



Equipment Heat Loss



- Review Examples Of Process Heat Transfer To Equipment Not Classified As Heat Exchangers (Fired Or Non-fired)
- Look At Ways To **Input** Heat To Equipment For Process Heat Transfer
- Identify Heat Transfer **Formulas** For Equipment Process Heat Transfer



- **Prevent Condensing (Gas/Vapor Service)**
 - Condensed Liquid May Cause Corrosion
 - Condensed Liquid May Create Downstream Operating Problems
- **Prevent Solidification (Liquid Service)**
 - Prevent Mechanical Damage To Pipe And Equipment Due To Freezing (Water Services)
 - Maintain Liquid State To Ensure Hydraulic Transfer
- **Viscosity Control**



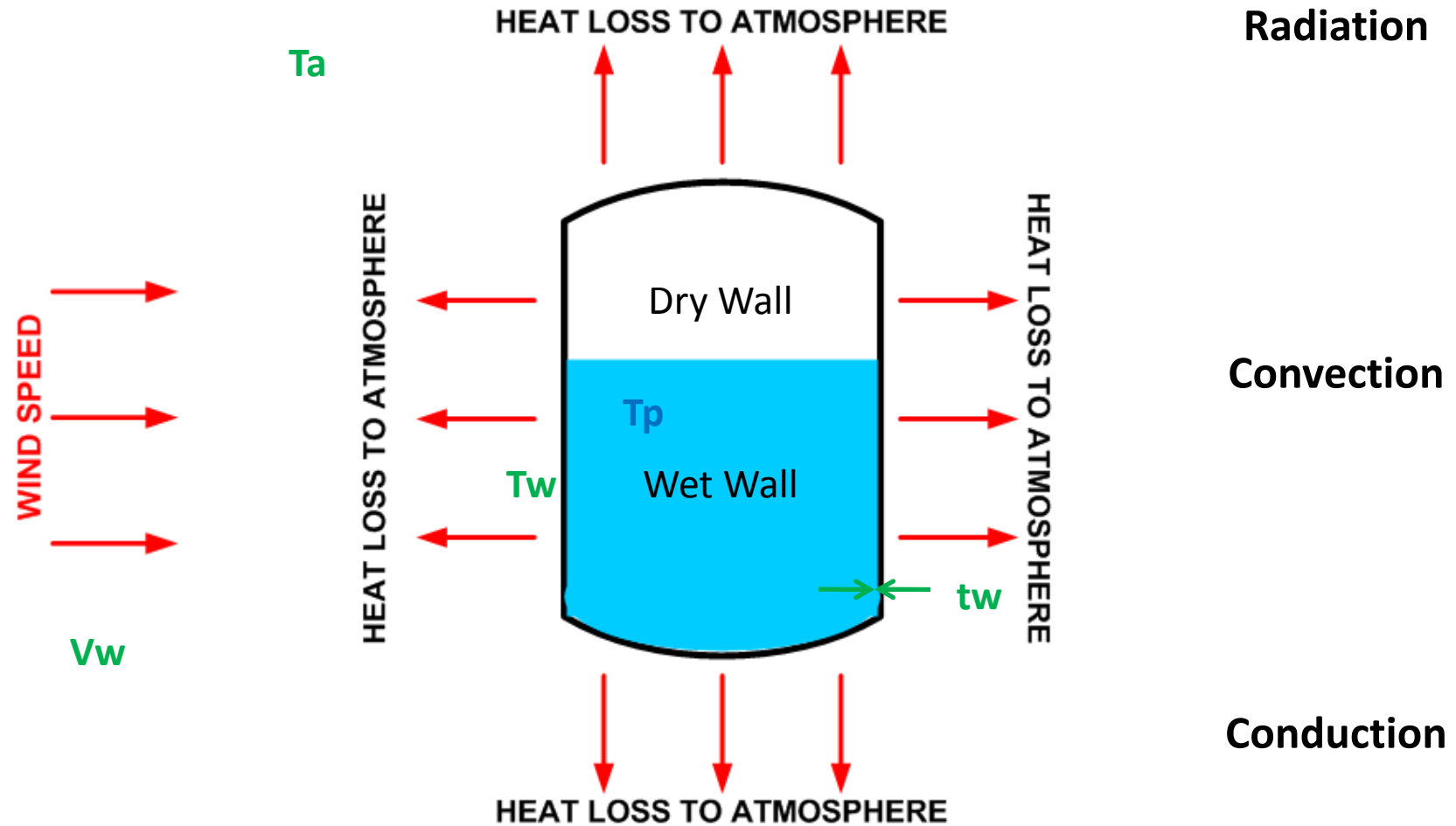
- **Heat Transfer To Change**
 - Fluid Temperature
 - Fluid State (Phase Change)
 - Fluid Properties
- **Heat Transfer To Process (Heating)**
- **Heat Transfer From Process (Cooling)**

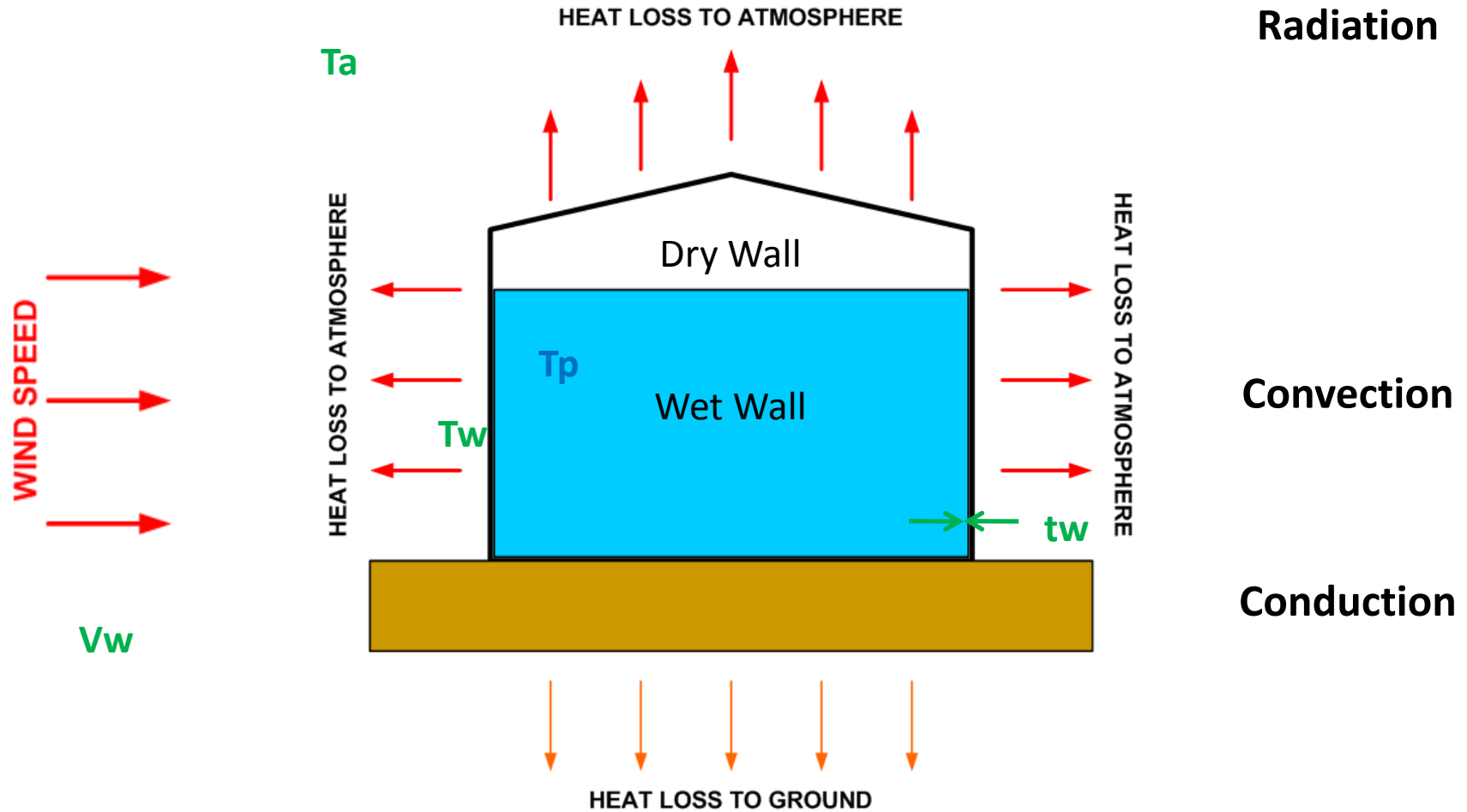


Equipment Heat Loss



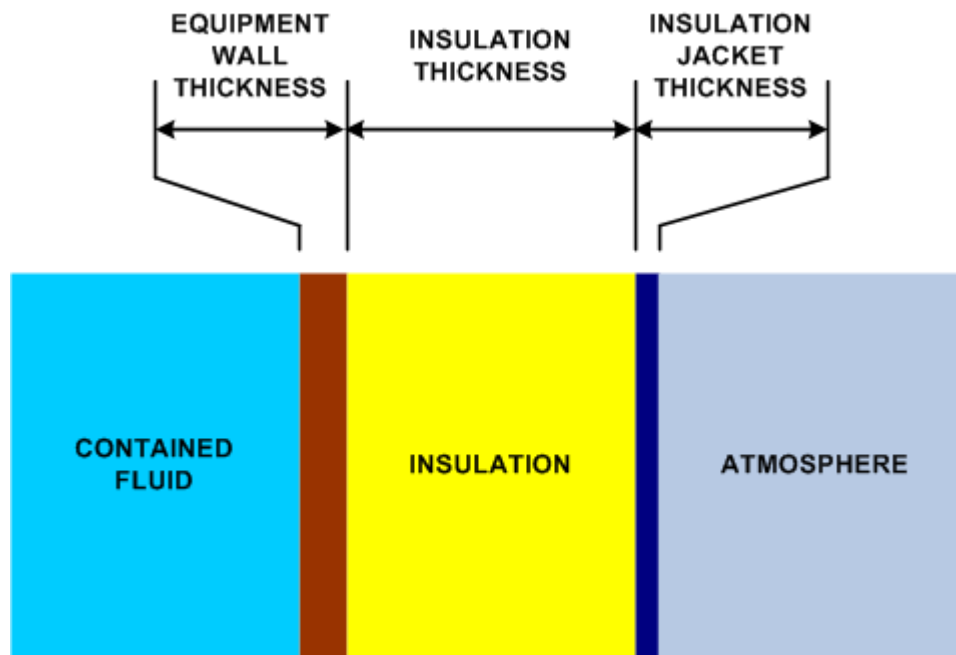
- **CONDUCTION** – Heat Loss Directly Through Equipment Materials And Materials In Contact With Equipment
- **CONVECTION** – Heat Loss Indirectly Through Fluid Boundary Layer at Equipment Or Insulation Surface
- **RADIATION** – Heat Loss Through Energy Wave Emission At Surface Exposed To Atmosphere





