

# Feeding CO<sub>2</sub> from air into solid oxide electrolyzer cells

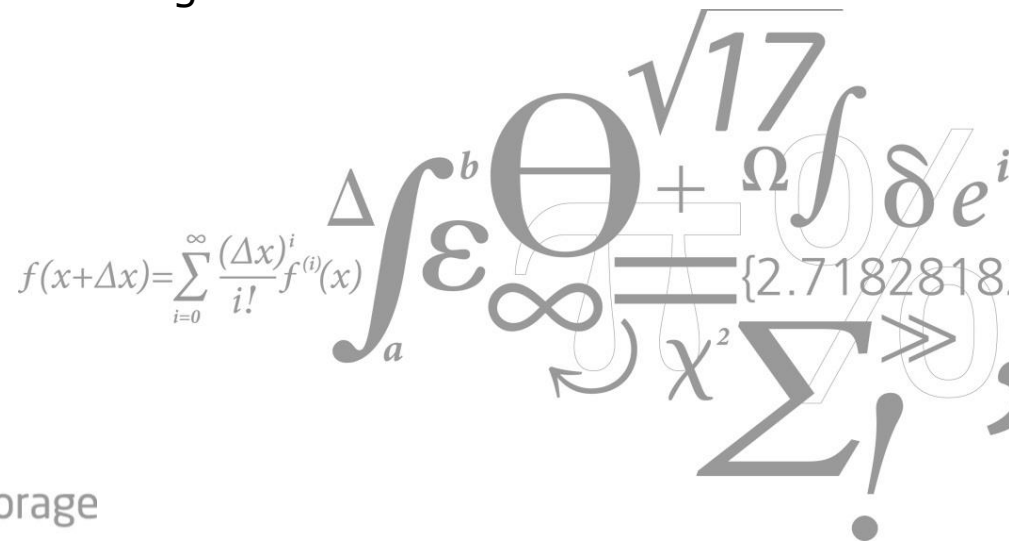
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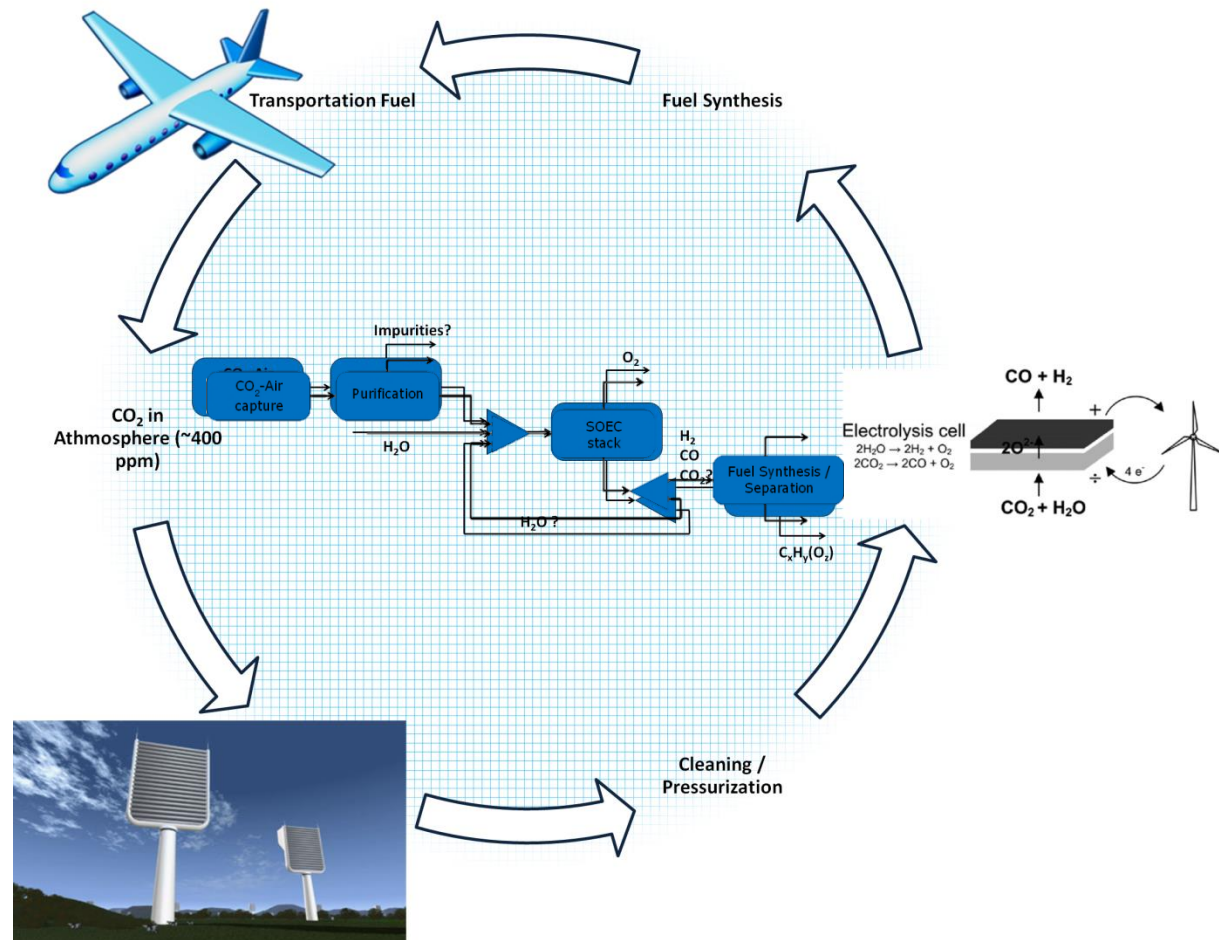


