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# **Electric Power Production Efficiency Improvements and Discussion of Carbon Dioxide Capture & Storage for Fossil-Fired Power Plants**

**South Texas Section (STS) of the  
American Institute of Chemical Engineers**

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# Topics

- Introduction
- Energy Efficiency Discussion – Power Plants
- CO<sub>2</sub> Capture and Storage Systems (CCS)
- Impact of Air Quality Control Systems (AQCS) on CCS – Energy Efficiency
- Summary



# Power Plant Efficiency Discussion

# Topics Concerning Efficiency Improvements in Fossil-Fired Power Plants

- Heat rate and power plant efficiency improvements
- Definitions of efficiency
- Boiler steam pressure and temperature
- Improved integration of power plant auxiliary systems
- Different fuels
- Co-fired alternative fuels with coal
- Repowering
- CO<sub>2</sub> production, capture, and storage
- Other issues

# Efficiency Definitions

(there are numerous definitions)

**Net Electrical Efficiency is  
net electrical energy divided by total heating value energy of input fuels**

- Examples of why efficiency definitions and values vary:
  - Where and how net electrical energy is measured (generator vs. transmission tower)
  - Type of fuels (coal, natural gas, oil, hydrogen, etc.)
  - Higher or Lower heating value of fuels (HHV vs. LHV)
  - Auxiliary plant equipment in *or* out of service (feed water heaters, cooling, AQCS, CCS)
  - Weather conditions (summer or winter cooling loads)
  - Test methods and procedure (ASME, international standards)
  - Other reasons why efficiency definitions and values can vary

# Boiler Steam Pressure and Temperature

(impacts plant efficiency, flue gas and CO<sub>2</sub> production, etc.)

- Ultra supercritical boilers
- Supercritical boilers
- Subcritical boilers
- Other

# Different Types of Fossil Fuels

(impact plant efficiency, flue gas and CO<sub>2</sub> production, etc.)

Fossil Fuel Type	Total Carbon Content (% carbon weight)	Higher Heating Value (HHV, Btu/pound fuel)	CO <sub>2</sub> Production Rate (lb CO <sub>2</sub> per million Btu, HHV)
Coal – A	83.7	11,890	258
Coal – B	74.0	12,540	216
Coal – SB	70.3	9,190	280
Coal – L	63.3	7,090	327
Bagasse	23.4	4,000	214
Fuel Oil – # 2	87.2	19,460	164
Fuel Oil – # 6	88.4	18,200	178
Natural Gas –1	75.2	23,170	119
Natural Gas –5	64.8	20,160	118
MSW	27.9	5,100	200
RDF	36.1	6,200	213

# Mass & Energy Balance CO<sub>2</sub> Issues

**Coal is readily available to generate electricity reliably, efficiently and cost-effectively, while meeting environmental regulations.**

- Combustion Chemistry (related to carbon):



- Example (typical coal containing ~70% carbon):
  - ▶ 1.0 tonne Coal
  - ▶ 2.5 tonne CO<sub>2</sub>
  - ▶ 6.6 million Kcal (HHV) total energy
  - ▶ ~85% of energy is from carbon

# Carbon Dioxide Capture

**(Energy Efficiency Issues)**

# Energy Efficiency and Carbon Dioxide Reduction for Various Types of Power Plants

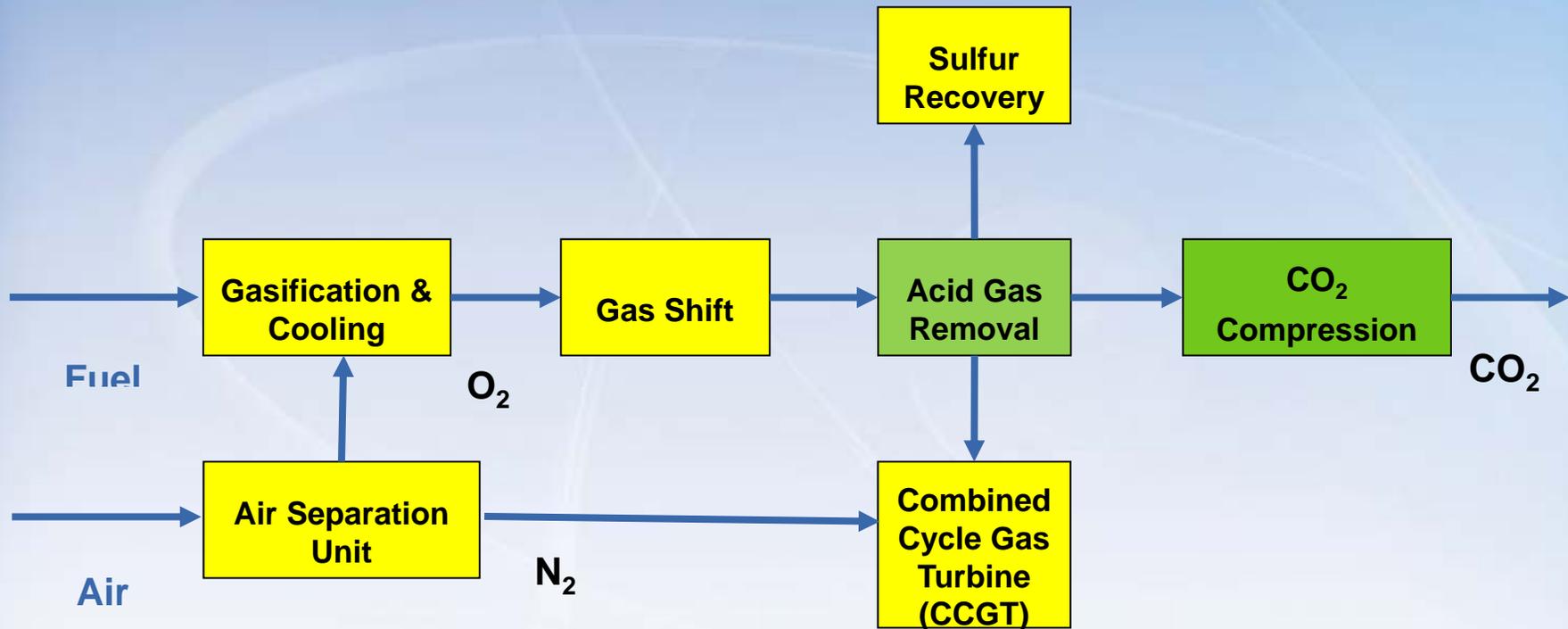
## CO<sub>2</sub> Reduction

- Heat rate and power plant efficiency improvements
- Co-fired alternative fuels with coal
- Repowering
- Other methods