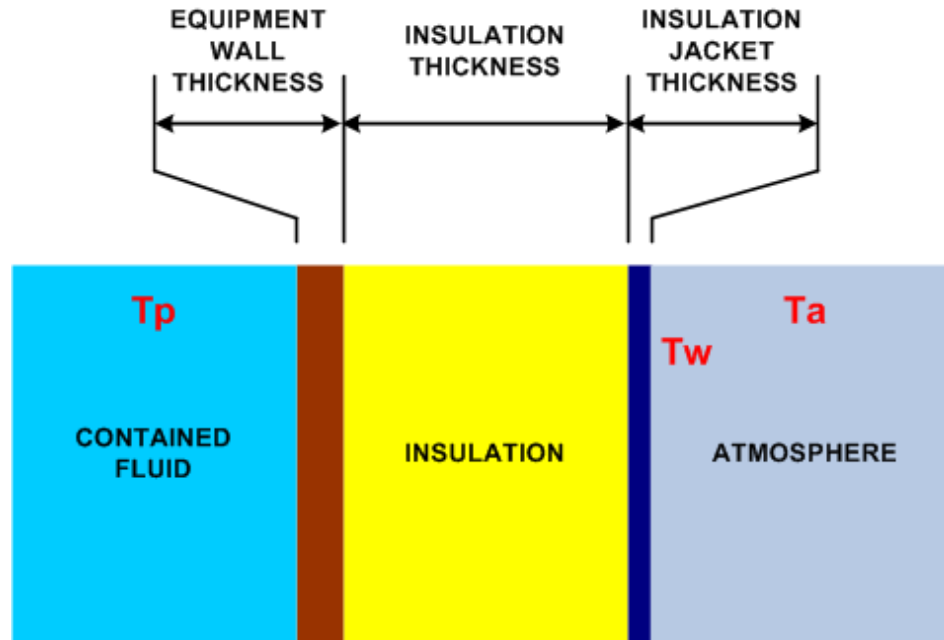


Equipment Heat Loss





Equipment Heat Loss



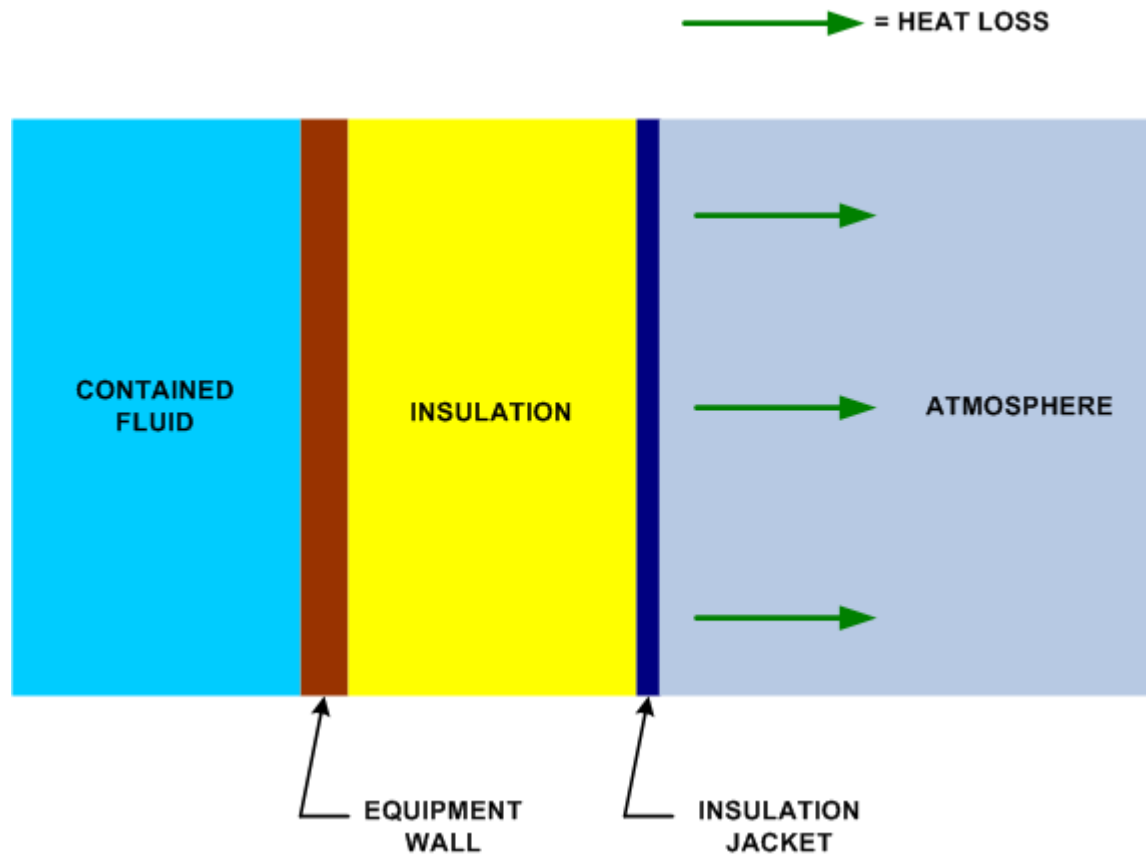
T_p = Process Temperature (°F)

T_w = Surface Temperature (°F)

T_a = Ambient Temperature (°F)

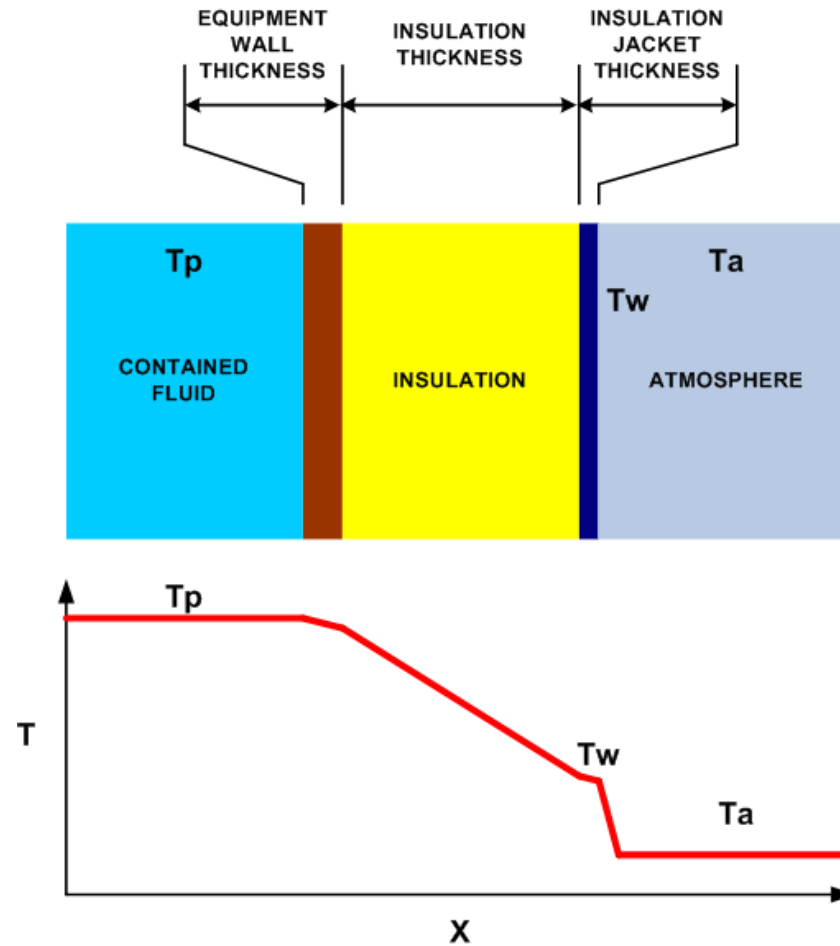


Equipment Heat Loss





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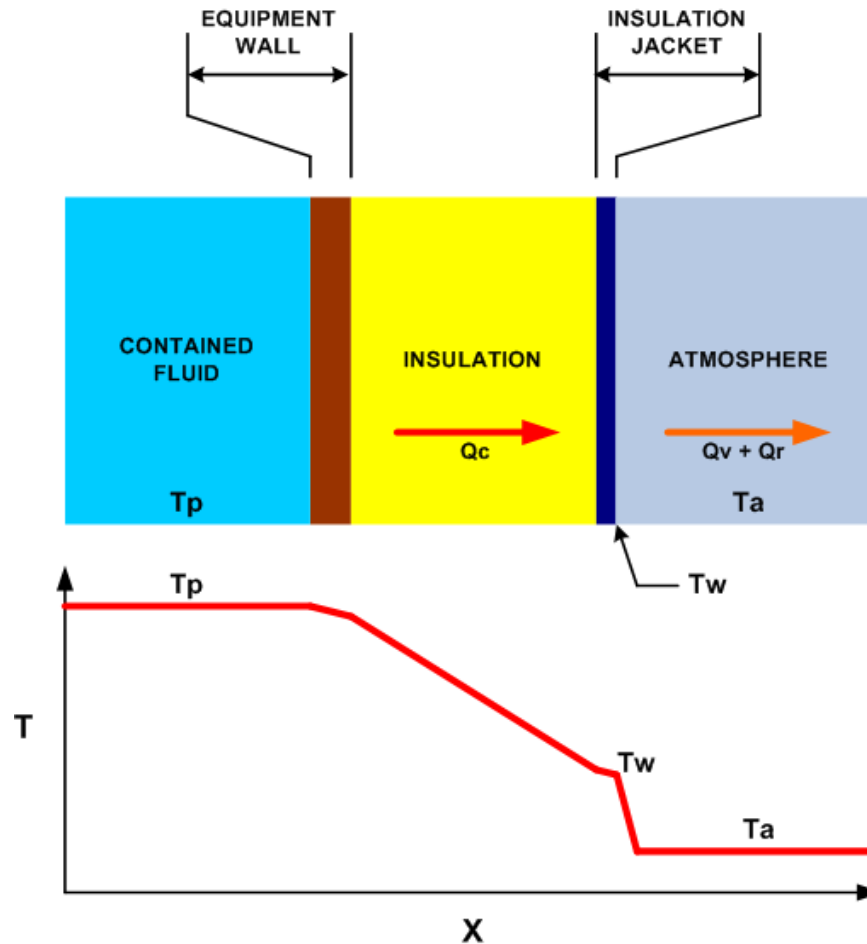




Q_c = Conduction Heat Transfer
(Insulation)

Q_v = Convection Heat Transfer
(Jacket To Atmosphere)

Q_r = Radiation Heat Transfer
(Jacket To Atmosphere)





**1/hc =
Insulation Thickness/
Insulation Thermal
Conductivity**

$$Q = \frac{1}{1/hc + 1/ha} * A * (Tp - Ta)$$

Q = Heat Transfer Rate (Btu/hr)

hc = Conduction Heat Transfer Coefficient (Btu/hr/ft²/°F)

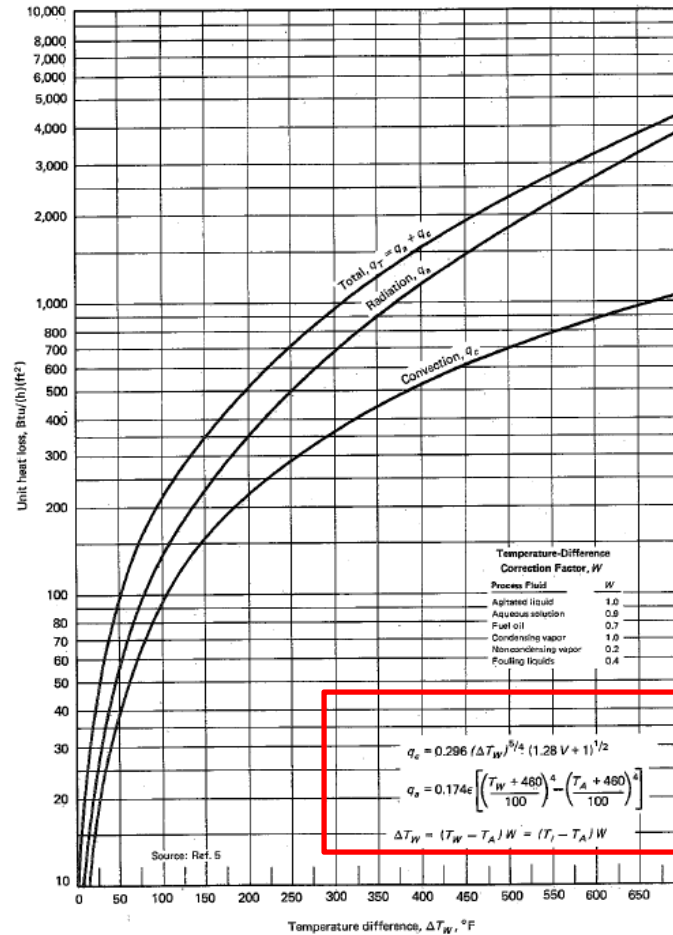
ha = Atmospheric Heat Transfer Coefficient (Btu/hr/ft²/°F)

**ha =
hv + hr
= Convection Coefficient
+ Radiation Coefficient**

A = Area (ft²)

Tp = Process Temperature (°F)

Ta = Atmospheric Temperature (°F)



Insulation Saves Energy – Chemical Engineering, 05/27/74



Convection Coefficient

$$h_{ac} = 0.296 * (T_w - T_a)^{1/4} * (1.28 * V_w + 1.0)^{1/2}$$

h_{ac} = Convection Coefficient (Btu/hr/ft²/°F)

T_w = Surface Temperature (°F)

T_a = Ambient Temperature (°F)

V_w = Wind Speed (mph)

Radiation Coefficient

$$h_{ar} = 0.174 * E * \frac{(T_w'/100)^4 - (T_a'/100)^4}{(T_w - T_a)}$$

h_{ar} = Radiation Coefficient (Btu/hr/ft²/°F)

E = Emissivity

T_w' = Surface Absolute Temperature (°R)

T_a' = Ambient Absolute Temperature (°R)

T_w = Surface Temperature (°F)

T_a = Ambient Temperature (°F)

$$h_a = h_{ac} + h_{ar}$$

h_a = Atmospheric Coefficient (Btu/hr/ft²/°F)

h_{ac} = Convection Coefficient (Btu/hr/ft²/°F)

h_{ar} = Radiation Coefficient (Btu/hr/ft²/°F)

Atmospheric Coefficient



Wind Speed mph	Surface Temperature °F	Ambient Temperature °F	hac Btu/hr/ft ² /°F
0	100	20	0.89
0	200	20	1.1
10	100	20	3.3
10	200	20	4.0
20	100	20	4.6
20	200	20	5.6
30	150	20	6.3
40	150	20	7.2



Emissivity	Surface Temperature °F	Ambient Temperature °F	har Btu/hr/ft ² /°F
0.50	100	20	0.49
0.50	200	20	0.66
0.70	100	20	0.69
0.70	200	20	0.92
0.90	100	20	0.89
0.90	200	20	1.2
1.0	100	20	0.98
1.0	200	20	1.3



