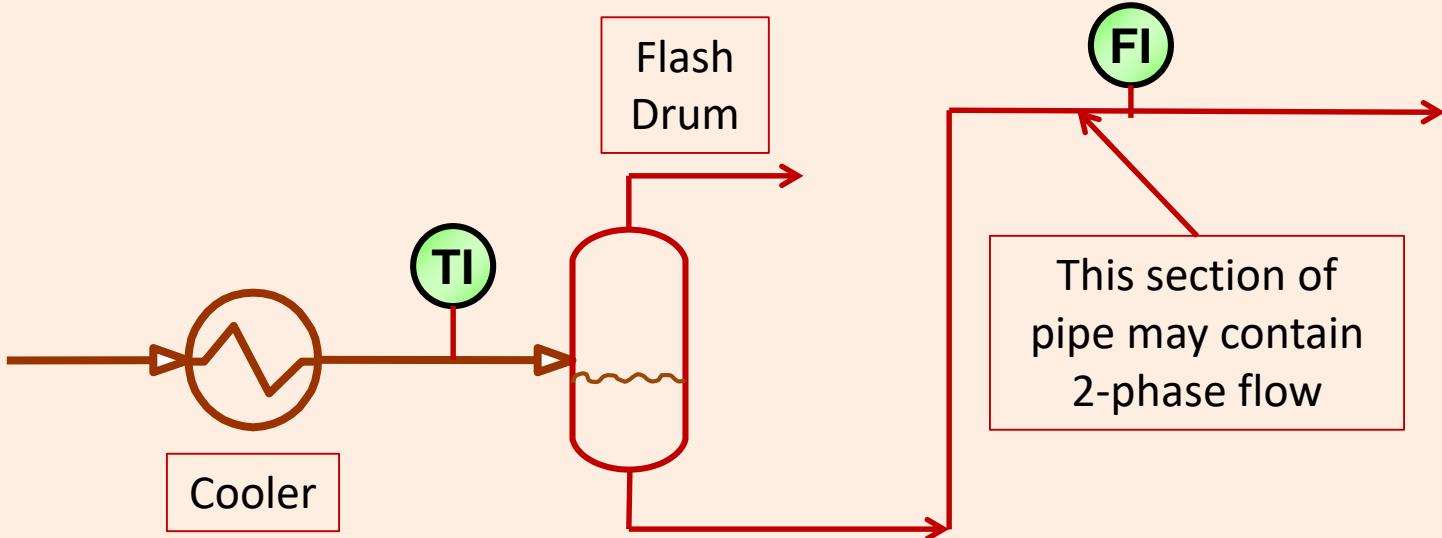
- Use daily material balance calcs as a starting point
- Normally closed lines must be included
- Agree how to account for any flaring during the test
- Identify any un-measured lines crossing envelope
- Try to use single-phase lines for flow measurement
- **Confirm material balance closure prior to test**