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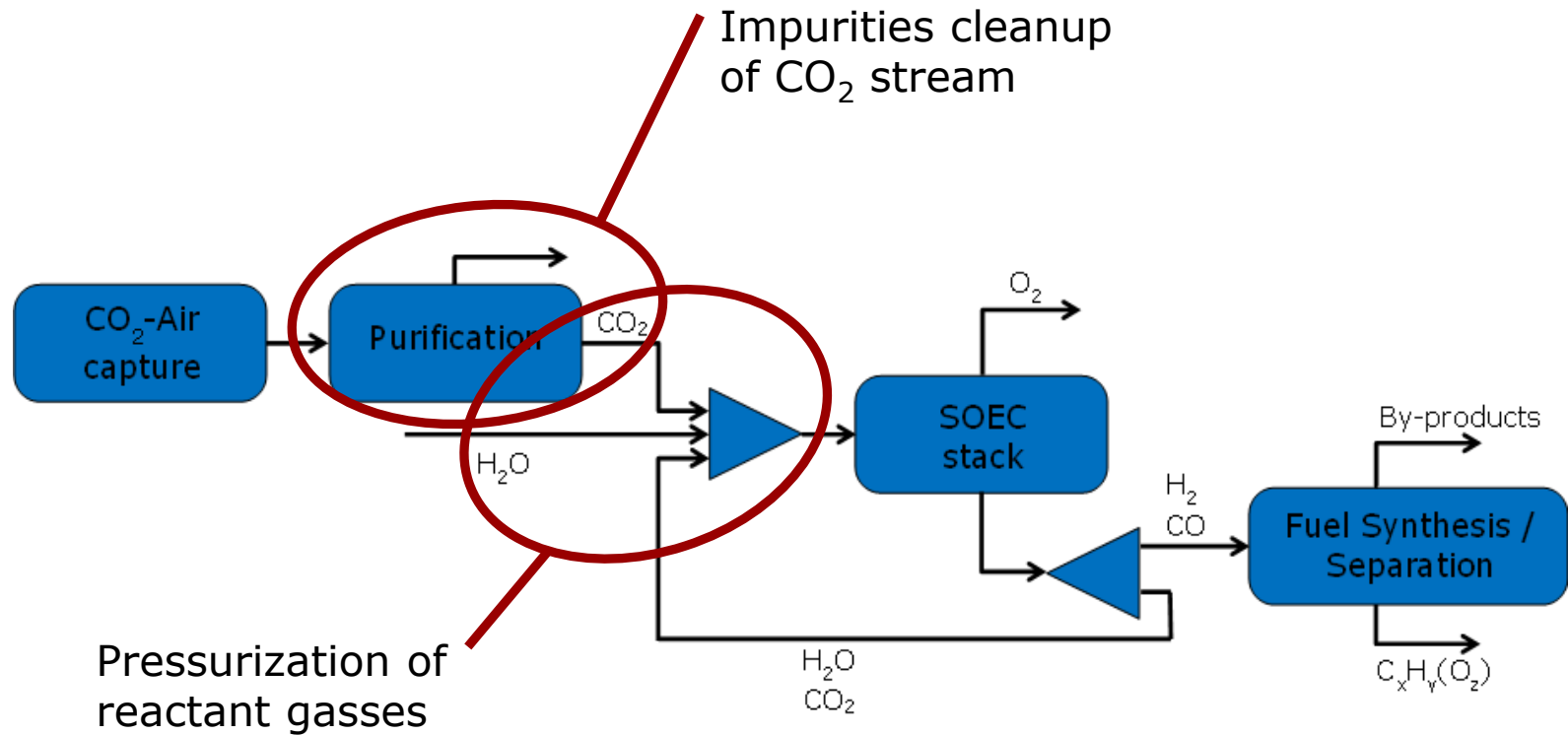
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# Project vision