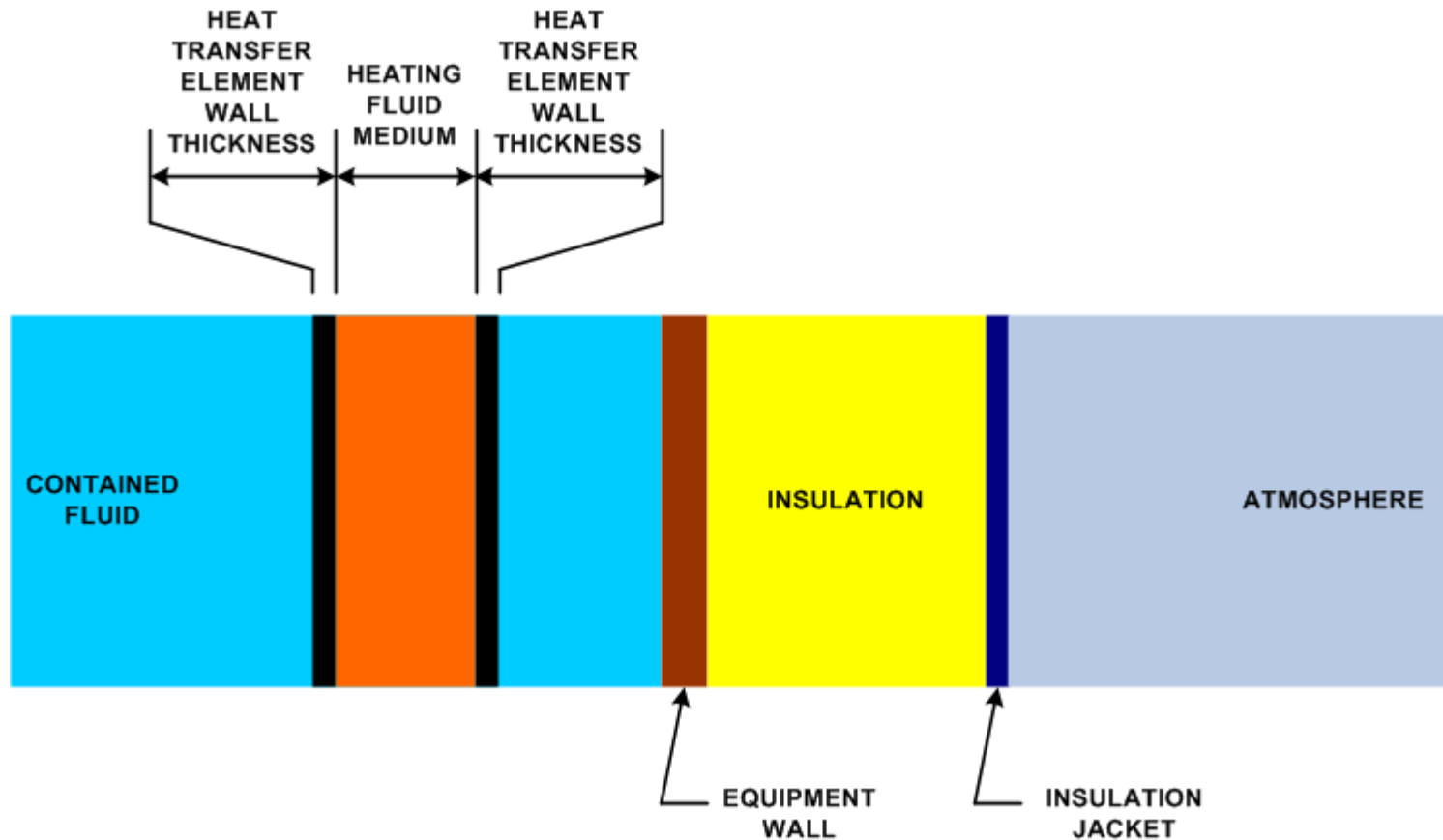
Equipment Heat Gain

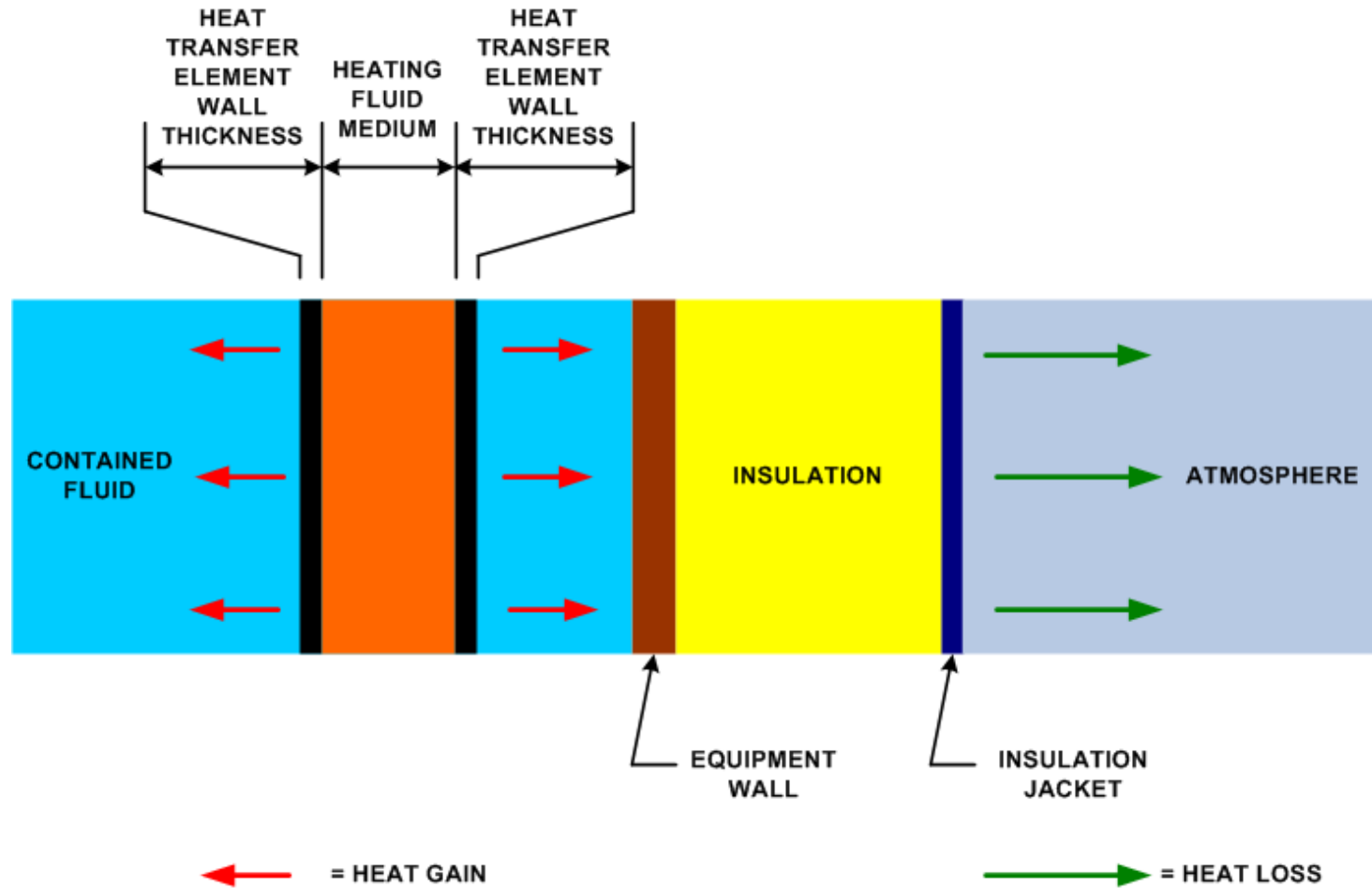


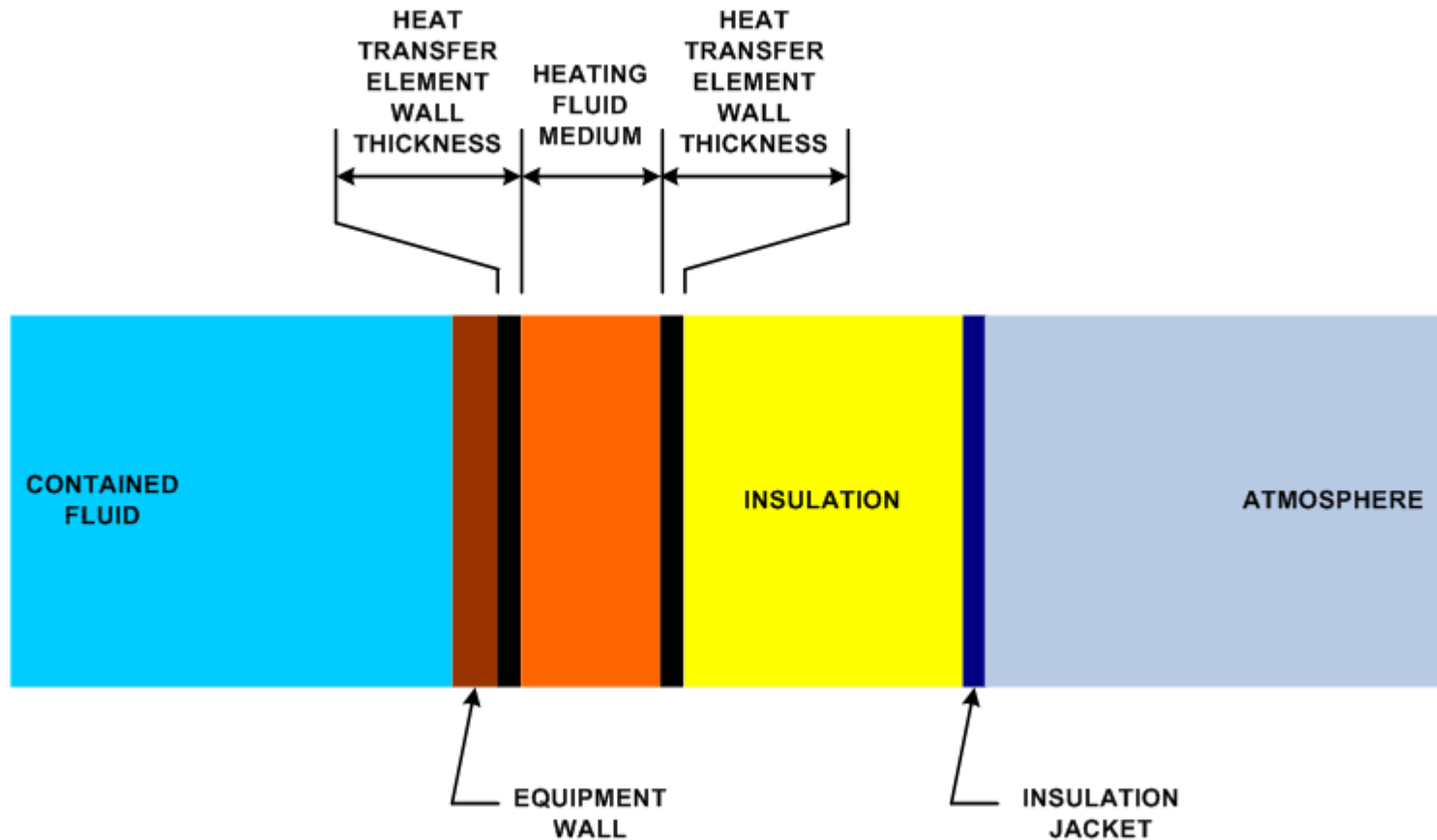
- **CONDUCTION** – Heat Transfer To Equipment Through Equipment Materials And Materials In Contact With Equipment
- **CONVECTION** – Heat Transfer At Fluid Boundary Layers Inside And Outside Of Equipment And Heat Exchange Attachments In Contact With Equipment