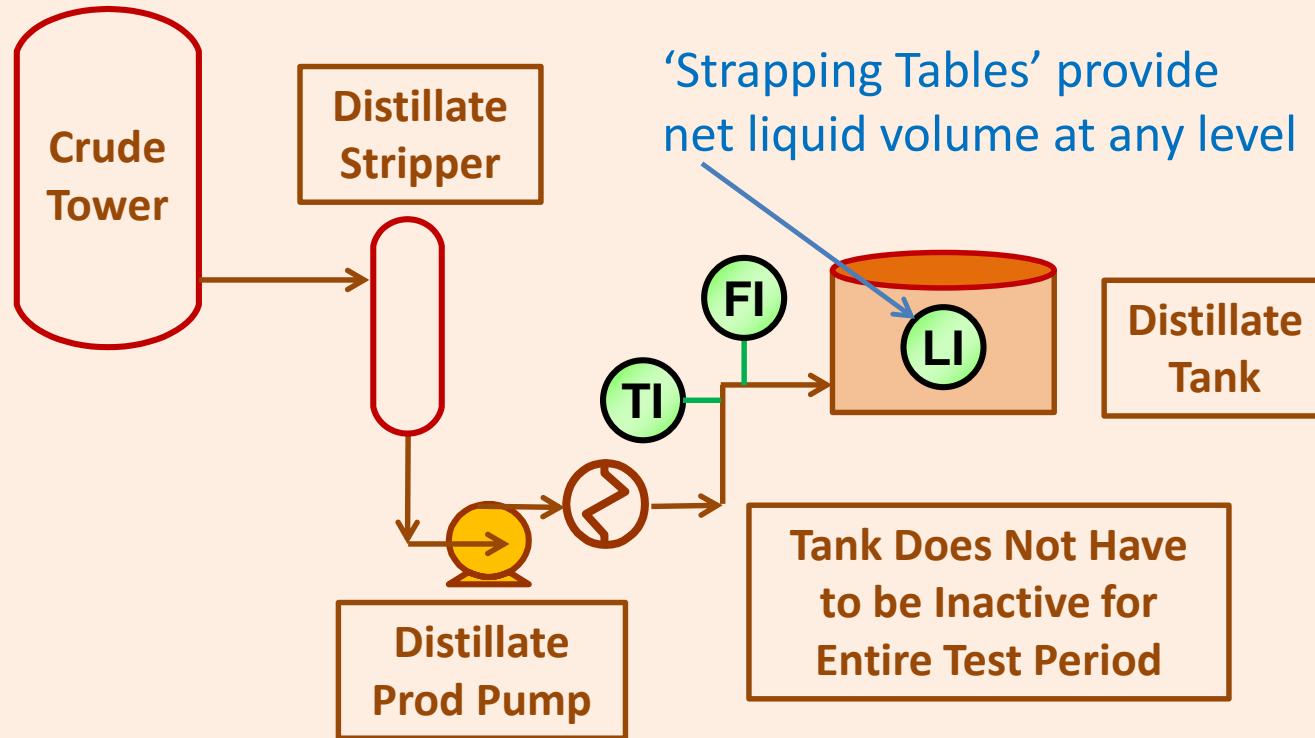
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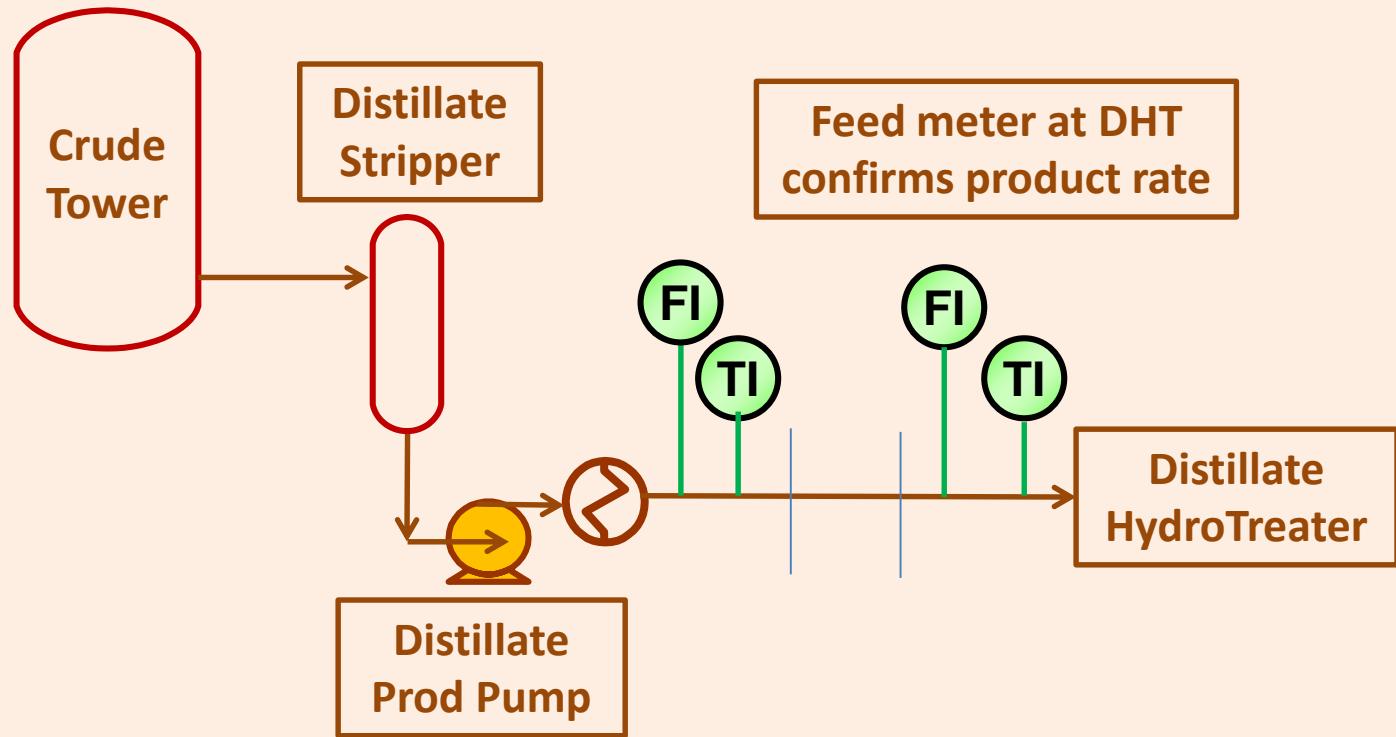
# Orifice Meters Work Best with One-Phase Flow