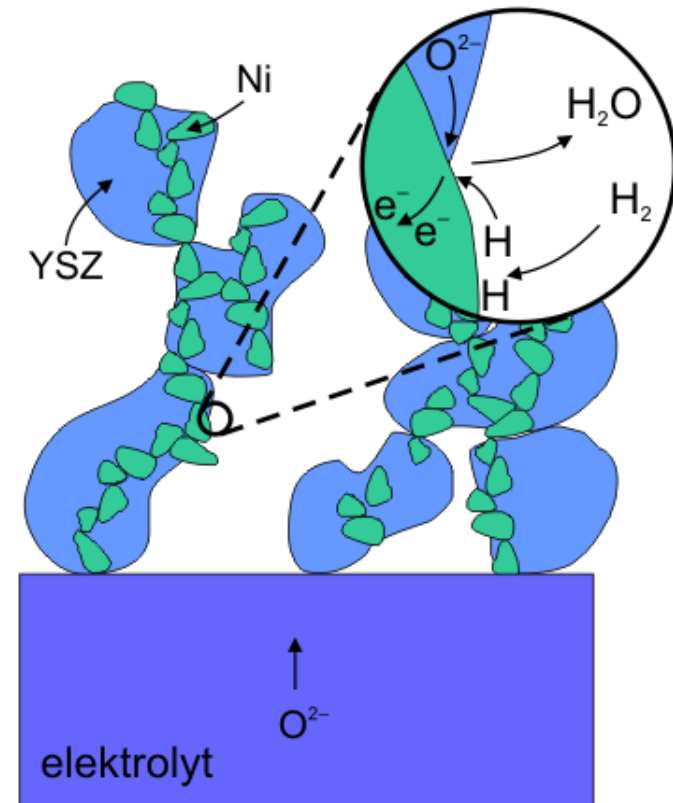
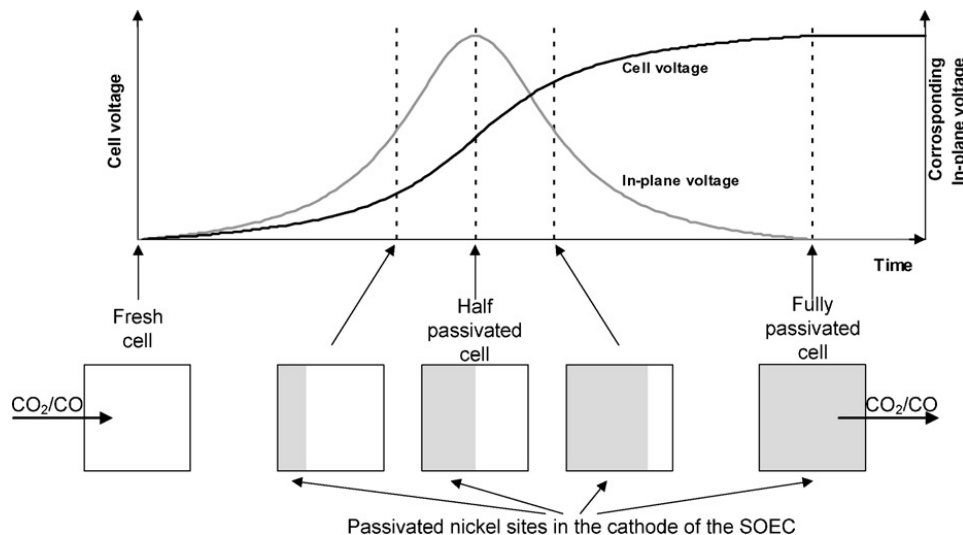