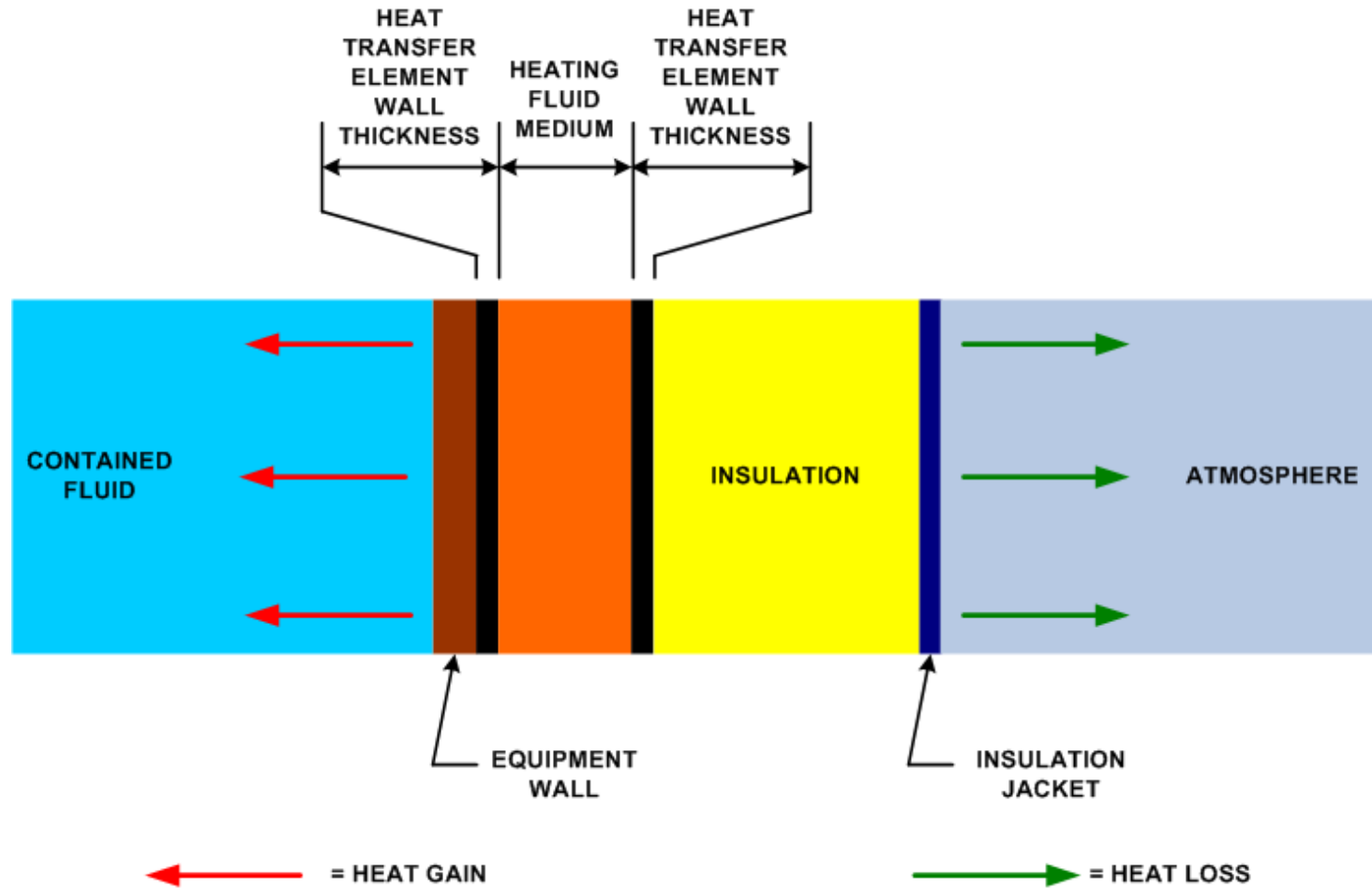


Internal Element











- Temperature Maintenance

Heat Gain = Heat Loss

- Process Heat Transfer

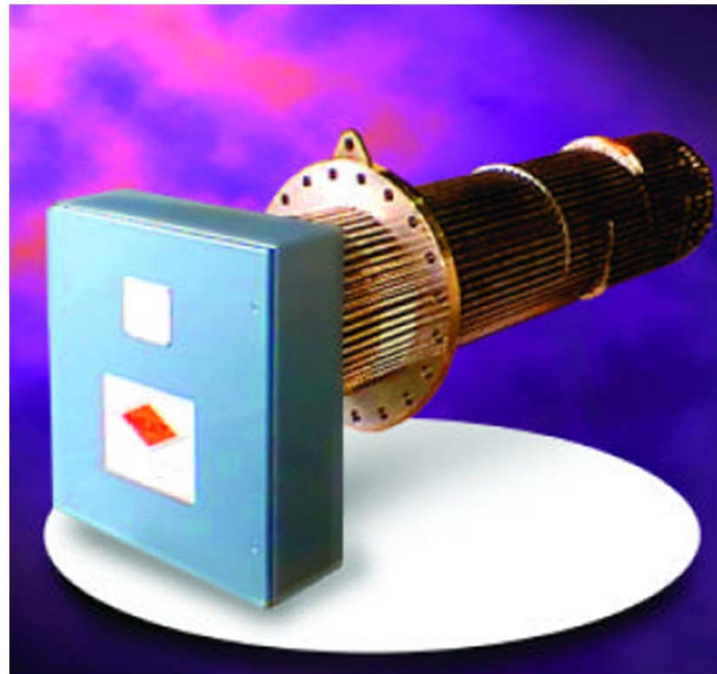
Heat Gain > Heat Loss



Equipment Heat Transfer Attachments



Option		Internal	External	Attached	Integral
Heat Exchange Insert	Bayonet Exchanger Pipe Coil Mixing Eductor Sparger	X			X
Jacket	Full Half Pipe		X		X
Tracers	Electric Pipe Tubing ControTrace		X	X	
Plate Coil			X	X	



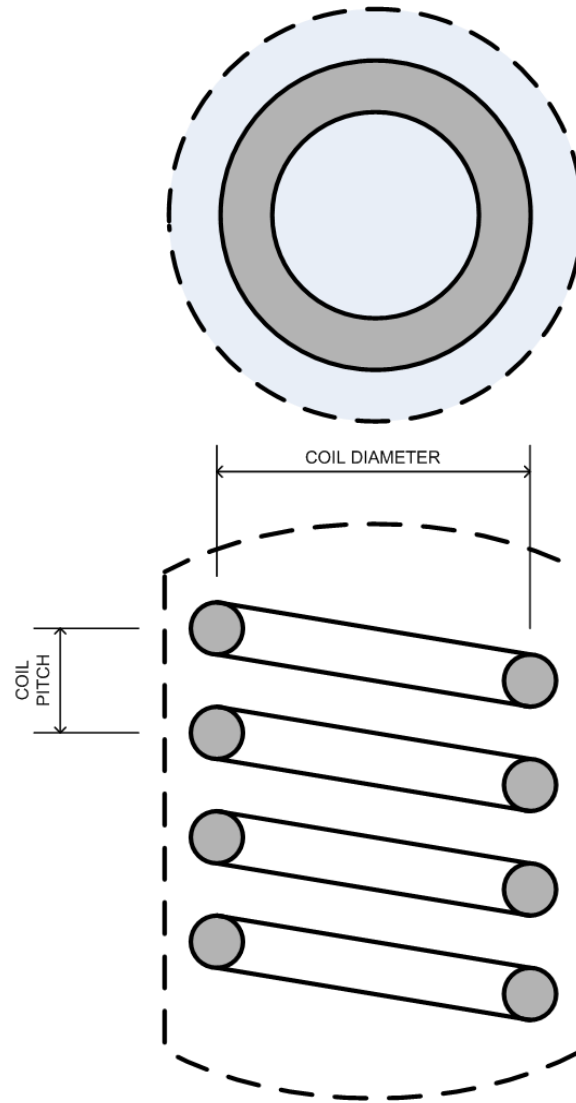
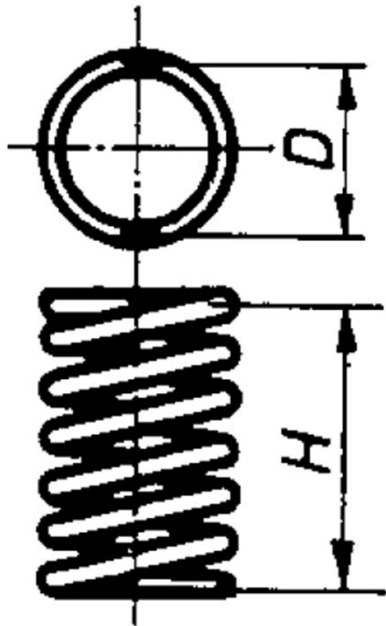