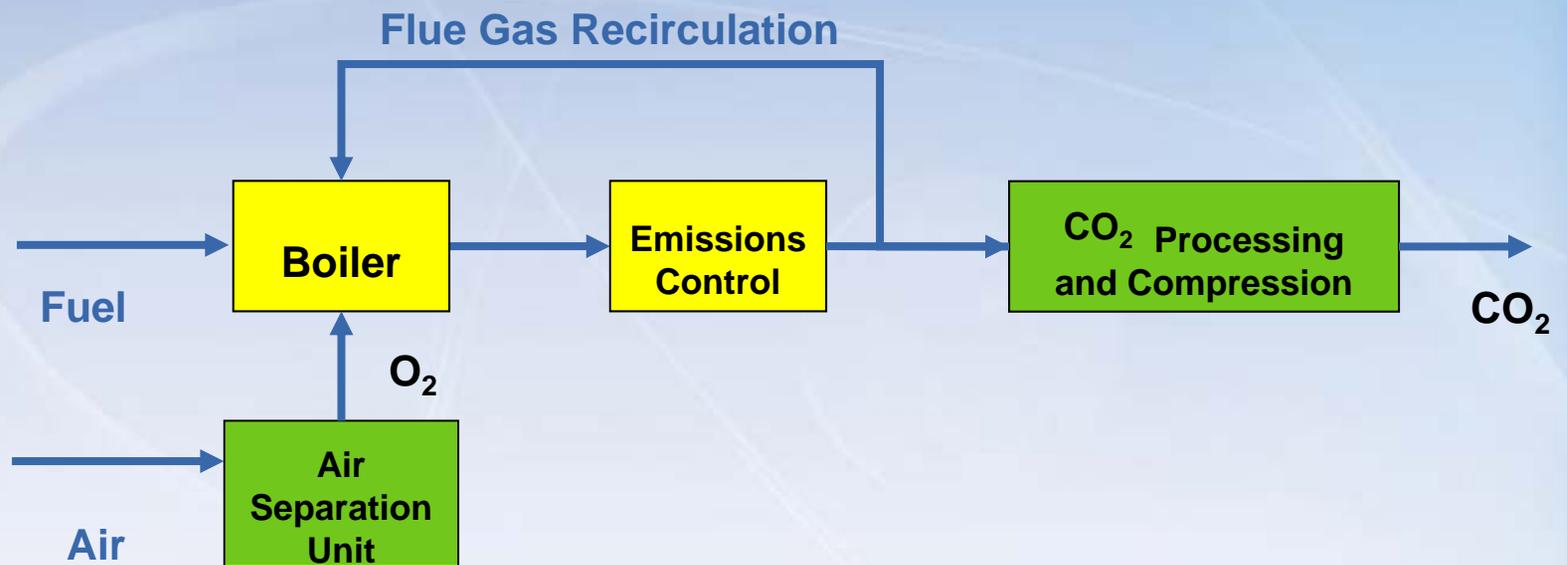
## CO<sub>2</sub> Capture

- Pre-combustion CO<sub>2</sub> capture technologies for Integrated Gasification Combined Cycle (IGCC)
- Oxy-fuel combustion technology with CO<sub>2</sub> capture
- Post-combustion (flue gas) CO<sub>2</sub> capture processes

# IGCC Process with Pre-Combustion Carbon Dioxide Capture



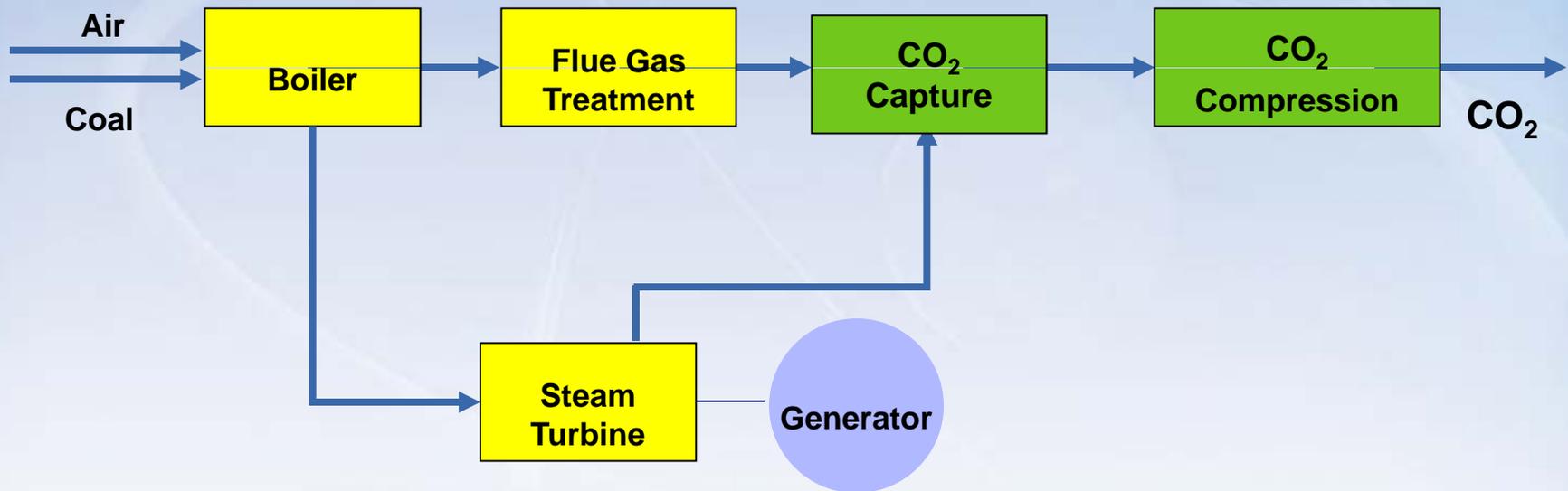
# OxyFuel Process with Carbon Dioxide Capture