# Project vision



# Impurities and SOEC operation

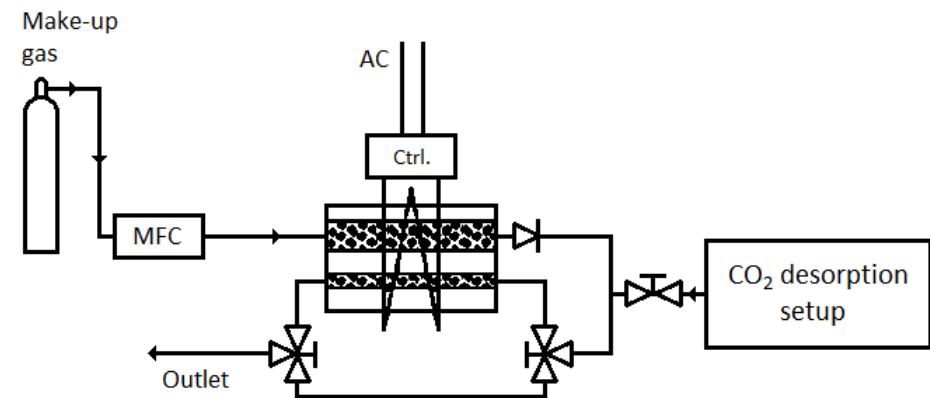
- Glassy Na, Si, Al, etc. Blocks catalytically active sites (TPB)
- Sulfurous compounds etc. block Ni surface sites
- Deposition damages structural integrity (carbon formation)
- Measurable below 5 ppb ( $H_2S$ )



Ebbesen SD, Mogensen M, Journal of Power Sources 193 (2009) 349–358

# Impurity collection experiments

- Solid state adsorption of trace impurities
- Crushed cathode material (Ni/YSZ)
- Operated at 1023 K
- Reducing conditions



## Climeworks Ltd.:

- functionalized amine based
- temperature-vacuum swing
- pre-pilot prototype
- ~99% CO<sub>2</sub> (N<sub>2</sub>, O<sub>2</sub>, H<sub>2</sub>O)

## Lenfest Centre for Sustainable Energy:

- an-ion exchange resin based
- carbonate-bicarbonate humidity swing
- simple bench scale setup
- 0.5~5 % CO<sub>2</sub> (N<sub>2</sub>, H<sub>2</sub>O, H<sub>2</sub>)

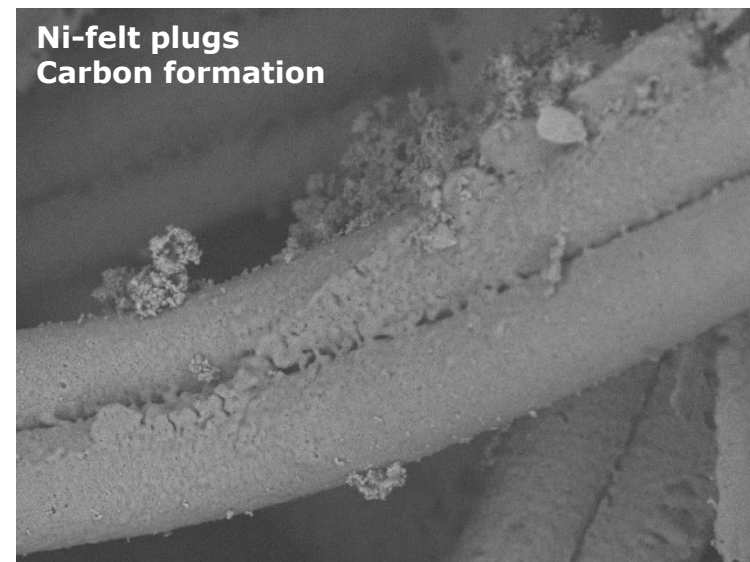
# Correction: revised numbers in table

## Elemental analysis of impurities

- Sorption on Ni/YSZ granulate (fuel electrode material)
- Operated at 1123 K
- Elemental analysis by XPS, EDS, SEM and Glow Discharge Mass Spectrometry (GDMS)
- Detection limit:  $\sim 10 \pm 2$  ppb (in gas)