Internal – Tube Bundle



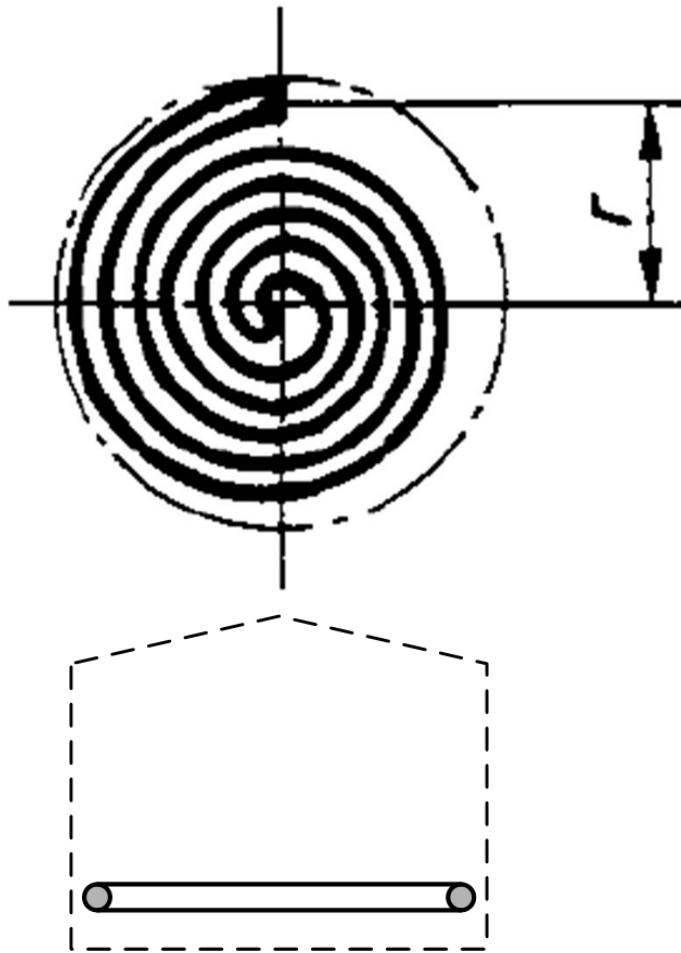


Internal - Helical Coil

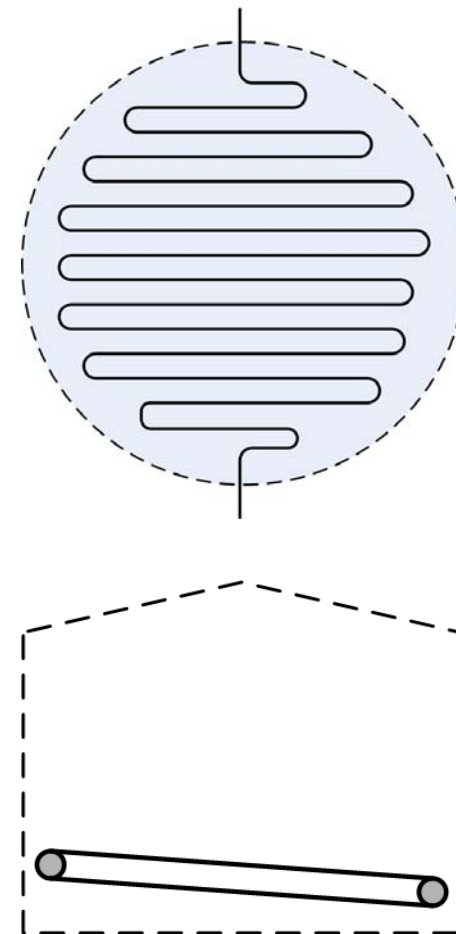




Spiral



Serpentine

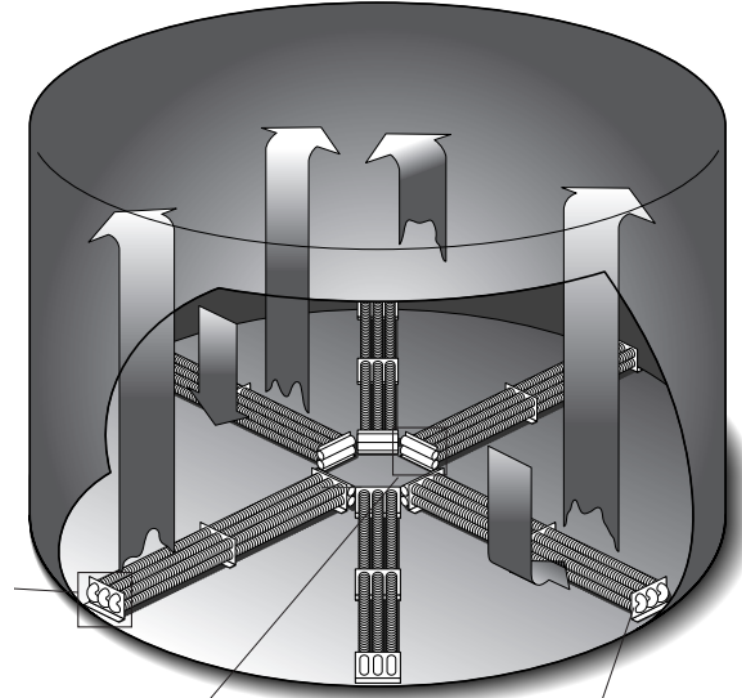




Koch TF

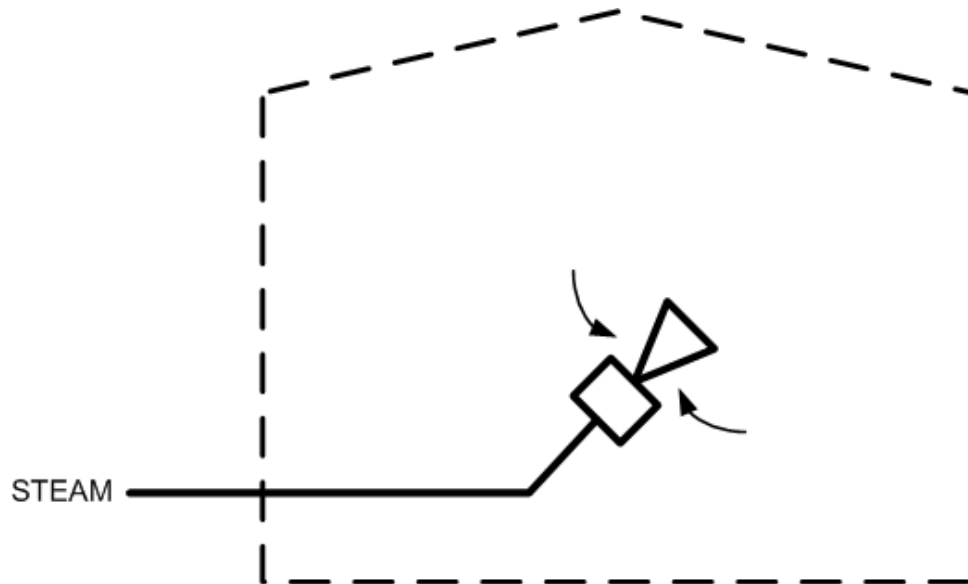


Armstrong BHC/BHS



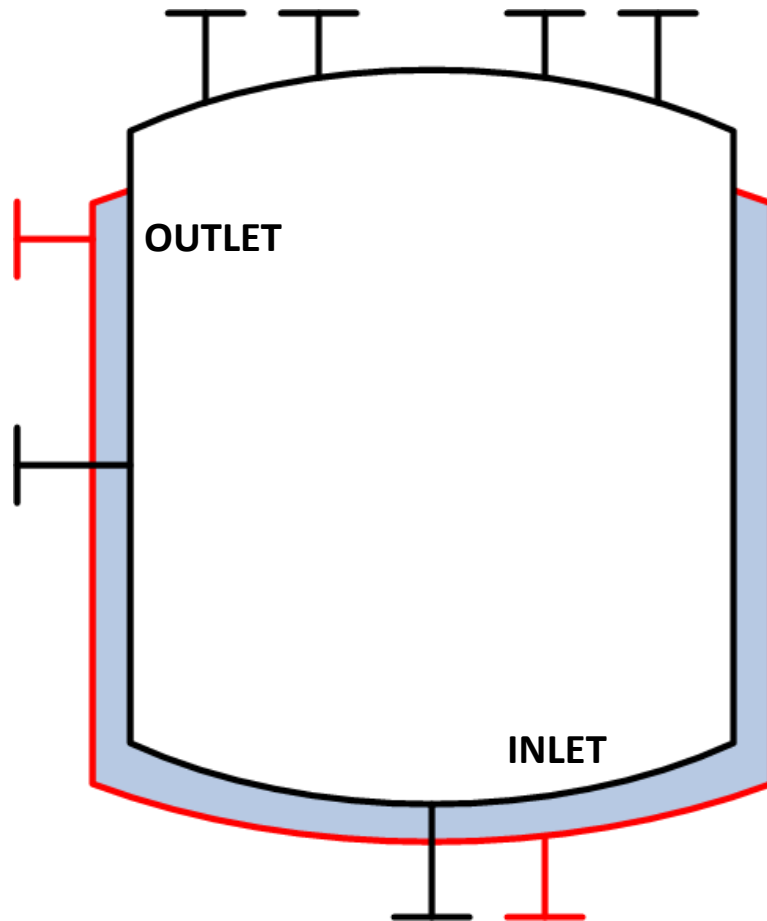


Internal – Mixing Eductor

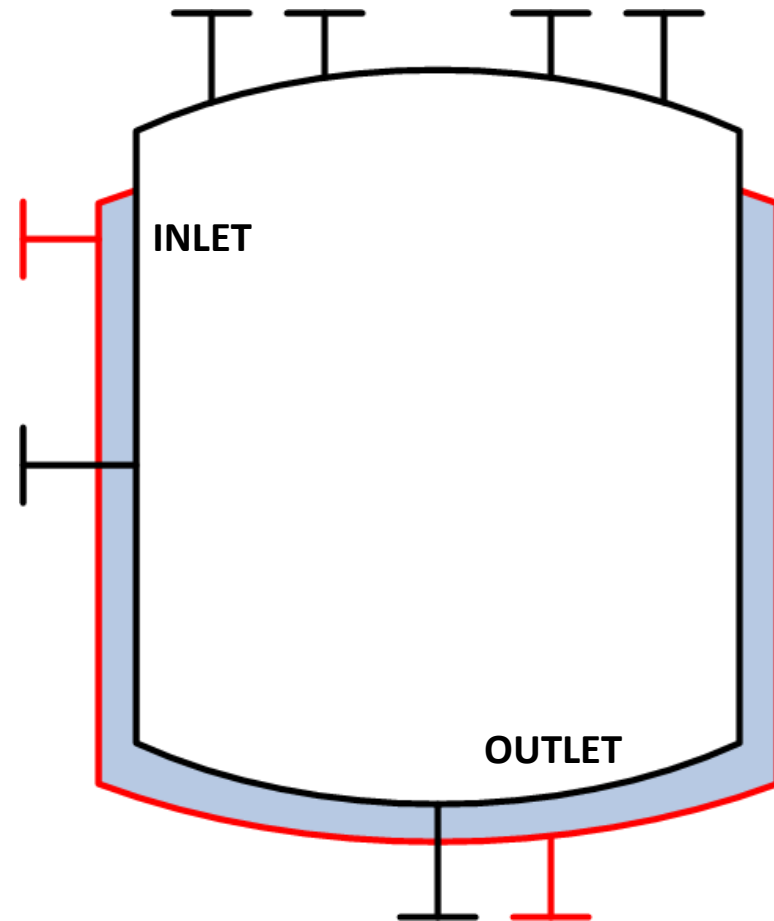




Liquid Service

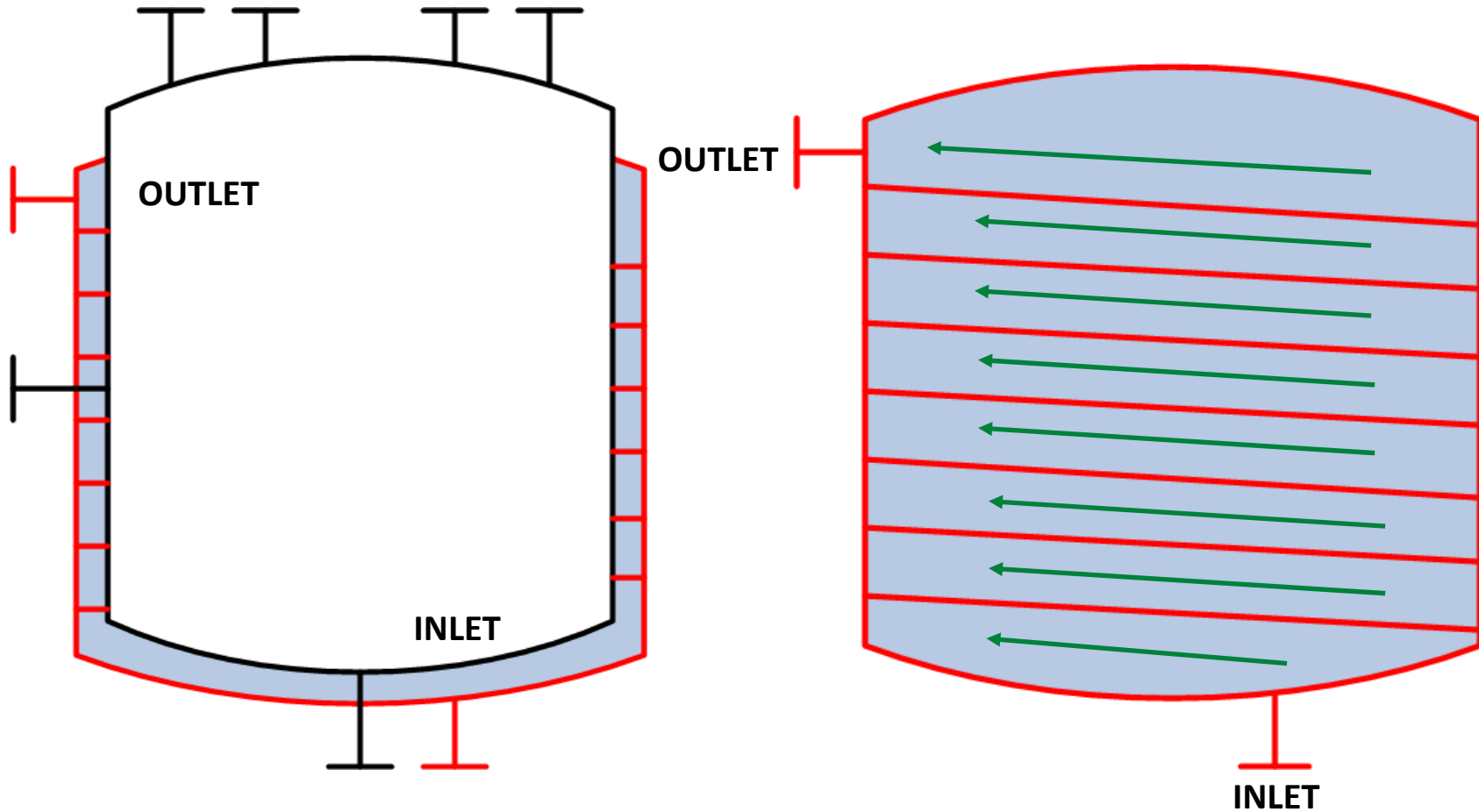


Steam Service



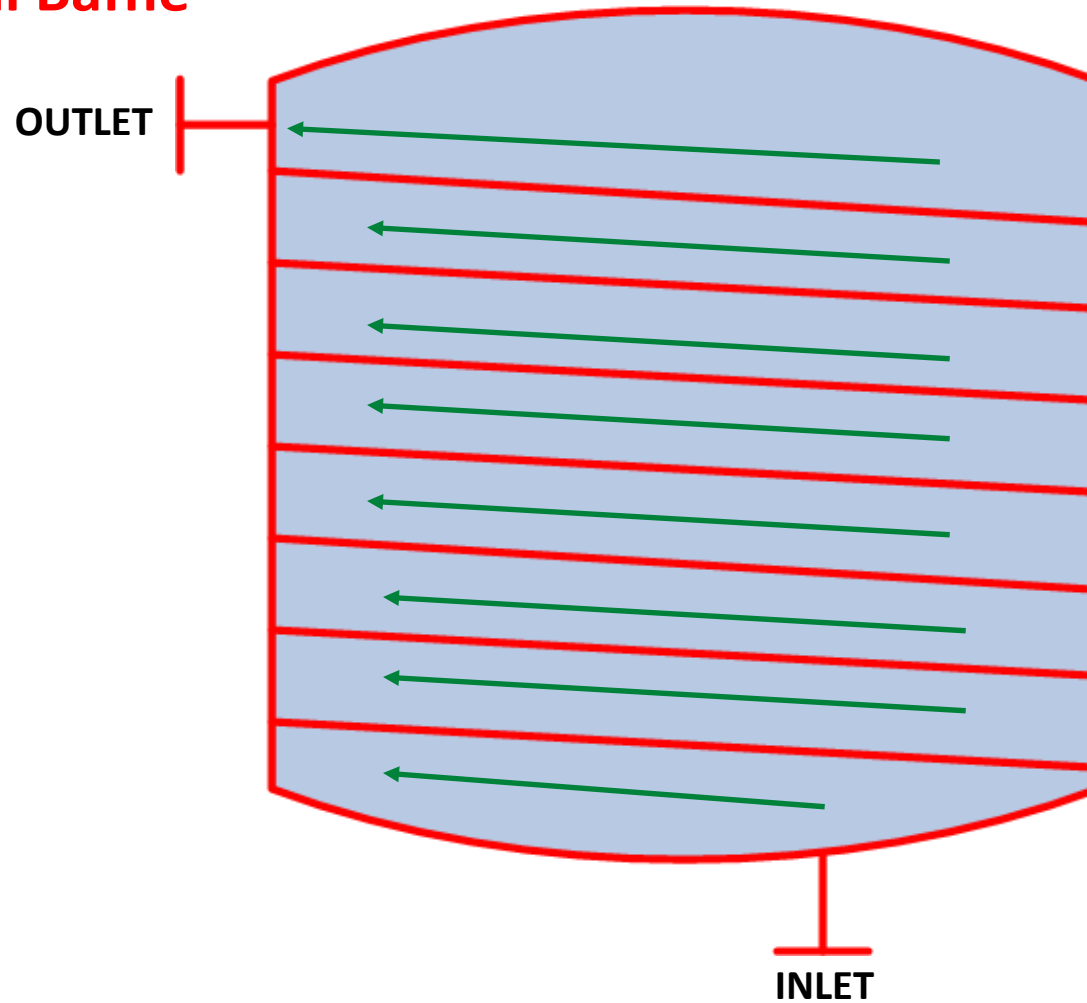


Spiral Baffle



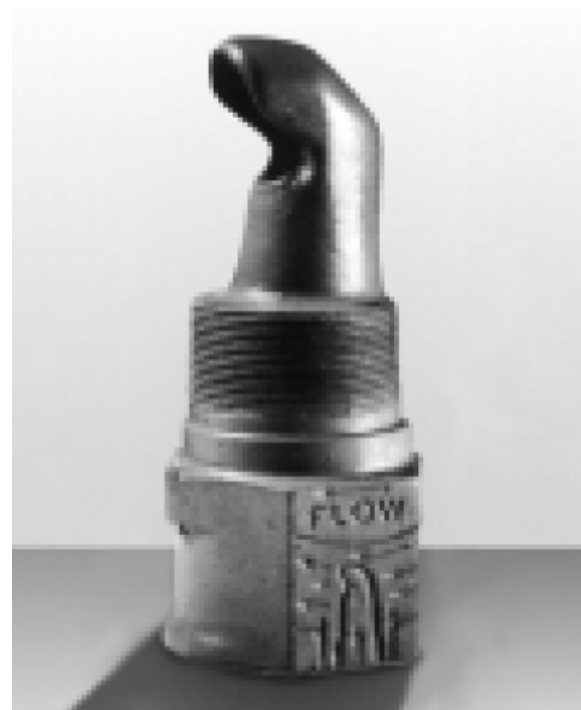
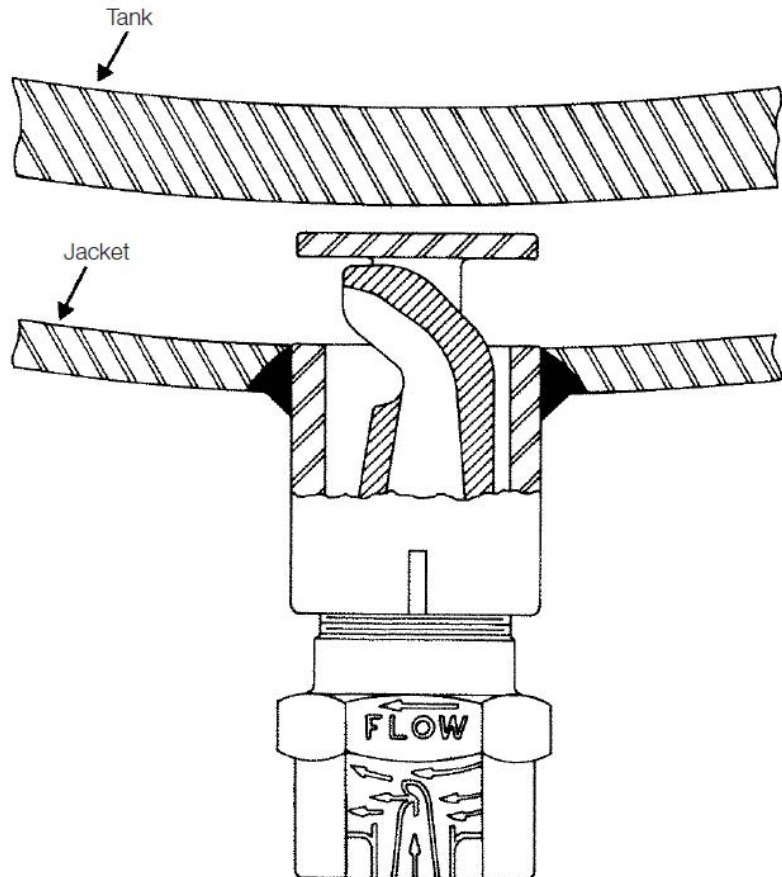