# Post-Combustion Carbon Dioxide Capture

**(Energy Considerations)**

# Pulverized Coal Post-Combustion Process CO<sub>2</sub> Capture



# Technology Options for Post-Combustion CO<sub>2</sub> Capture

(each process has its own energy efficiency issues)

- Amine-based absorption (generic and advanced amines)
- Ammonia absorption process (aqueous ammonia, not chilled)
- Chilled ammonia absorption (aqueous ammonia)
- Solvent-based absorption (non-amine-solvents)
- Algae-based process using solar energy
- Enzyme-based process
- Membrane-type processes
- Physical adsorption of CO<sub>2</sub> in solvents
- Solid sorbents for CO<sub>2</sub> absorption and/or adsorption.
- Frosting or anti-sublimation processes
- Other technologies (being developed, R&D, piloted)

# Technical Feasibility of Pulverized Coal (PC) CO<sub>2</sub> Capture (energy efficiency considerations)

- Most individual equipment components are demonstrated
- Most unit operations are demonstrated – (but often under conditions not typical for most coal-fired power plants)
- CO<sub>2</sub> capture systems need to be demonstrated (various scales)
- PC CO<sub>2</sub> capture – future pilot and demonstrations - (with lessons learned with regard to design, energy usage, operation, and maintenance)
  - Amine CO<sub>2</sub> capture process
  - Ammonia CO<sub>2</sub> capture process
  - Chilled ammonia CO<sub>2</sub> capture process
  - Solvent-based absorption (non-amine-solvents)
  - Algae/sunlight-based CO<sub>2</sub> capture process
  - Frosting or anti-sublimation process
  - Other

# Post-Combustion Carbon Dioxide Capture Integration and O&M Considerations

**Energy Efficiency Issues of CCS on  
Fossil-Fired Power Plant**



# Typical CO<sub>2</sub> Capture and Storage Equipment

(Designed for Proper Energy Efficiency, O&M, Layout)

- Flue gas booster fan
- Deep FGD equipment (if required)
- CO<sub>2</sub> absorber column
- Heat exchangers (cooling water)
- CO<sub>2</sub> capture solvent delivery, storage, and handling equipment
- CO<sub>2</sub> desorber column
- Steam generator (reboiler) for CO<sub>2</sub> desorber column
- Spent CO<sub>2</sub> solvent storage, handling, and disposal equipment
- CO<sub>2</sub> coolers, dryers and compressors
- CO<sub>2</sub> pipeline and storage equipment

# Impacts and Integration of CO<sub>2</sub> Capture and Storage System

(Design in Advance for Energy Efficiency Considerations)

- Real estate (land area) for deep FGD equipment (if required)
- Real estate for additional NO<sub>x</sub> and PM reduction systems (if required)
- Real estate required for CO<sub>2</sub> capture system equipment
- Real estate for CO<sub>2</sub> cooling, drying, and compression equipment
- Real estate for CO<sub>2</sub> transport (pipeline)
- Real estate for interconnecting piping, roads, ductwork, BOP equipment, etc.
- Real estate for CO<sub>2</sub> sequestration or re-use system (if onsite)
- Electrical power usage and impact on plant electrical system
- Steam requirement and impact on plant steam turbine system
- Cooling water usage
- Route for interconnections

# Impacts and Integration of CO<sub>2</sub> Capture and Storage System

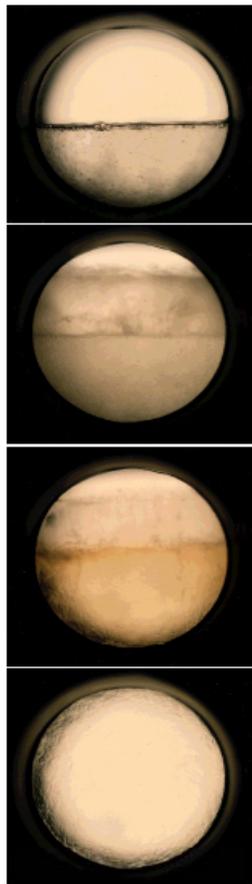
(Design in Advance for Energy Efficiency Considerations) (cont.)

- Impact on flue gas cleaning system (e.g., deep FGD, if required)
- Impact on stack for the processed flue gas
- Water balance issues
- O&M personnel requirements
- Maintenance and spare part requirements
- Disposal or regeneration of the spent CO<sub>2</sub> sorbent/material
- Permit issues
- CO<sub>2</sub> by-product reuse or CO<sub>2</sub> storage
- Safety, environmental and other issues