# Flow Data is Reconciled Against Tank Volume



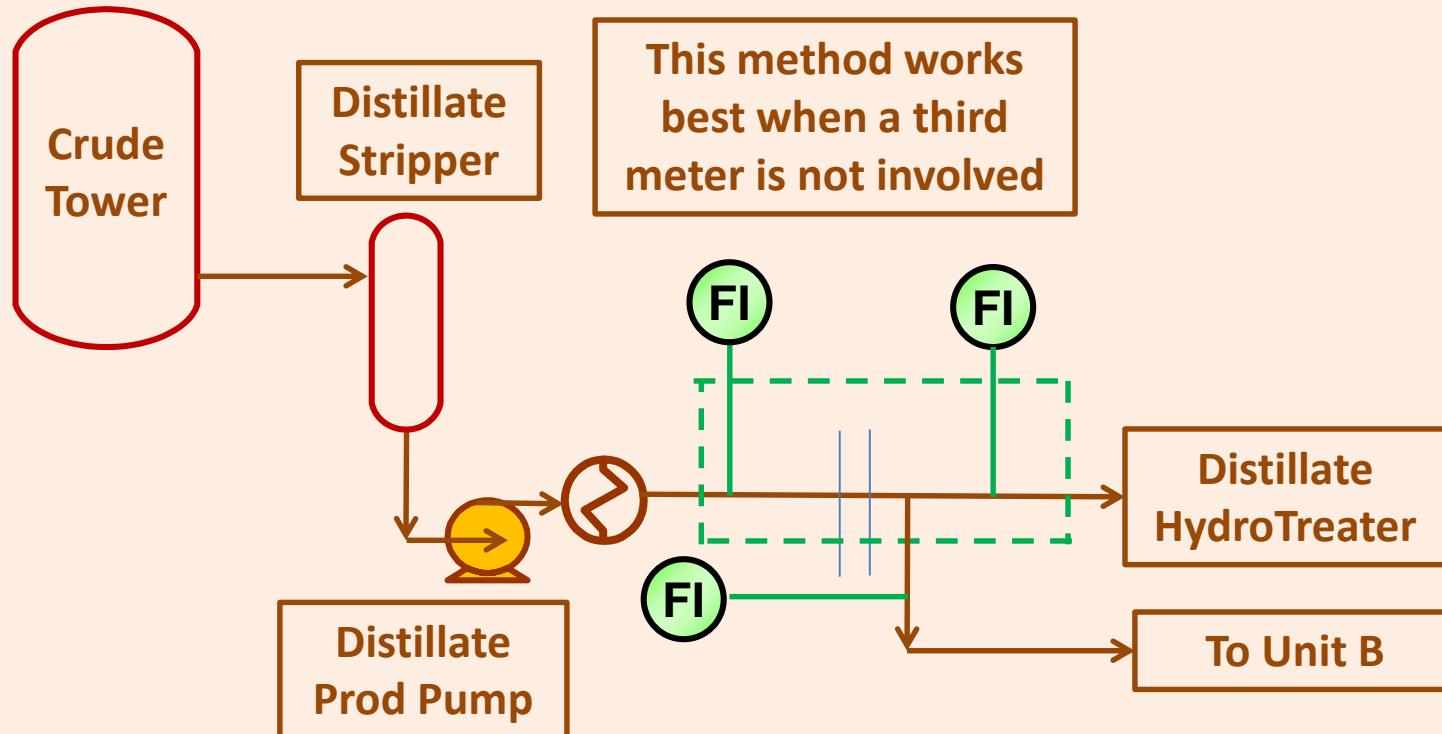
# Downstream Data Reconciles Product Rate



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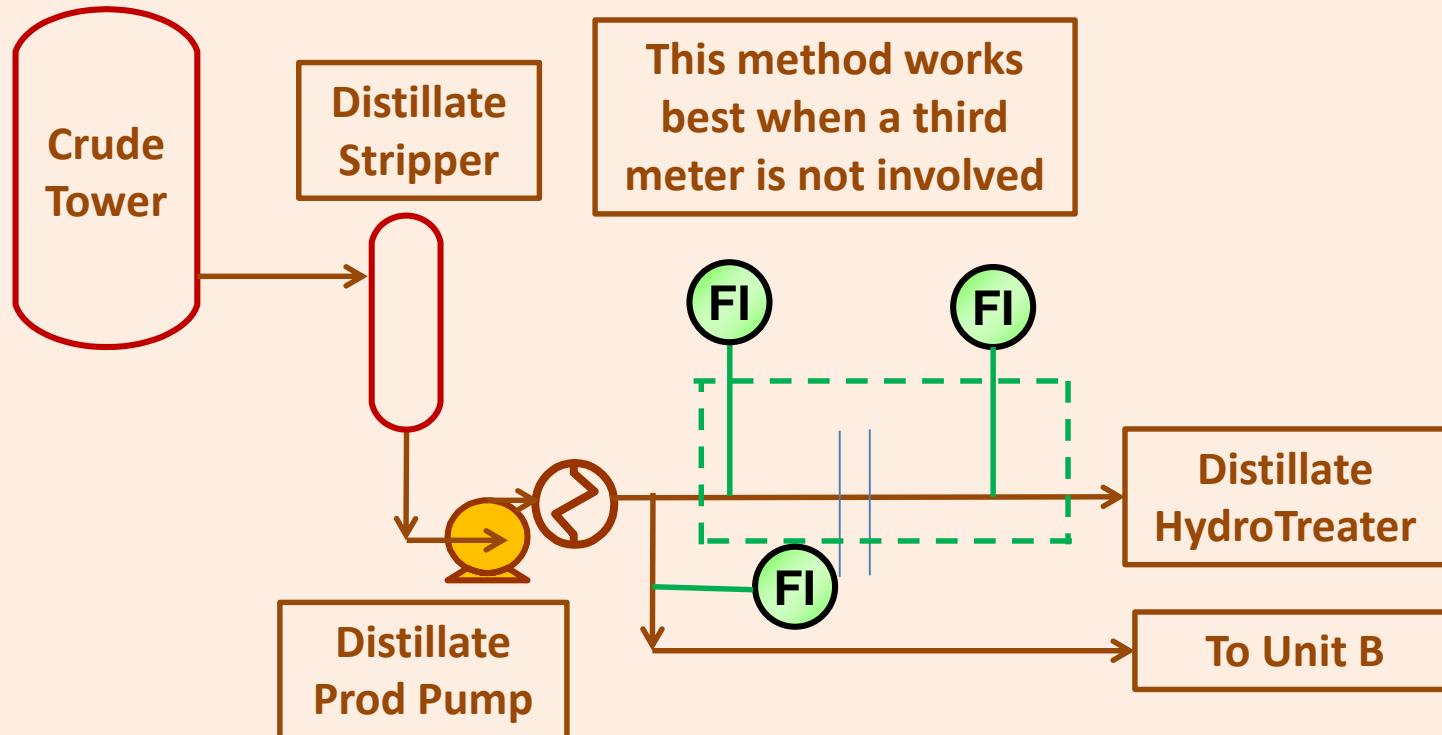
# Confirm Envelope with Downstream Unit