Spiral Baffle



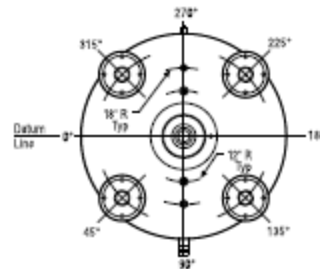
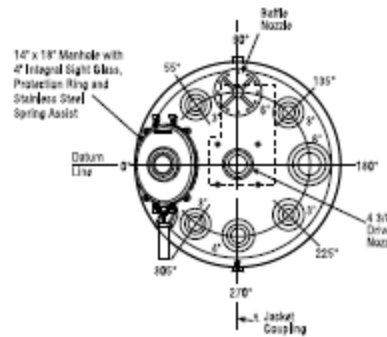
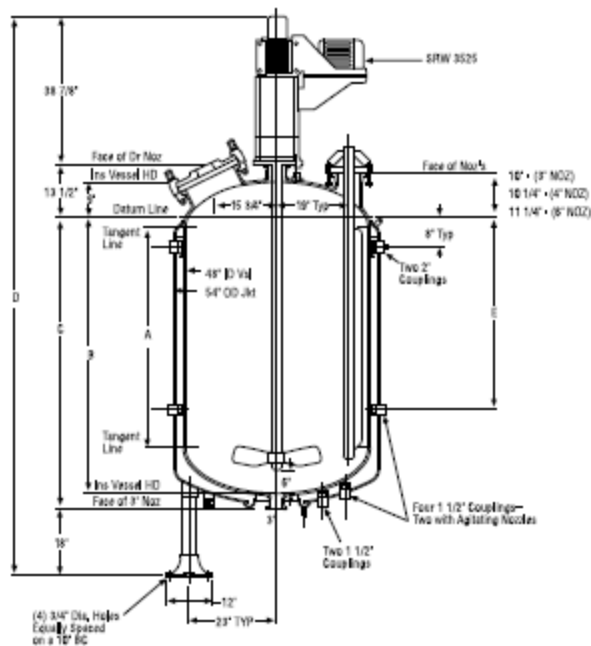


Pfaudler Agitating Nozzle





Pfaudler RS-48



HT Fluid: Water

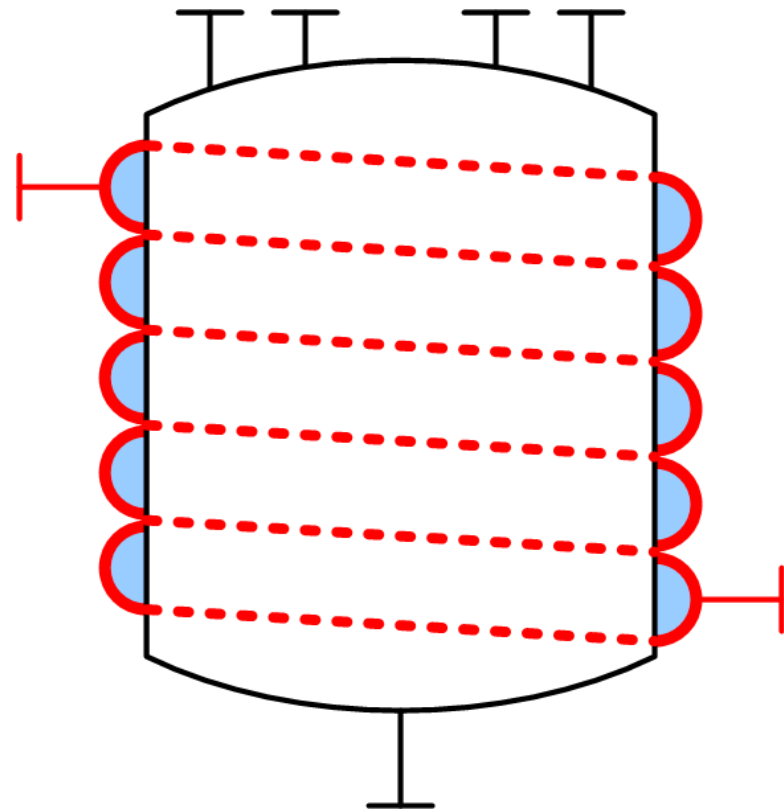
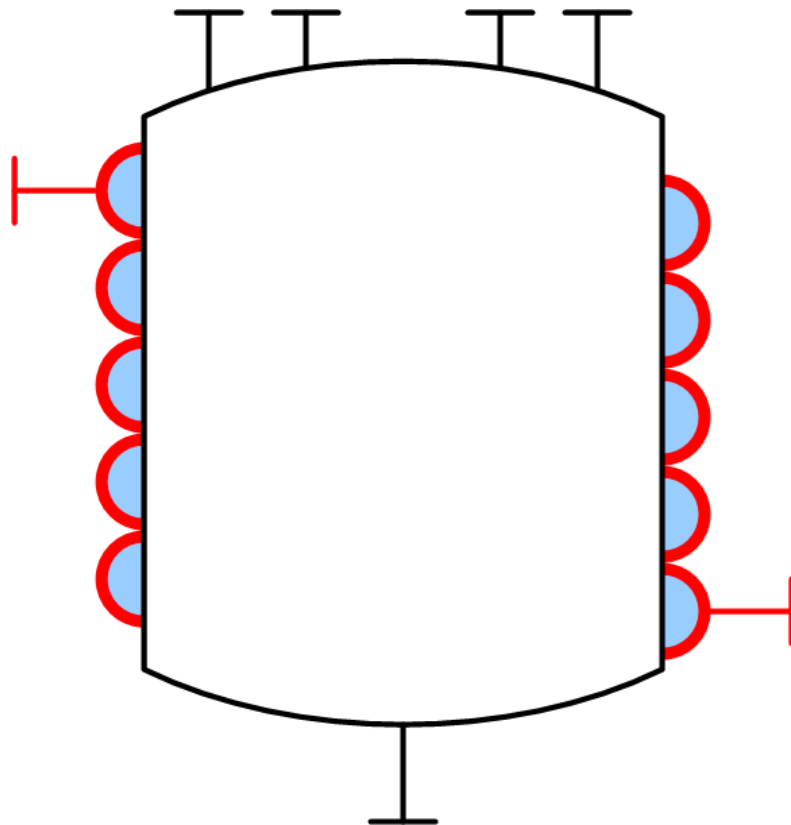
Nozzles Required: 2

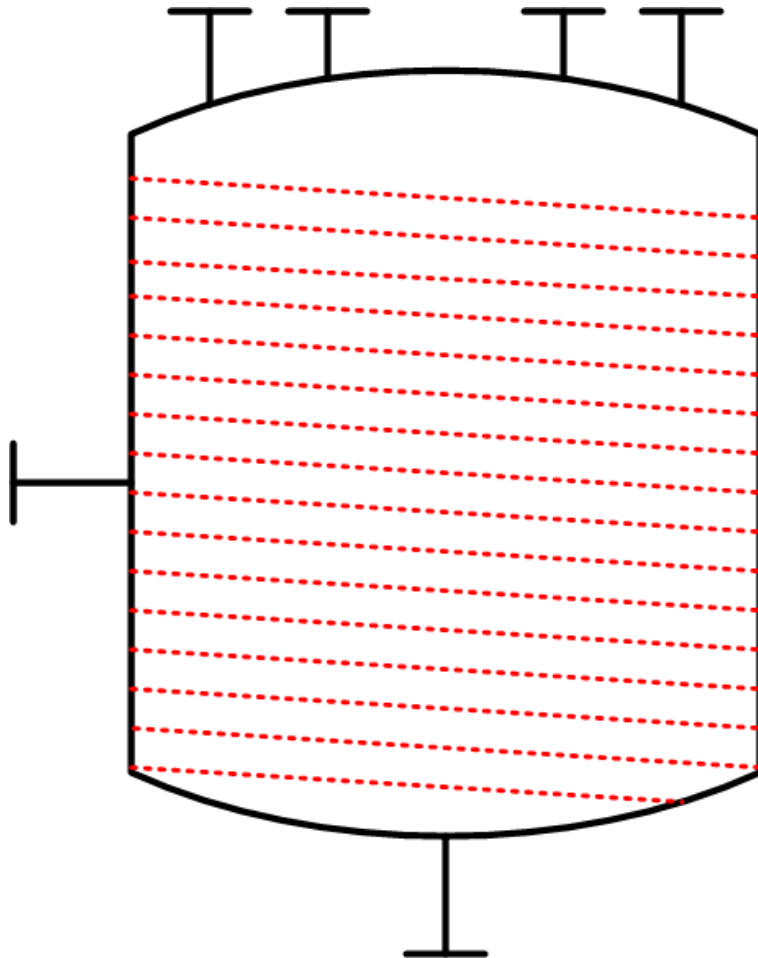
Nozzle Size: 1.5 in.

dP: 20 psi

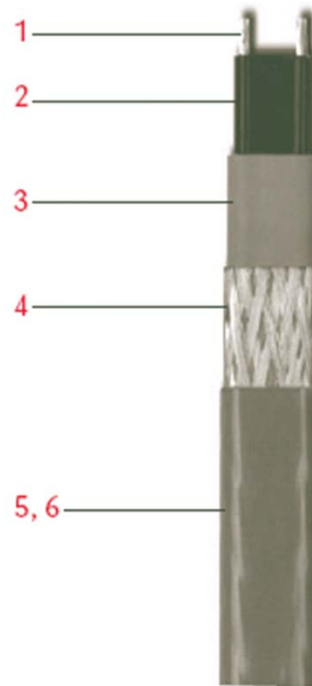
Total Flow: 68 gpm

hj = 548 Btu/hr-ft²-°F





Thermon BSX



Construction . . .

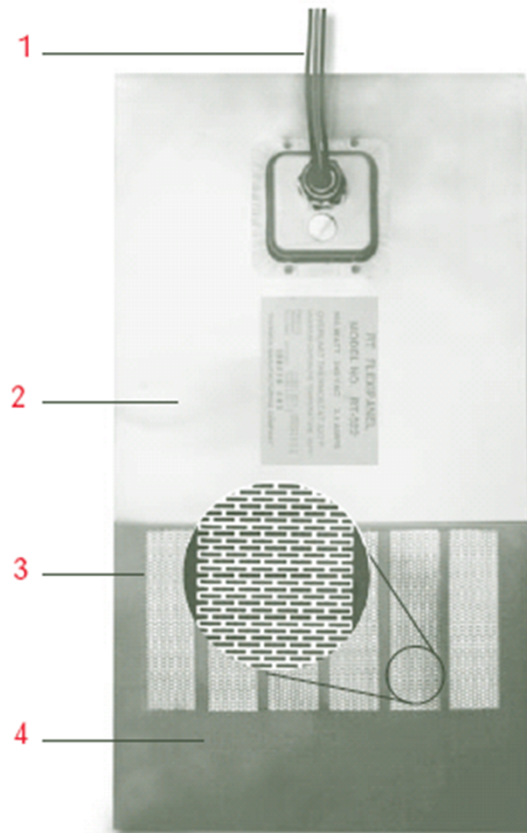
- 1 Nickel-Plated Copper Bus Wires (16 AWG)
- 2 Radiation Cross-Linked Semiconductive Heating Matrix
- 3 Radiation Cross-Linked Dielectric Insulation
- 4 Tinned Copper Braid
- 5 Polyolefin overjacket provides additional protection to cable and braid where exposure to aqueous inorganic chemicals is expected.

Options . . .

- 6 FOJ Fluoropolymer overjacket over tinned copper braid provides additional protection to cable and braid where exposure to organic chemicals or corrosives is expected.



Thermon RT Flexipanel



Construction³ . . .