# Example of Potential Heat Integration



## PT Diagram & Supercritical Phase



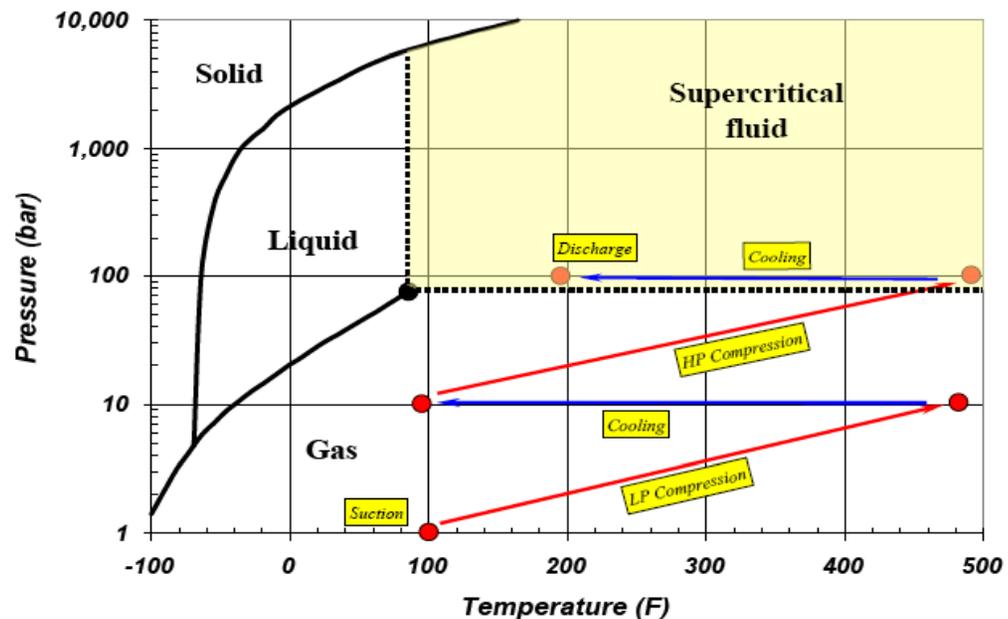
Separate Phases  
Visible-  
Meniscus Clearly  
Observed

Increase in  
Temperature-  
Diminished  
Meniscus

Further Increase in  
Temperature-  
Gas & Liquid  
Densities more Similar

At Critical P & T-  
Distinct Gas & Liquid  
Phases no Longer  
Visible "Supercritical  
Fluid" with Properties  
of Both Liquids & Gases

- Compression process transitions from superheated to supercritical phases
- Avoids liquid (sub-cooled) phase



# Disposition of the Captured CO<sub>2</sub>

(energy efficiency considerations)

**Where will 12,000 tonnes CO<sub>2</sub>/day  
of liquid CO<sub>2</sub> product be sent?**

# Mass Balance CO<sub>2</sub> Issues

*Coal is readily available to generate electricity reliably, efficiently and cost-effectively, while meeting environmental regulations.*

- Combustion Chemistry (related to carbon):



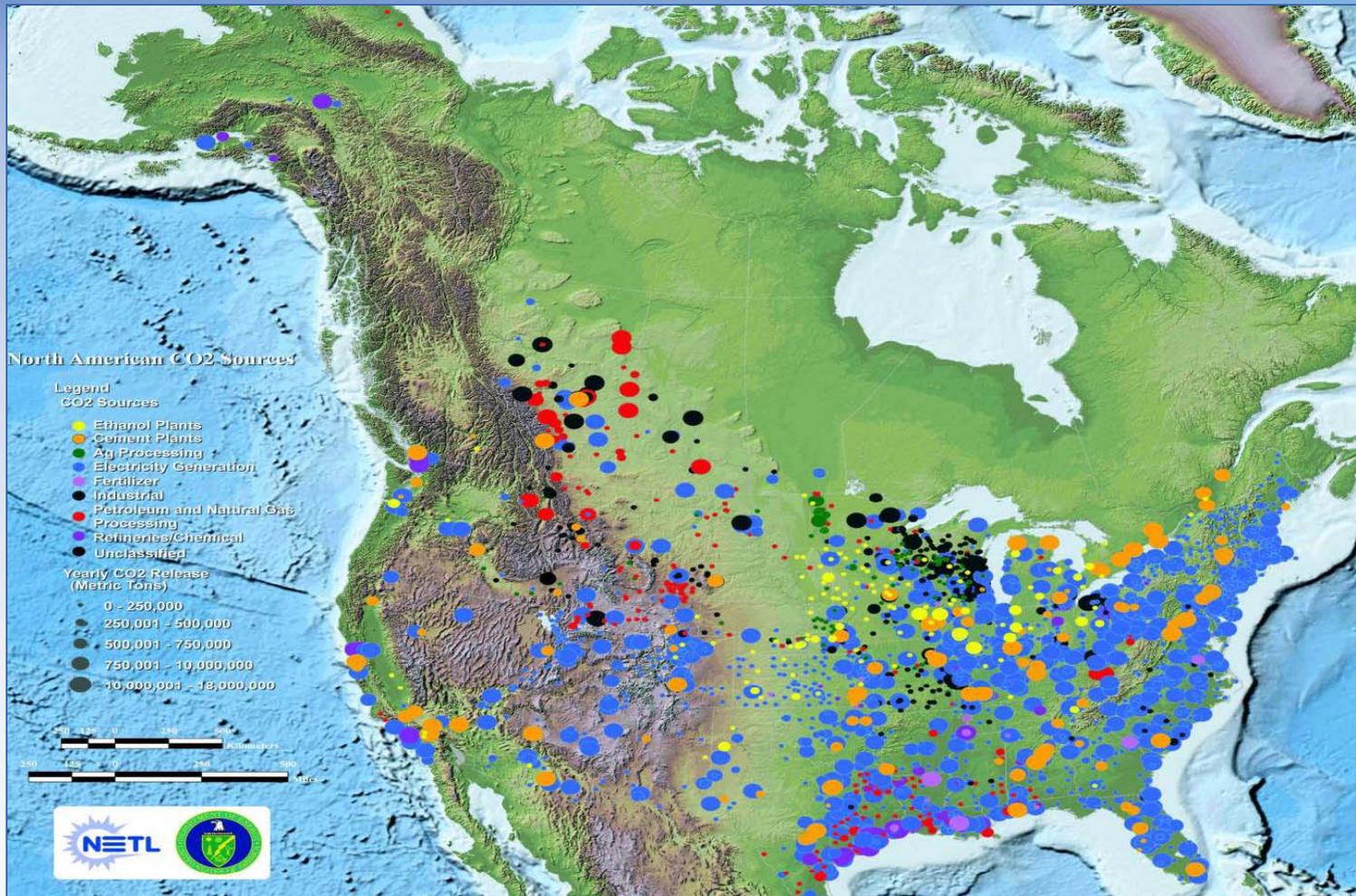
- Example (typical coal containing ~ 70% carbon):