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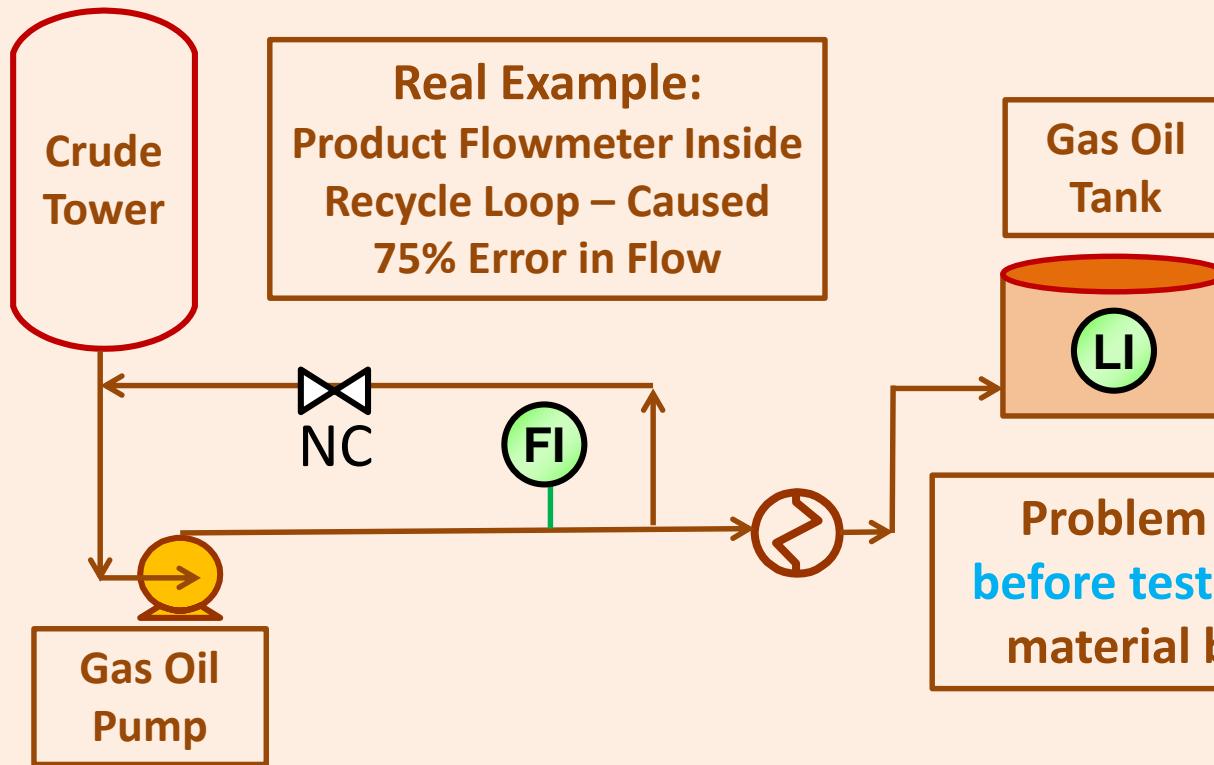
# Confirm Envelope with Downstream Unit



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# Identify Problems **BEFORE** Test Begins

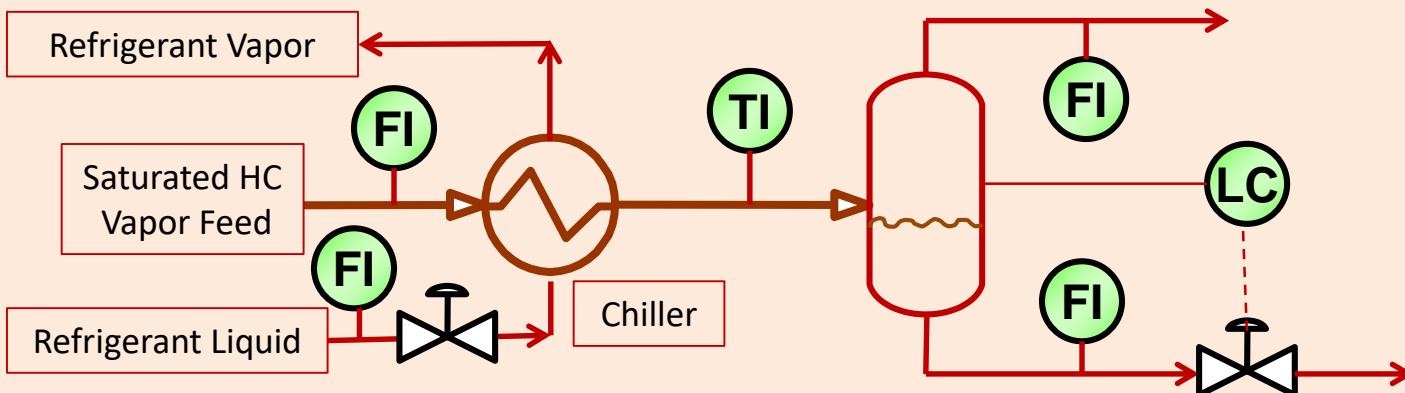


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# Refrigeration Example: Simulation Helps!