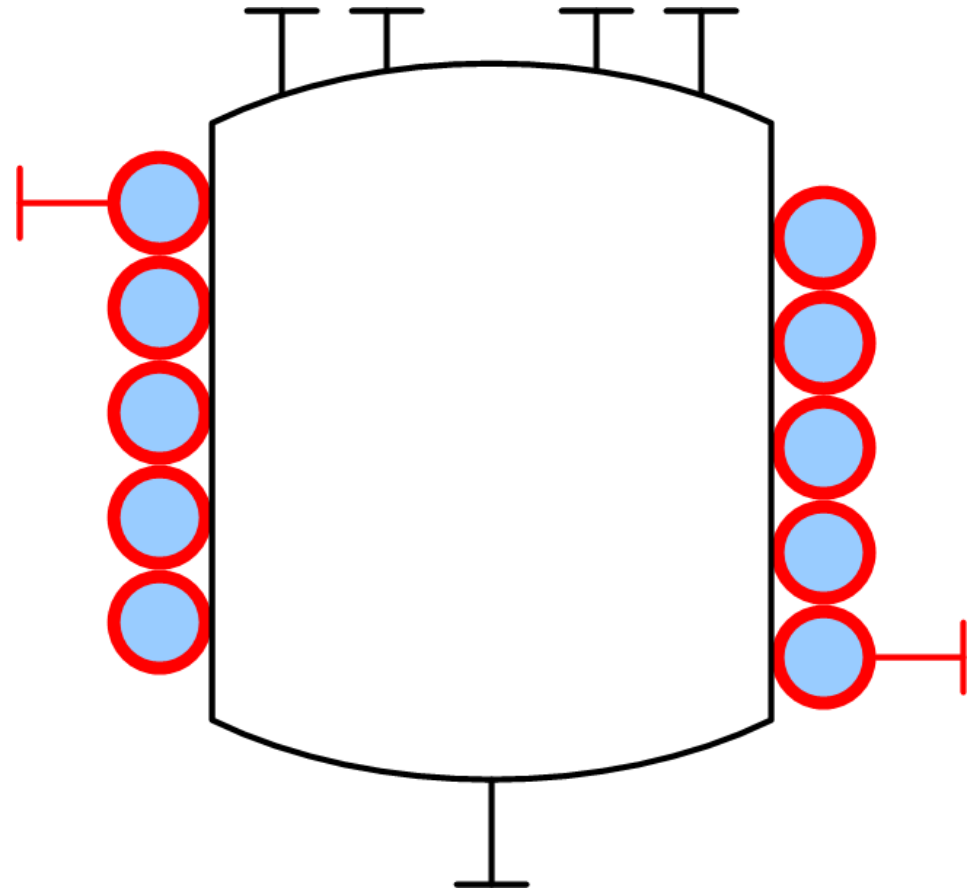
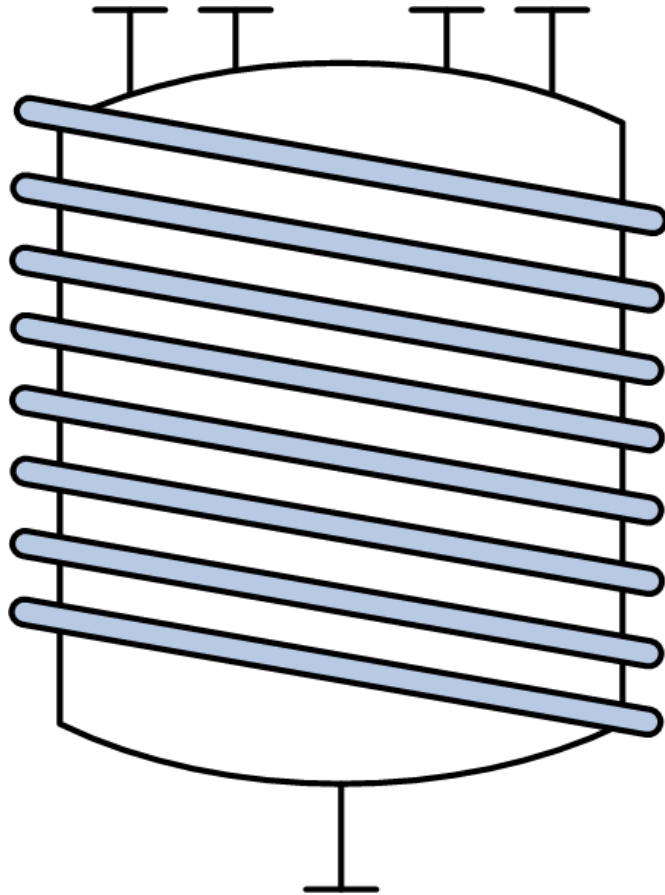
- 1 High Temperature Lead Wires (16 AWG)
- 2 Protective Metal Jacket
- 3 Parallel Circuit High Temperature Alloy Heating Element
- 4 Heat-Laminated, High Temperature Silicone Rubber Insulation



- Heat Duty In Watts Per Foot For Cable Or Watts Per Square Inch For Panels
- Self-Regulating Feature Available
- For Offsite Location, Electricity May Be More Available Than Other Energy Sources
- Remote Monitoring And Control Possible

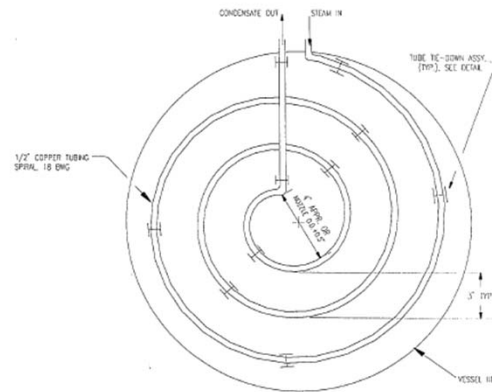
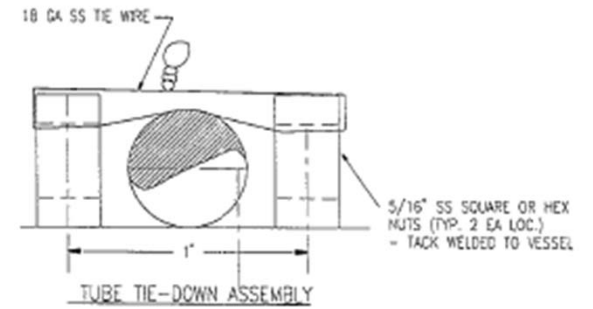
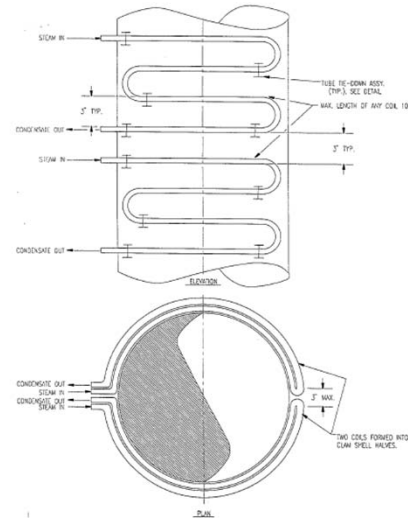
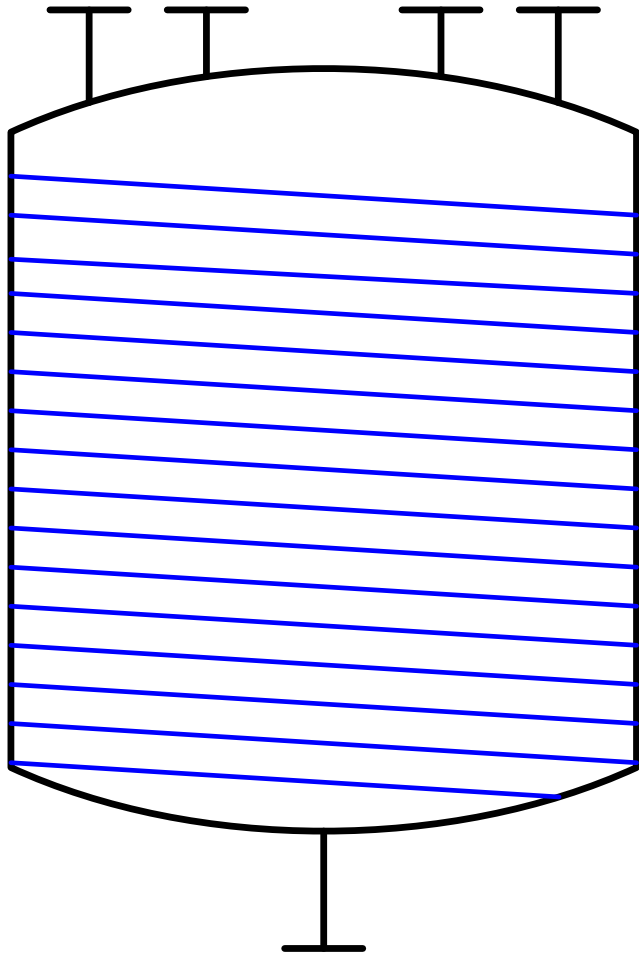