Element	Content in CO <sub>2</sub> [ppm molar]	
	LCSE	Climeworks
B	-6.9 ± 9.7	-8.0 ± 17.3
Na	-13.6 ± 4.6	-10.1 ± 10.7
Mg	5.6 ± 8.2	0.0 ± 8.7
Al	-8.3 ± 13.3	0.5 ± 9.1
Si	4.1 ± 6.5	1.5 ± 9.5
P	-0.1 ± 0.1	-0.1 ± 0.1
S	1.2 ± 0.2	-0.2 ± 0.1
Cl	3.4 ± 1.3	3.6 ± 4.9
Co	1.6 ± 6.9	3.8 ± 11

GDMS elemental analysis



Ni-felt-U-0004

2013-10-17

N

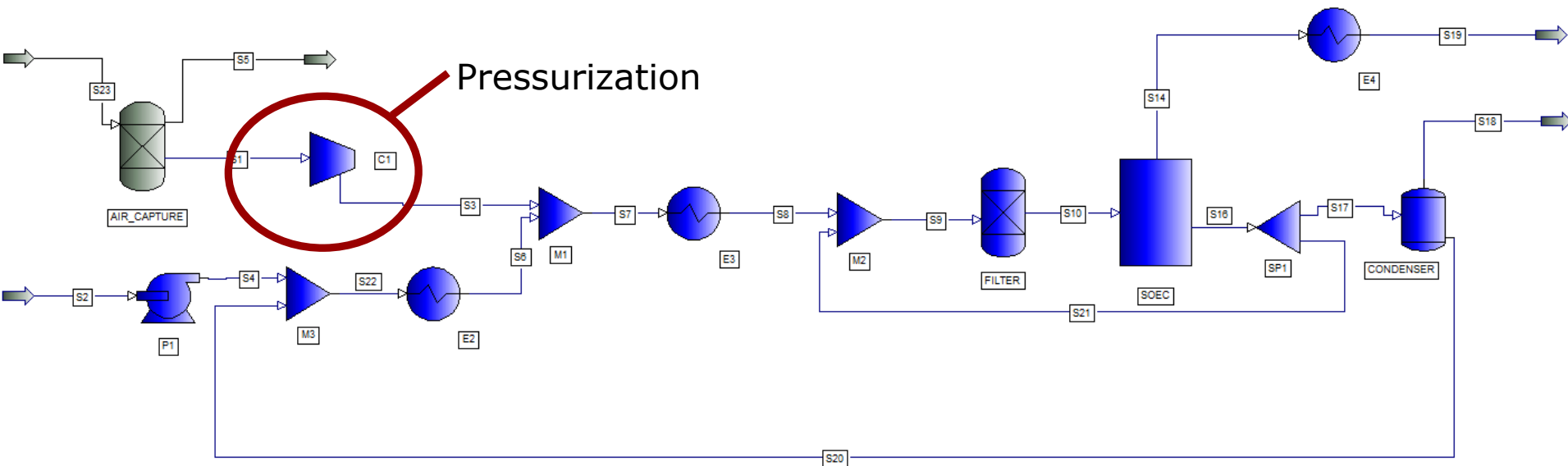
D4,2 x1,2k 50 um

# Elemental analysis: Glow Discharge Mass Spectrometry

- Various trace elements present in low concentrations
- Many are expected to be harmful for high purity applications (÷ carbon)
- Expected impurity sources:
  - Machine parts
  - Sorbent and filter material contaminants
  - Adhesives/oils
  - Captured from air (difference in location?)
- Most of these are preventable (minimize) in real systems
- Cheap and reliable filtering strategies available and tested
  - Ni/YSZ filter required for S-content <8 ton/1000 ton CO<sub>2</sub>
  - Easily regenerated by redox-cycling

# Compression: System simulation

- Steady state, thermodynamic model
- 1000 ton of CO<sub>2</sub> per year Climeworks Ltd. plant ~ 530 kW SOEC
- Starting conditions: CO<sub>2</sub> in air, clean H<sub>2</sub>O, ambient conditions
- SOEC operating conditions: 1123 K, 50 atm, 1.24 V (> thermo neutral)
- Syngas H<sub>2</sub>/(CO+CO<sub>2</sub>) = 3 ~ methane production (~12% CH<sub>4</sub>)
- Outlet conditions: syngas stream at 400 K and 50 atm.