Level Must be Steady to Reconcile Data



Use Chiller Data Sheet and Condensing Curve



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# Sources of Flaring During Test

- Venting of non-condensibles from exchangers
- Exceeding capacity of condensing heat exchanger
- Making off-spec product
- **Increasing the feed too rapidly can result in flaring**



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# What Happens if Feed Increases too Rapidly?

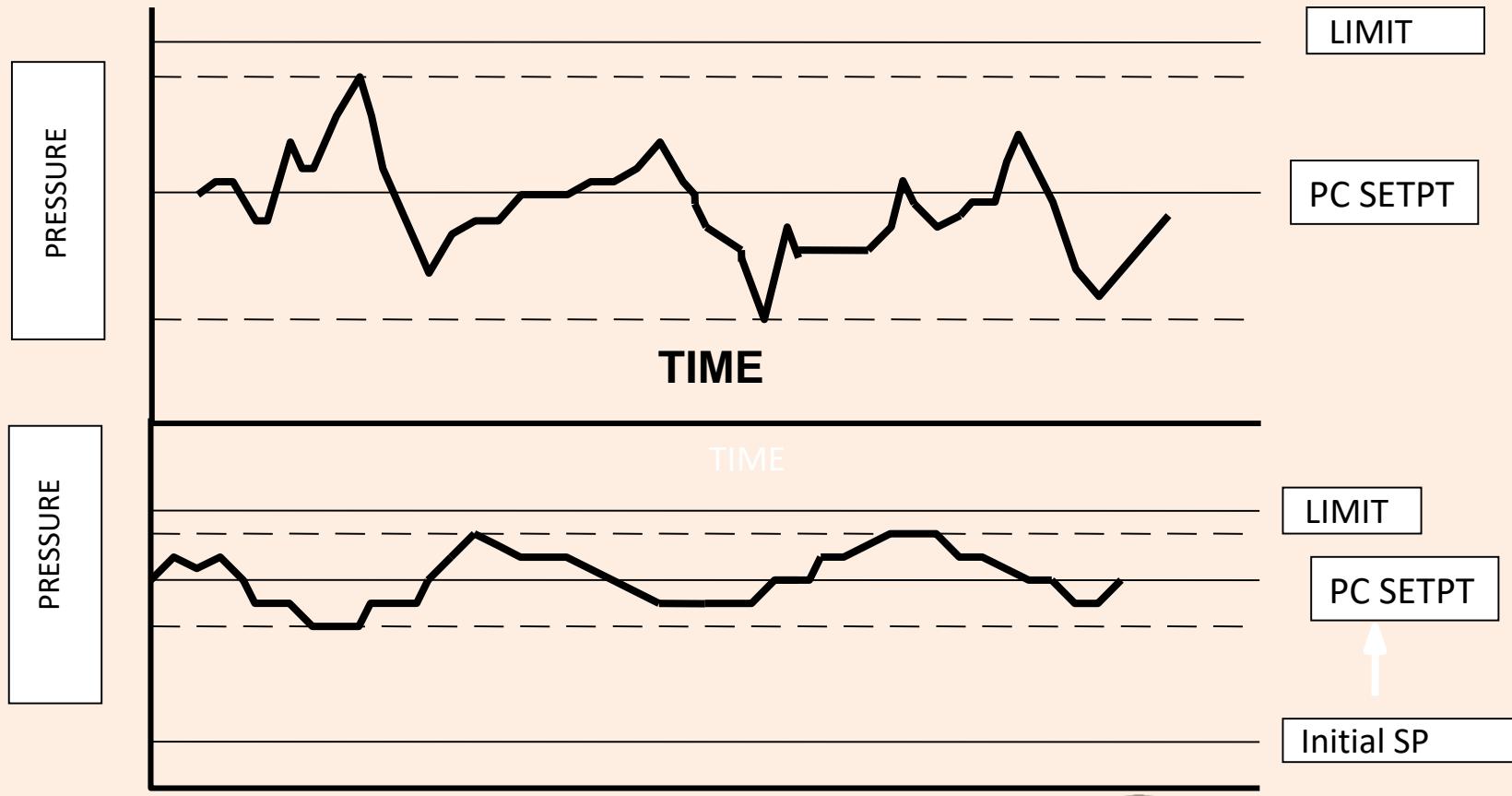
- Control system may fail to keep unit steady
- Equipment constraints may cause adverse result