External - Pipe Tracer



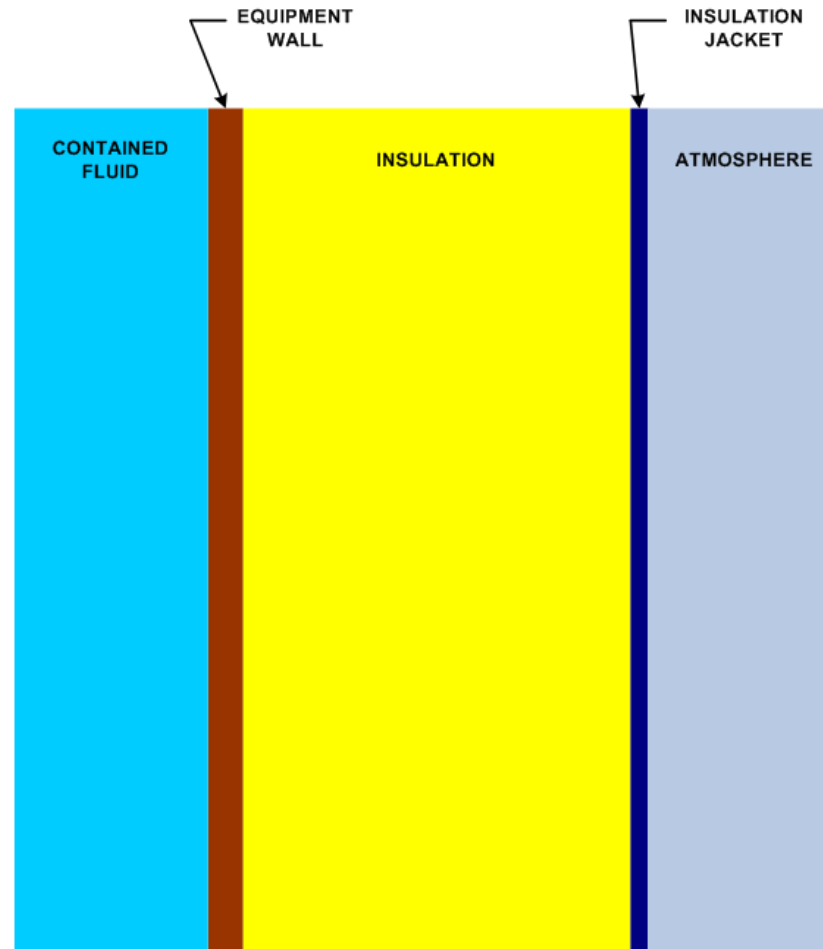


External - Tubing Tracer



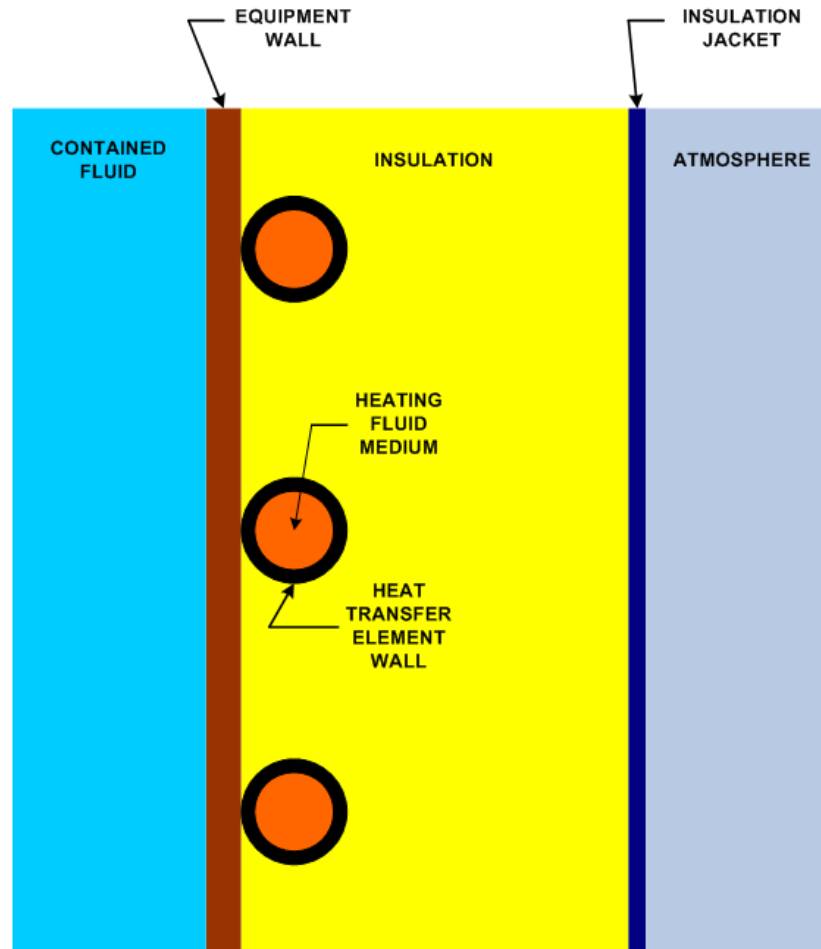


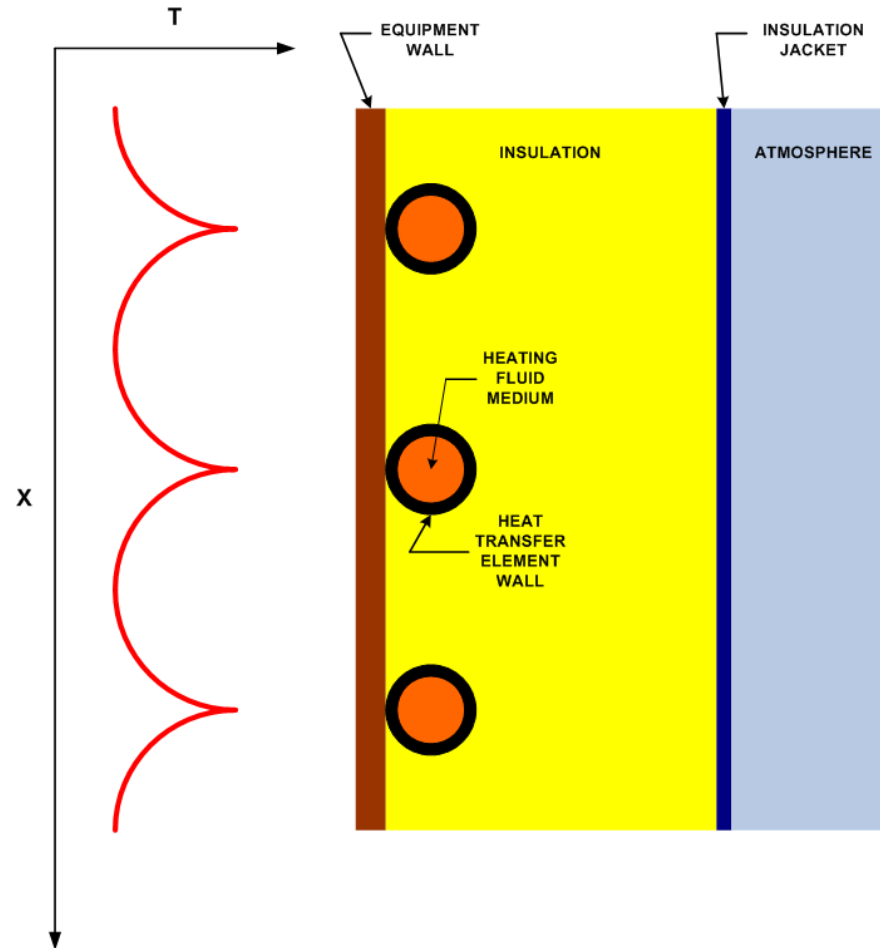
- Tubing Is Easier To Bend To Follow Equipment Contours Particularly Heads and Nozzles
- Selection of Pitch (Distance Between Runs) Is Critical To Ensure Wall Temperature Stays Above **Minimum Maintain Temperature**
- Design Of Tubing Heat Tracing Is Typically The Engineering Contractor Responsibility

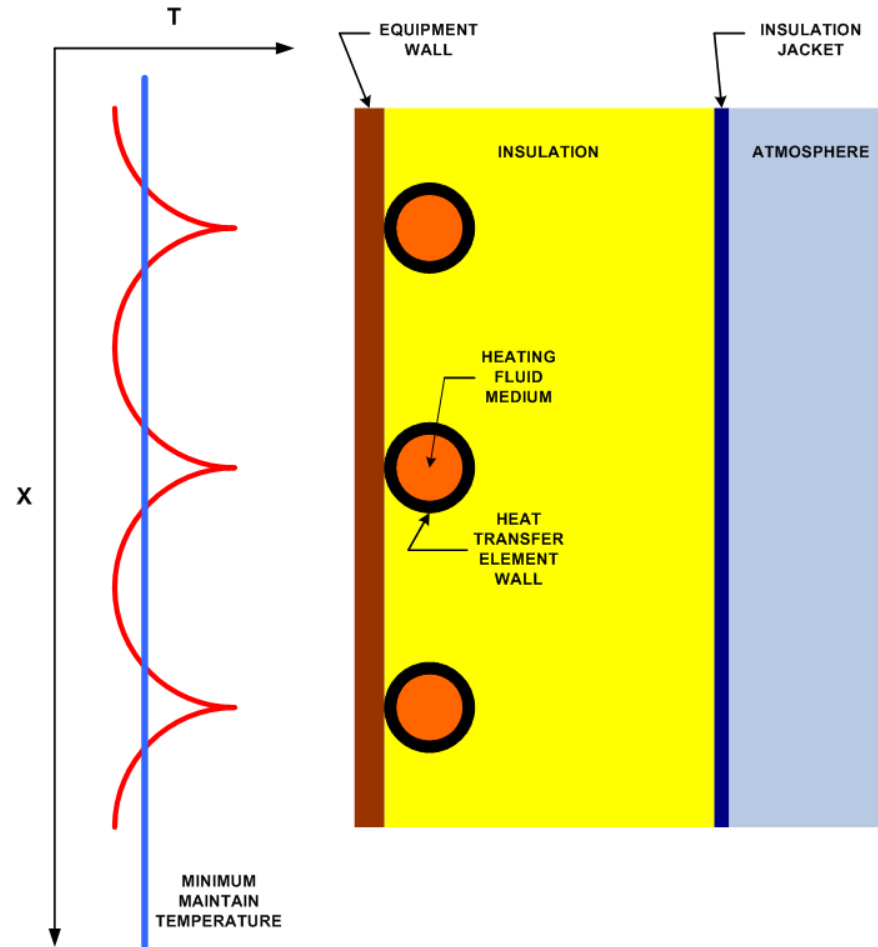


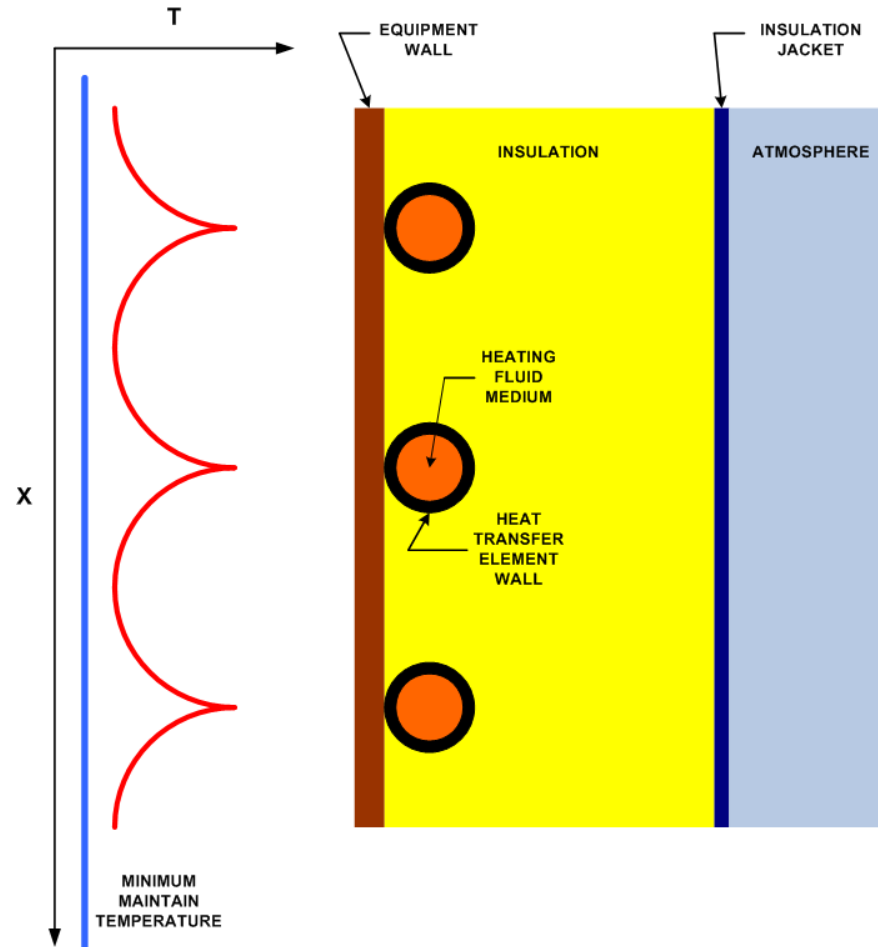


Pipe / Tubing Tracers



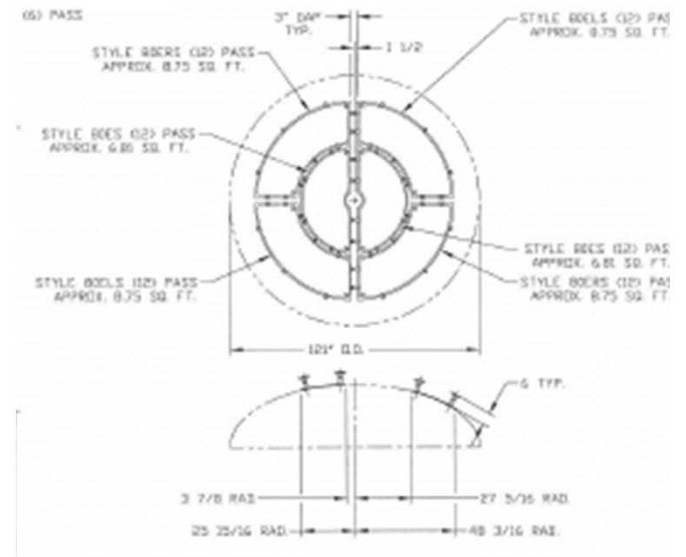
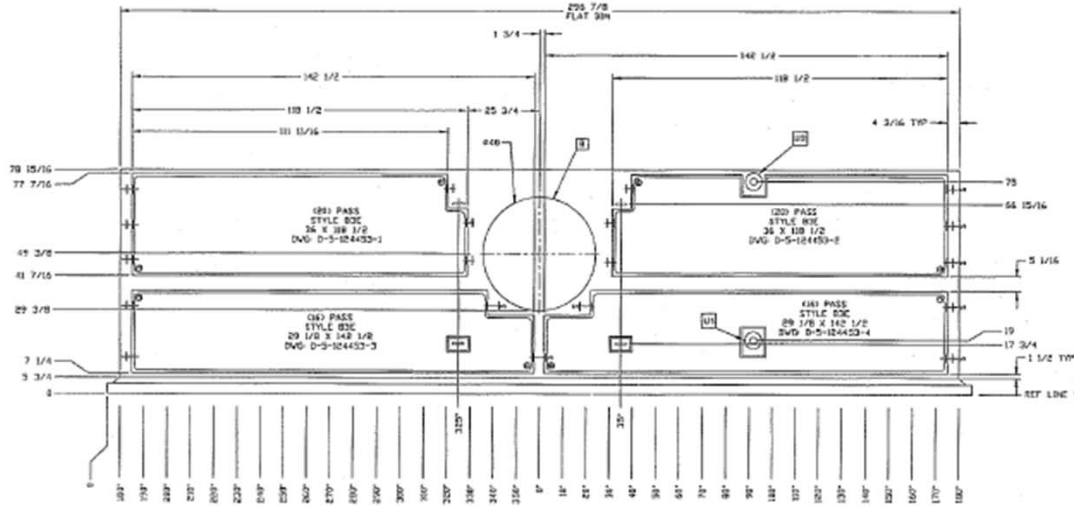






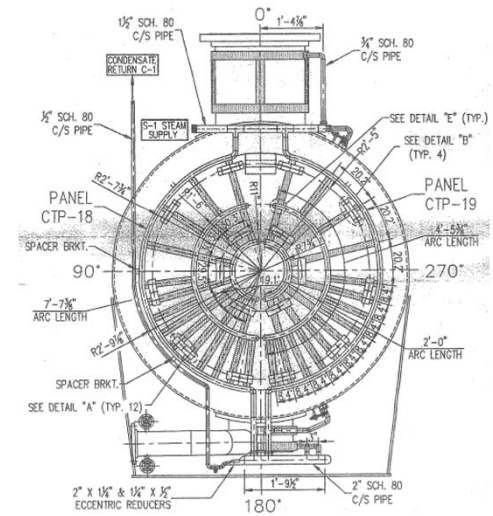
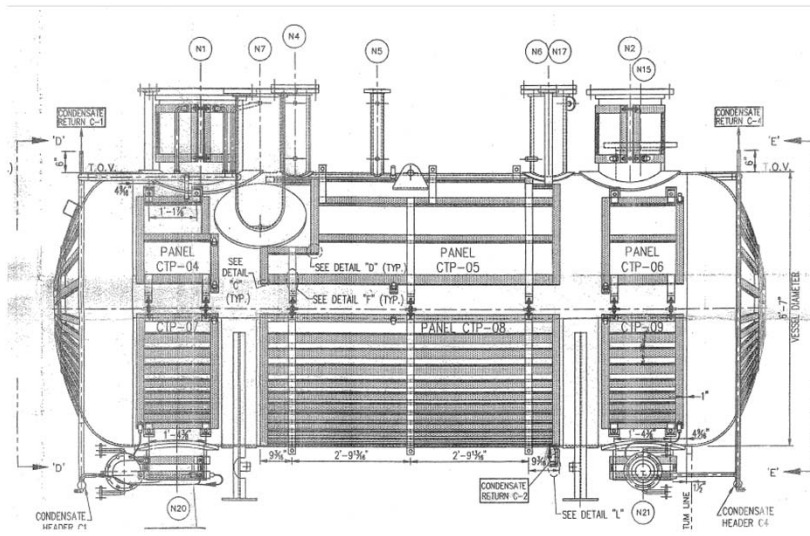


Tranter





External - ControTrace





Clamp-On Jacket





- Manufactured Assembly Takes Less Labor To Install Than Pipe Or Tubing Tracers
- Tubing Tracer Installed At Fabricator May Be Damaged During Shipping – Coil Assembly Is Typically More Rugged Design
- Heat Transfer Design Is Typically Coil Assembly Vendor Responsibility



- **Understand Process Objective:**
 - Temperature Maintenance
 - Process Heat Transfer
- **Selection Of Heat Transfer Components For Equipment Should Be Based On:**
 - Level Of Heat Transfer Requirement
 - Process Considerations
 - Cost