▶ 12,000 tonne CO<sub>2</sub> per day

# Earth at Night



# U.S. and Canada – CO<sub>2</sub> Sources and Size

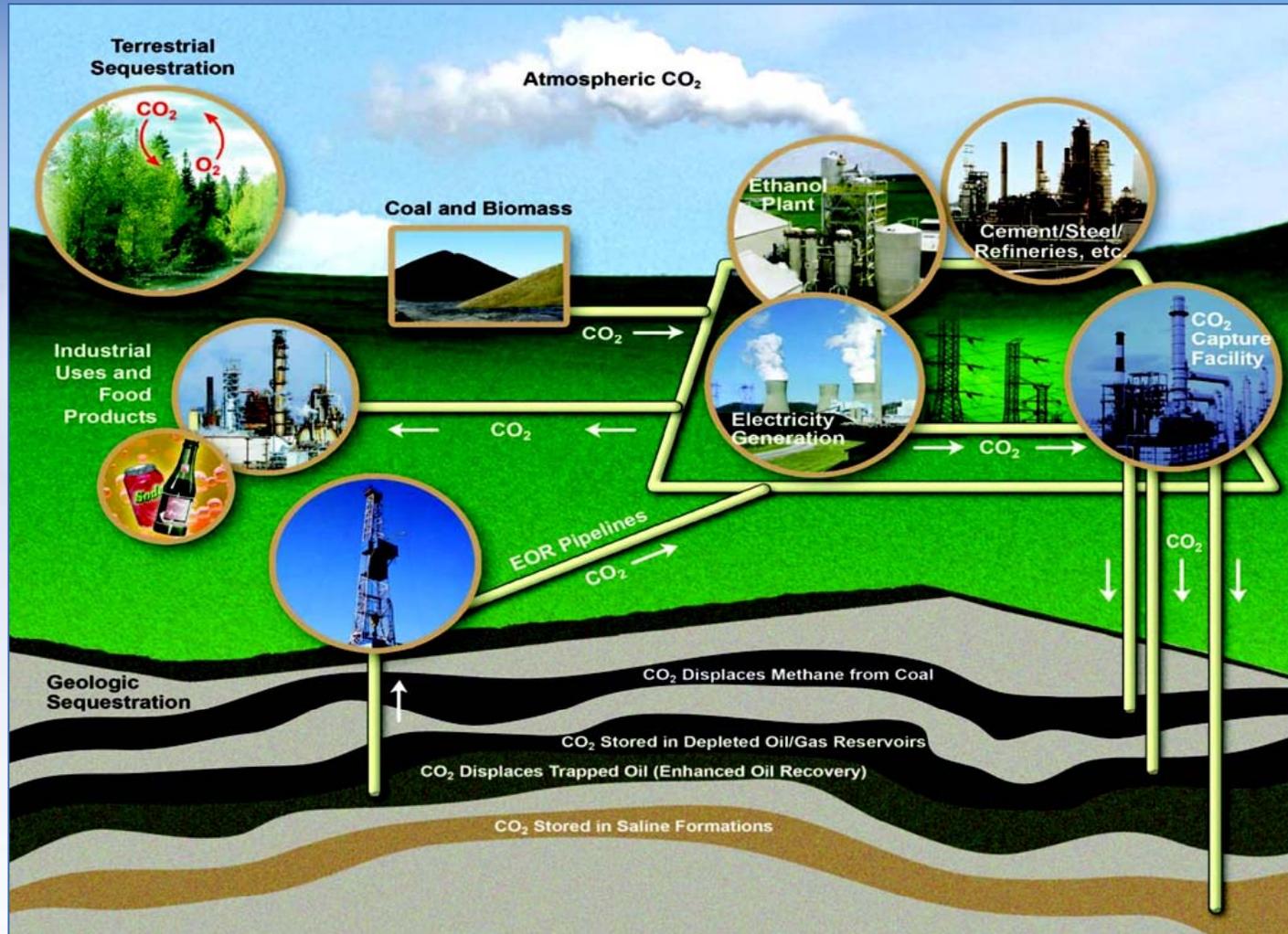


# Re-Use of Carbon Dioxide

## (energy efficiency considerations)

- Enhanced oil recovery (EOR) with CO<sub>2</sub> sequestration (storage)
- Enhanced gas recovery (EGR) with CO<sub>2</sub> storage
- Manufacture of chemicals (e.g., urea, methanol, etc.)
- Carbonated beverages
- Refrigeration medium and dry-ice refrigerant
- Algae-based bio-diesel fuels
- Algae-based bio-mass fuel
- Algae-based fish-food
- Ammonia-based fertilizers
- Other methods to re-use the CO<sub>2</sub> (e.g., propellants, health care, cast molds, transport fluid, etc.)