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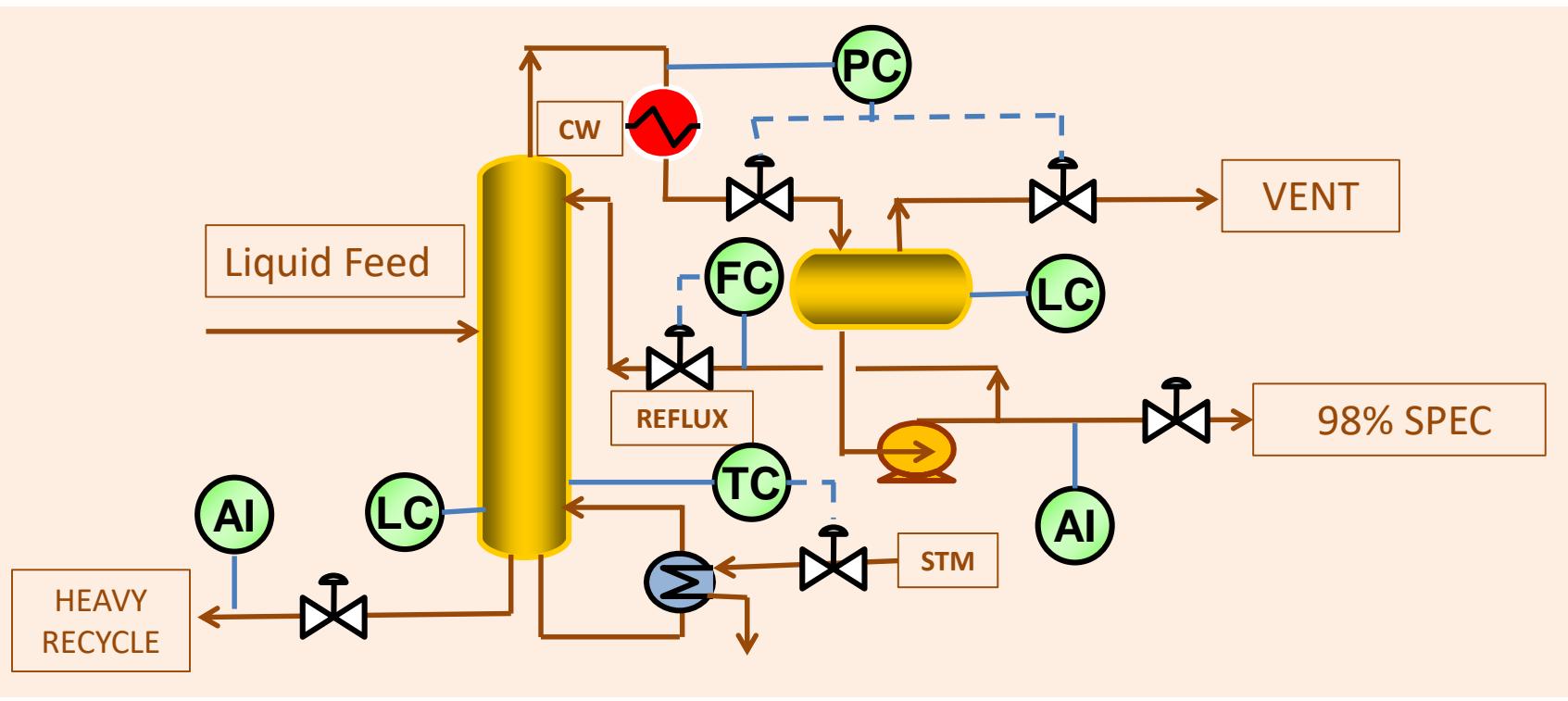
# Reduce Pressure Variation to Reduce Flaring



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# Condenser Constraint Causes Test Failure



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# Synchronize Lab Data with DCS Data

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1. Create a 'Lab Data' page on the Operator console
2. List all samples to be taken during the test
3. Operator clicks 'Sample Caught' as sample is drawn
4. Lab results are correctly saved in test historian



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# Synchronize Lab Data with DCS Data

## Typical 'Lab Data' Entry Page

Date: xx                      Time: yy

Crude Oil                     

Naphtha                     

**Kerosene**                     

Gas Oil                     

Sample  
Caught

Operator uses this display to time-stamp Kerosene sample



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# Obtain or Create a Simulation of the System