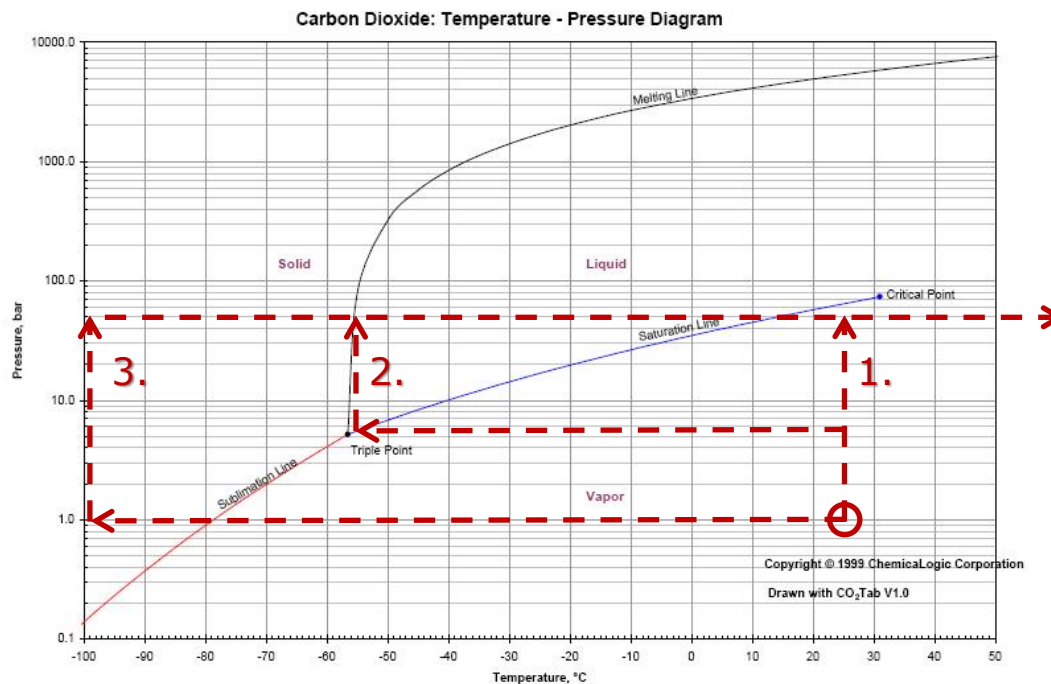




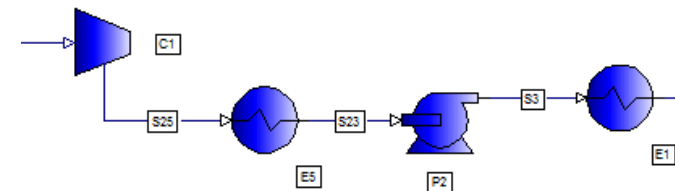
# Compression cases

1. Base case: Simple compressor
2. Cryo: Cryogenic compression (5.15 atm, 205 K)
3. Solid Cryo: Cryogenic via solid CO<sub>2</sub> (1 atm, 187 K)

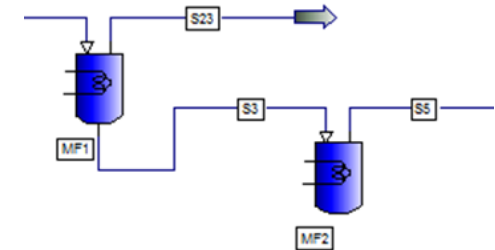
Inlet: ambient, outlet: 50atm, 533 K



2.