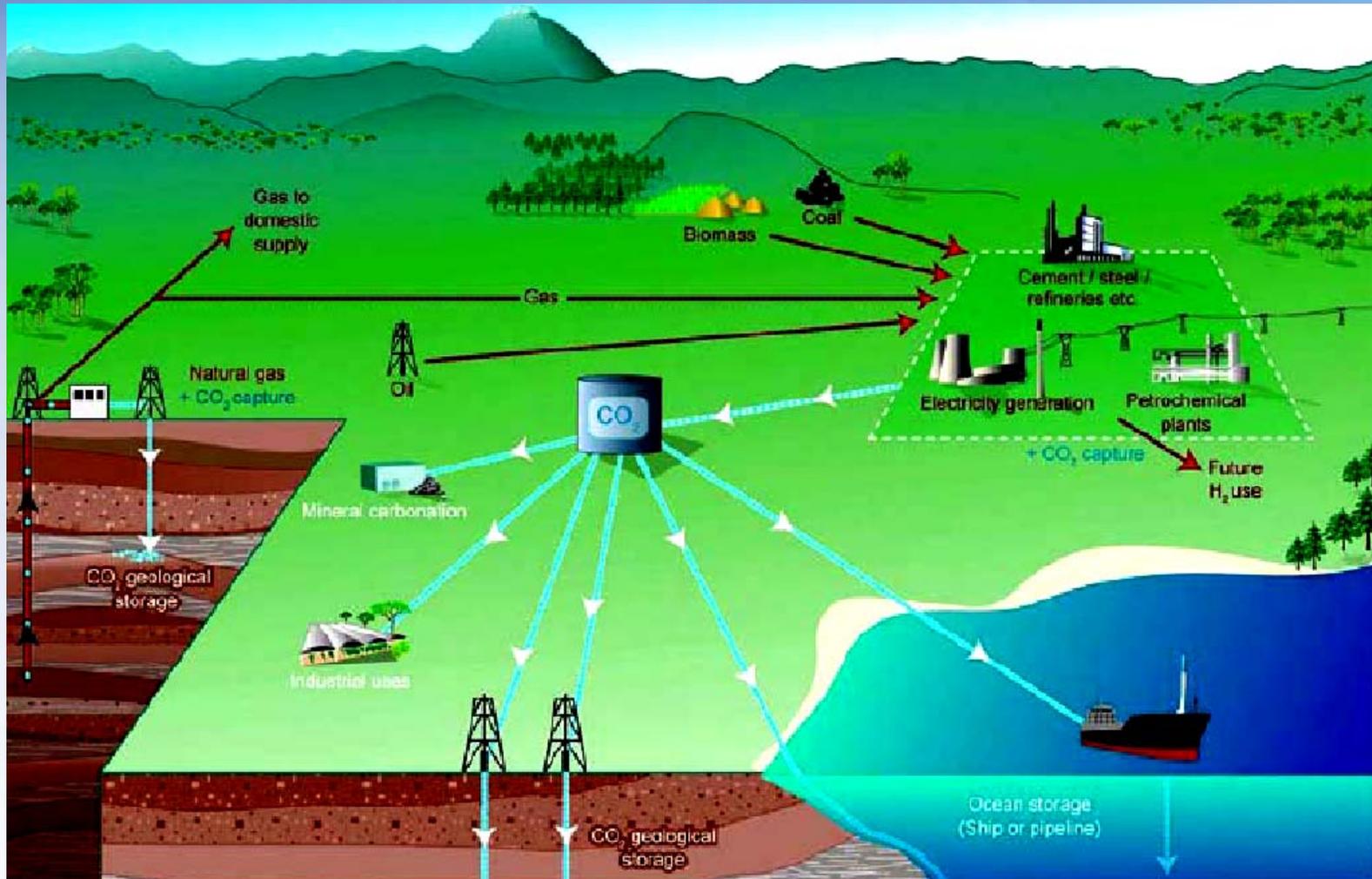
# Carbon Capture and Storage (CCS) Options



US DOE

# Carbon Dioxide Storage Options

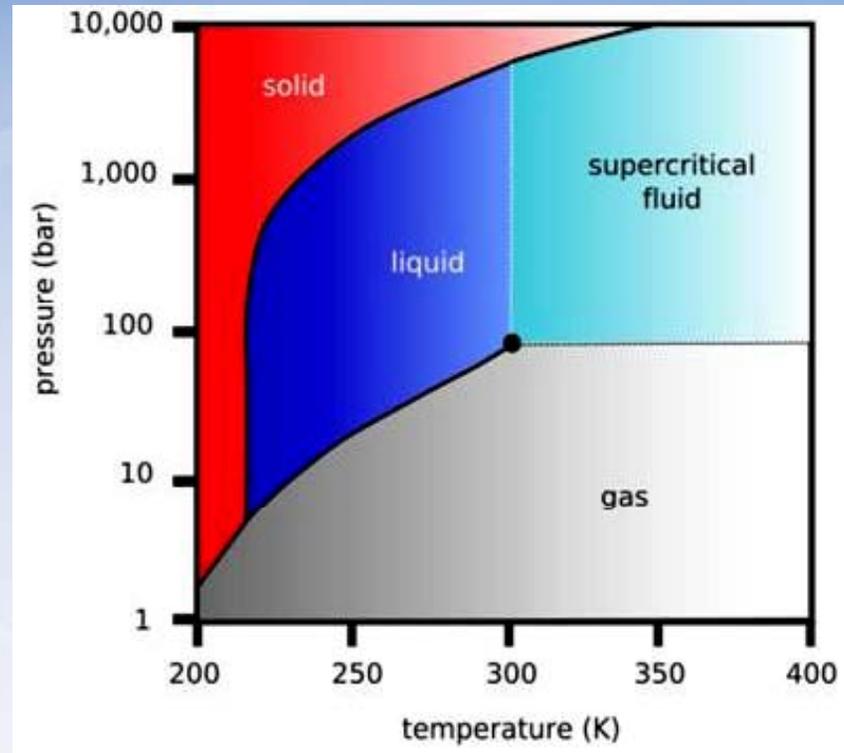
(each option has its own energy efficiency issues)



IPCC Special Report, Carbon Dioxide Capture and Storage, Technical Summary

# Carbon Dioxide Phases

Pure CO<sub>2</sub> can exist as a gas, liquid, or solid depending on its pressure and temperature.



Phase Diagram for CO<sub>2</sub>

- Carbon dioxide exists in four phases: gas, liquid, solid, and supercritical.
- Supercritical is important as CO<sub>2</sub> acts both as a gas and a liquid.
- In the supercritical phase, CO<sub>2</sub> acts like a gas, but has the density of liquid.
- The supercritical phase occurs at 31°C (88°F) and at 73 atm (1,070 psi).