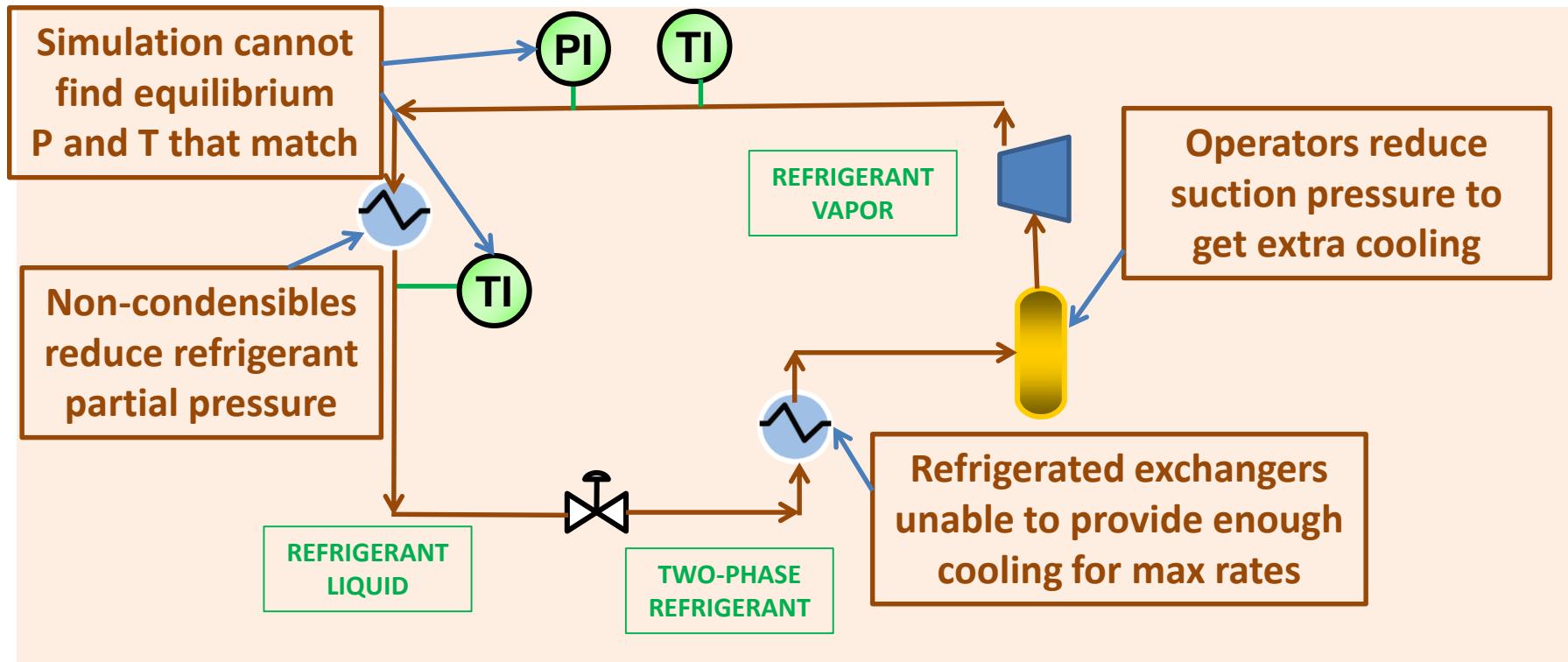
- Often there is an existing simulation available
- Use simulators for balances and density calculations
- Simulation can help identify certain problems
- Simulating the system adds credibility
- **Agreed simulation leads to report acceptance**



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# Use Simulation to Identify Root Cause



# On Site Test Activities

- **Verify material balance closure in advance**
- Bring plant to test run conditions **SLOWLY**
- Get products **on spec** before increasing feed
- Ensure levels are steady before increasing feed
- Provide real-time feedback to Operations
- **Identify equipment nearing its capacity limit**



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# Test Run Spreadsheet

Use spreadsheet for most functions:

- Data Acquisition / Flow Compensation
- Heat and material balancing
- Management reports
- Saving intermediate results of all complex calcs



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# Test Run Spreadsheet

- Only the spreadsheet ‘**Owner**’ changes formulas
- Owner provides data entry areas as necessary
- Exercise care in copying and pasting formulas
- Naming cells or ranges eliminates some errors



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# Data Acquisition

Establish a single data acquisition sheet for raw data

- Create a data block for every flowmeter in the system
- Include columns for temp, press, and compensation calcs
- Verify instrument ranges from [latest](#) instrument data sheets
- Include all related tags in the data acquisition list
- Include ‘redundant’ tags at upstream or downstream units



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# Typical Data Block

| Tag: FI-1000   | Desc: Ethylene Product |       |               | Units: Mlb/hr                            |        |           |  |
|--|------------------------|-------|---------------|--|--------|-----------|--|
| Flow: 120.0  | Oper P: 1800 psi       |       | Oper T: 60° F | Dens: 24.0                               | lb/cf  |           |  |
| Time   | Raw Flow               | Press | Temp          | Dens                                     | Factor | Comp Flow |  |
| 0100   | 112.0                  | 1820  | 58.2          | 24.1                                     | 1.002  | 112.2     |  |
| 0115   | 112.2                  | 1819  | 58.1          | 24.1                                     | 1.002  | 112.4     |  |
| 0130   | 112.3                  | 1819  | 58.1          | 24.1                                     | 1.002  | 112.5     |  |
| Simulator calculates density for compressible fluids |                        |       |               | Ensure continuity with reference density |        |           |  |



# Consider Using a Tool to Create Data Blocks

- Steam
- Condensate
- Process Liquid
- Process Gas

| Add New Process Liquid Tag |              |            |
|----------------------------|--------------|------------|
| Tag Name                   | fi-1         |            |
| Description                | overhead     |            |
| Flow Units                 | lb           |            |
| Time Units                 | hr           |            |
| Gravity Units              | lb / cu ft   |            |
| Flow Compensation Type     | Liq Mass     |            |
| Base Gravity Measurement   | not measured |            |
| Flow Gravity Measurement   | none         |            |
| Temperature Tag            | ti-1         |            |
| Gravity Tag                | gi-1         |            |
| Full Scale Flow            | 100.00       | Mlb / hr   |
| Base Gravity or Density    | 50.00        | lb / cu ft |
| Design Temperature         | 90.00        | ° F        |
| Grav / Dens at Design Temp | 49.00        | lb / cu ft |



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# Establish Flow Compensation

- Engineering units may be mass, volume, or std volume
- Flow compensation equation depends on units of flow
- Create columns for each flow tag:
  - “Raw” flow from DCS
  - Compensating temperature
  - Compensating pressure
  - Molecular weight (based on analysis)
  - Flowing gravity for liquids
  - Compensated flow

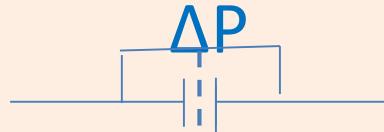


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# Orifice Flow Meter Compensation