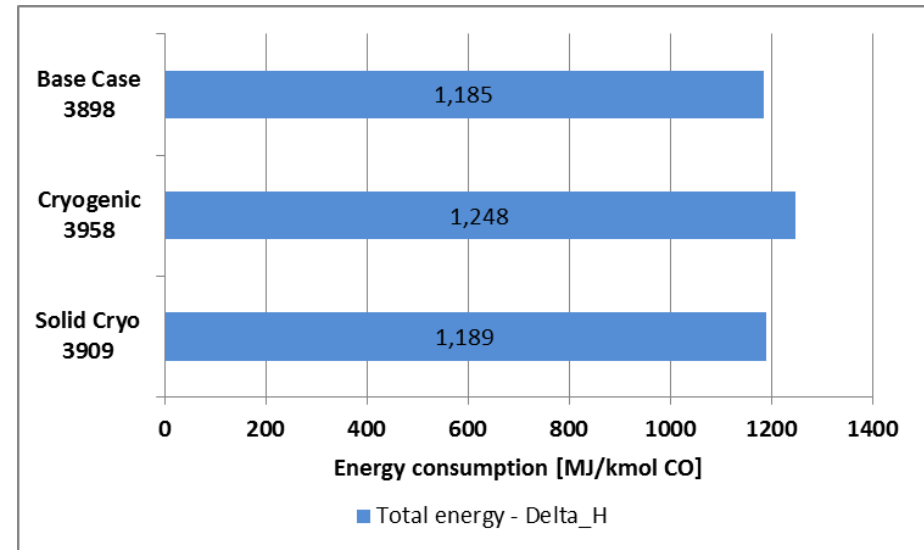
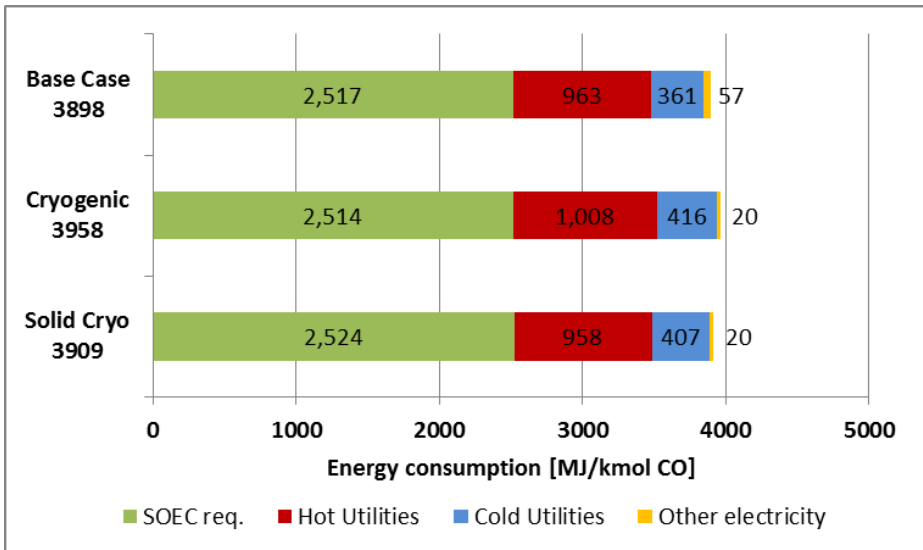


3.



# Energy balance

- Energy consumption based on production of CO
  - 1 mol CO
  - ~6 mol H<sub>2</sub>
  - 1 mol CH<sub>4</sub>
  - H<sub>2</sub> : (CO+CO<sub>2</sub>) = 3 : 1
- Heat integration pinch analysis:



## Conclusion and future work

- Impurities pose a minor problem for SOEC operation and will probably require filtering
- Careful selection of materials will solve some of the problem
- Cheap, efficient filtering strategies exist to take care of the rest
  
- Alternatives to simple compression of CO<sub>2</sub> exists
- Further heat integration analysis, sizing and costing is needed to evaluate these
  
- Sorbent based compression is being looked into
- Further system analysis is planned
  - Including matching to various fuel synthesis technologies

# Acknowledgements

- Eurostars E! CAPFUEL - CO<sub>2</sub> capture from air and conversion into hydrocarbon fuels



- Climeworks Ltd.:
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