# Carbon Dioxide Properties

(ground level and deep earth)

(useful for design and predicting energy related parameters)

**CO<sub>2</sub> Properties at Two Different Nominal Representative Conditions**

Property P (bar), T(°C)	Depth in Earth (approximate)	Units	Brine	CO <sub>2</sub>
Density @ 201 bar and 60°C	2 km	kg/m <sup>3</sup>	1191	725
Density @ 1 bar and 10°C	0 km (ground level)	kg/m <sup>3</sup>	1205	1.9
Viscosity @ 201 bar and 60°C	2 km	10 <sup>-6</sup> Pa s	940	60
Viscosity @ 1 bar and 10°C	0 km (ground level)	10 <sup>-6</sup> Pa s	1800	14

«Carbon Capture and Sequestration, Integrating Technology Monitoring and Regulation,» edited by Elizabeth J. Wilson and David Gerard, published by Blackwell Publishing, 2007.

# Examples: CCS Demonstration Projects

(O&M experience, although not on pulverized coal applications)

## Weyburn



- Project launched in 1999
- Enhanced oil recovery
- Expected - 22 Million tonne CO<sub>2</sub>
- Dakota Gasification Company
- 320 km pipeline

## Sleipner



- Field on stream since 1996
- Contains 4 to 9.5% CO<sub>2</sub>
- Need to reduce to 2.5%
- Elf – amine technology
- CO<sub>2</sub> – saline aquifer injection

## In Salah



- Field on stream since 2004
- Largest dry gas field in Algeria
- Jointly operated with Statoil
- 1,200 km south of Algiers
- 1 Million tonne CO<sub>2</sub> / year

# Ongoing or Planned CCS Programs

(each program will develop valuable CCS experiences with regard to energy efficiency results)

United States

Japan

Canada

Germany

United Kingdom

China

Italy

Australia

Norway

Netherlands

United Arab Emirates

Finland

France

Denmark

Sweden

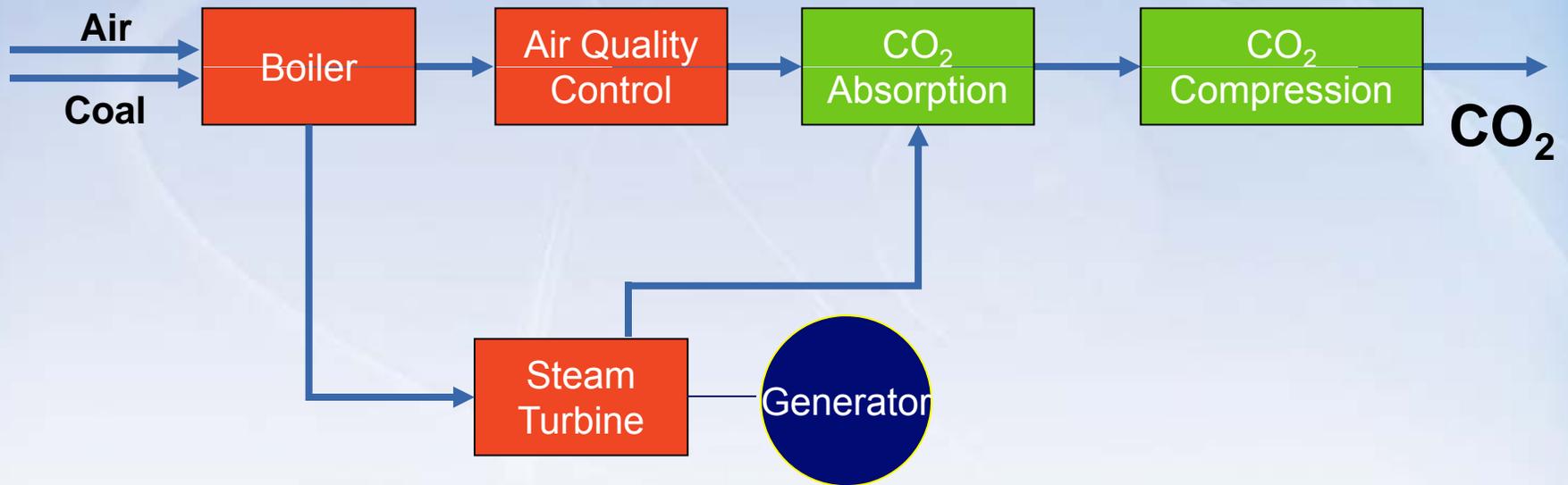
Belgium

Spain

Other

# Impact of Air Quality Systems on Fossil Power Plant and Carbon Capture Systems Energy Efficiency Issues

# Coal – Fired Power Plant Post-Combustion CO<sub>2</sub> Capture



# Air Quality Control Systems (AQCS) for Carbon Capture Ready (CCR) Fossil fired Power Plants

- AQCS primary purpose is to clean the flue gas to meet environmental stack emission limits
- Most CO<sub>2</sub> capture systems require (or can be optimized with) a relatively clean gas stream (e.g., PM, SO<sub>2</sub>, HCl, NO<sub>x</sub>, Hg, etc.)