- Based on Bernoulli's Principle
- Typical orifice measures differential pressure ( $\Delta P$ )
- Mass flow proportional to  $( \Delta P \times \rho )^{1/2}$
- Flow meter compensation accounts for density
- **L.K. Spink** is a reference for flow compensation



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# Frequently Used Compensation Equations

## Vapor Streams:

- P, T, MW compensation for compressibility  $> 0.9$
- Typical Eng Units are Mass or '**Standard Vapor Volume**'

## Liquid Streams:

- Liquid density independent of pressure
- Estimate slope of **density vs temperature**
- Standard volume (e.g., barrels) use different equations



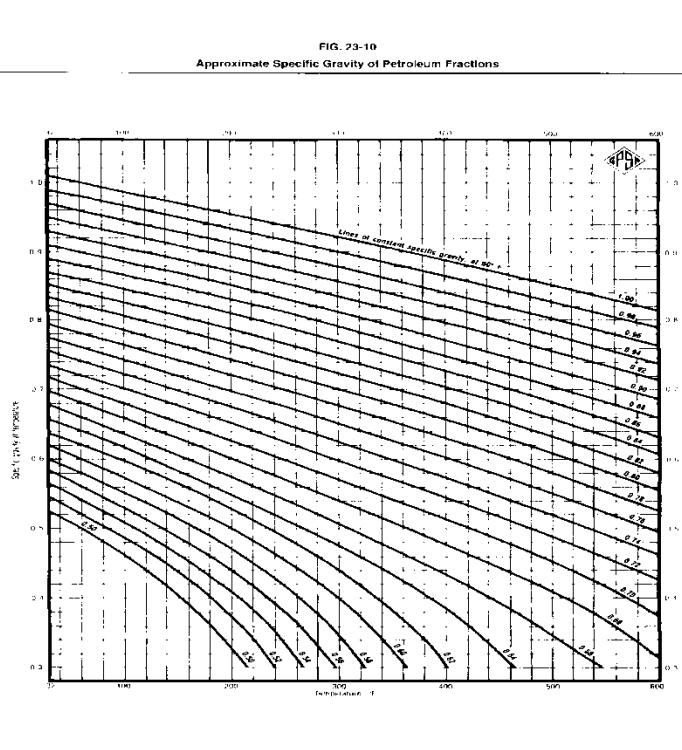
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# Use GPSA Tables for Oil Products

## GPSA Fig 23-10

# Gravity vs Temp



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# Standard Vapor Comp vs Mass Flow Comp

Examples of Standard Vapor Flow Units:

- Standard Cubic Feet Per Minute (SCFM)
- Normal Cubic Meters Per Hour

Standard Vapor Flow is Proportional to **MOLES / HR**



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# Standard Vapor Comp vs Mass Flow Comp

Vapor Mass Flow Compensation:

$$\text{Comp Factor} = \left( \frac{P}{P_0} \times \frac{T_0}{T} \times \frac{MW}{MW_0} \right)^{1/2}$$

Standard Vapor Flow Compensation:

$$\text{Comp Factor} = \left( \frac{P}{P_0} \times \frac{T_0}{T} \times \frac{MW_0}{MW} \right)^{1/2}$$



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# Standard Liquid Comp vs Mass Flow Comp

Example of Standard Liquid Flow Units:

**Standard Barrels Per Day (BPD)**

Standard Barrels are Referenced to 'Base Gravity'

**Base Gravity = GB = Specific Gravity at 60°F**

The **base gravity** is a function of composition only



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# Standard Liquid Comp vs Mass Flow Comp

Mass Flow Compensation:

$$\text{Comp Factor} = (\rho / \rho_0)^{1/2}$$

$$\rho = \rho_0 + \text{slope} \times (T - T_0)$$

Standard Liquid Flow Compensation:

$$\text{Comp Factor} = (\text{GF} / \text{GF}_0)^{1/2} / (\text{GB}_0 / \text{GB})$$

GF and  $\text{GF}_0$  refer to flowing specific gravity at T and  $T_0$



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# Common Problems to Avoid

- Allowing insufficient time to prepare
- Using the incorrect flow compensations
- Failure to review report with Operations
- Failure to verify balances before test
- Failure to tune DCS control loops



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# Create a Tool for Operations Staff

- Establish flexible test run report with user-entered start and end times
- Having a **computer-savvy** person on the team helps
- Make certain that operations staff understand report format and calculations before actual test begins



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# Test Run Report for Crude Oil Unit

Date: xx

Time Start: yy

Time End: zz

Overall Test

Last 4 Hours

Feeds:

|  | MB/D | LB/HR | MB/D | LB/HR |
|--|------|-------|------|-------|
|--|------|-------|------|-------|

Crude A

aa

bb

cc

dd

Crude B

etc

Total

Products

.....

Total

% Error

Include Tag  
Numbers for  
All Streams



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# Final Test Preparations

- Review unit operation for 24 hours prior to test
- Ensure that the unit material balance is reaching acceptable closure
- Identify any unsteady flows or operating conditions. Fix control problems if possible
- Control problems tend to get worse when equipment operates near capacity limit



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# Offer Assistance During the Test

- Once the actual test has begun, be available to offer assistance as needed.
- Monitor the initial reports during the first few hours of the test.
- Identify any material balance errors or any performance criteria that are not being satisfied.



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# Thank You!