# Air Quality Control Systems (AQCS) for Carbon Capture Ready Fossil Fired Power Plants

(energy efficiency considerations)

- Nitrogen Oxides ( $\text{NO}_x$ )
- Particulate Matter (PM)
- Sulfur Dioxide ( $\text{SO}_2$ )
- Sulfur Trioxide ( $\text{SO}_3/\text{H}_2\text{SO}_4$ )
- Mercury (Hg)
- HAPs (future MACT, including HCl)

# Air Quality Control Systems for CO<sub>2</sub> Capture & Storage (CCS) Systems

(energy efficiency issues)

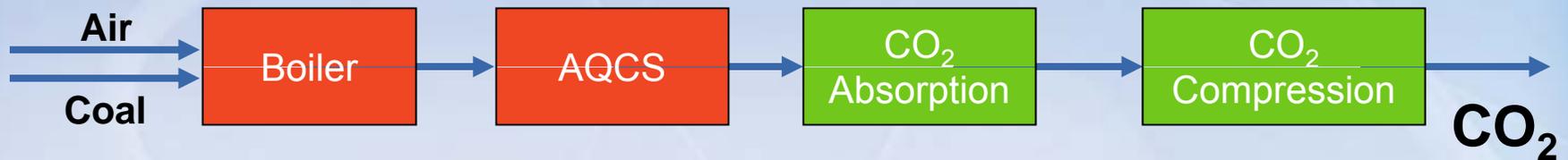
- The potential benefits of AQCS on CCS include:
  - optimized energy efficiency,
  - reduced operation & maintenance (O&M) costs of CCS,
  - decreased equipment size and real estate of CCS system,
  - decreased installed capital cost of CCS,
  - improvement in reliability of CCS operation.
- **Question:** Does the CCS system require additional gas cleaning beyond what the CO<sub>2</sub> Capture Ready (CCR) power plant AQCS has already provided (e.g., upgraded FGD, CCS deep FGD, reduced PM, flue gas cooling, etc.)?

# Stack Flue Gas Composition after AQCS and Post-Combustion CO<sub>2</sub> Capture

(energy efficiency issues)

- AQCS significantly reduces stack emissions (e.g. NO<sub>x</sub>, PM, SO<sub>2</sub>, SO<sub>3</sub>, H<sub>2</sub>SO<sub>4</sub>, HCl, and Hg).
- CO<sub>2</sub> capture system further reduces stack emissions, depending on % of total flue gas treated by CO<sub>2</sub> capture system (e.g., CCS bypass).
- CO<sub>2</sub> capture system may further lower the flue gas temperature (e.g., stack flue gas dispersion issues).
- Stack flue gas from CO<sub>2</sub> capture system is N<sub>2</sub>, O<sub>2</sub>, H<sub>2</sub>O, CO<sub>2</sub>, and trace components.
- CCS may have its own stack (depends on site specifics)

# Carbon Dioxide Product Composition from a CO<sub>2</sub> Capture System (AQCS and energy efficiency considerations)



Type of AQCS can influence the composition of the CO<sub>2</sub> product and byproducts produced from CO<sub>2</sub> capture system.

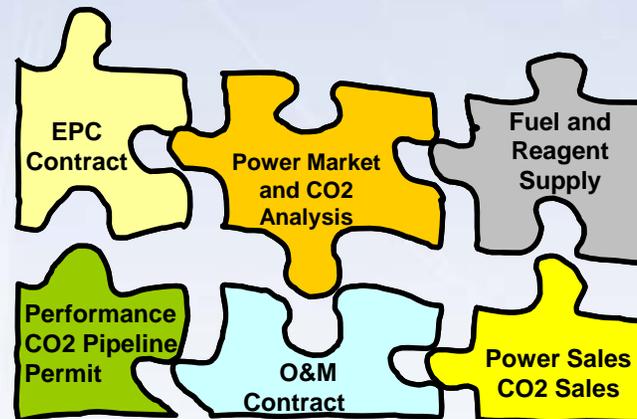
Liquid compressed CO<sub>2</sub> product from a CO<sub>2</sub> capture system consists of mostly CO<sub>2</sub>, some N<sub>2</sub>, and trace O<sub>2</sub>, H<sub>2</sub>O, and other components.

# Energy Efficiency, Economics and Managing Risk

# Project Economics and Managing Risks

(energy efficiency considerations are important, but not the only issue)

- Technology scale-up
- Installed capital cost (material and labor)
- Annual energy and operation & maintenance costs
- Carbon dioxide value or liability (\$/tonne, sale price, carbon credits, disposal cost, etc.) and disposition



# Process Parameters Influencing Energy Consumption of CO<sub>2</sub> Capture Systems

- Percent (%) of total flue gas that is treated
- Percent (%) removal of CO<sub>2</sub> removed from flue gas
- Total mass of CO<sub>2</sub> (tonnes/day) removed from flue gas
- Type of CO<sub>2</sub> capture process chosen
- Degree of flue gas pre-treatment (if required)
- Storage of CO<sub>2</sub> product

# Process Parameters Influencing Annual O&M and Energy Costs of CO<sub>2</sub> Capture Systems

- Total mass of CO<sub>2</sub> removed (tonnes/day) from flue gas
- Type of CO<sub>2</sub> capture process chosen
- Steam unit cost and usage rate
- Electricity unit cost and usage rate
- Cooling water unit cost and usage rate
- Reagent(s) unit cost and make-up rate
- Waste by-product(s) disposal cost
- Corrosion issues
- Solar flux, air humidity & temperature (e.g., algae process)
- O&M costs of flue gas pre-treatment (if required)
- Storage of CO<sub>2</sub> product
- Other issues

# Key Issues

## Energy Efficiency in CCS

- CO<sub>2</sub> capture system design **must** address energy issues.
- CO<sub>2</sub> capture technologies are available for pilot or demonstration
- CO<sub>2</sub> capture technology demonstration systems are being installed
- CO<sub>2</sub> capture process **greatly impacts** PC plant or NGCC power plant
- Long-term operating experience is needed (steady-state, load-following, & upset conditions)
- **Significant** cost issues (capital and annual O&M, including energy)
- CO<sub>2</sub> can be used in enhanced oil or gas recovery projects
- CO<sub>2</sub> storage projects (geological, saline, or depleted oil/gas reservoirs)
- New and/or improved power plant designs and CO<sub>2</sub> capture technologies being developed

# Summary

- Efficient electric power production technologies are available.
- CCS demonstration programs are being conducted, including addressing energy efficiency issues.
- New and/or improved power plants and CCS technologies are being developed.

# Contact Information

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***Thank You***



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