



Mass Transfer Rate Modeling Basics

Nathan A. Hatcher, P.E.

AIChE South Texas Section Dinner

Pellazio Banquet Hall, Houston TX

September 11, 2014



Outline

- History of Process Simulation
- Briefly about the ProTreat® Simulator
- Characteristics of True Mass Transfer Rate Based Models
- The Ideal Stage
- Elements in a Rate Model



Background

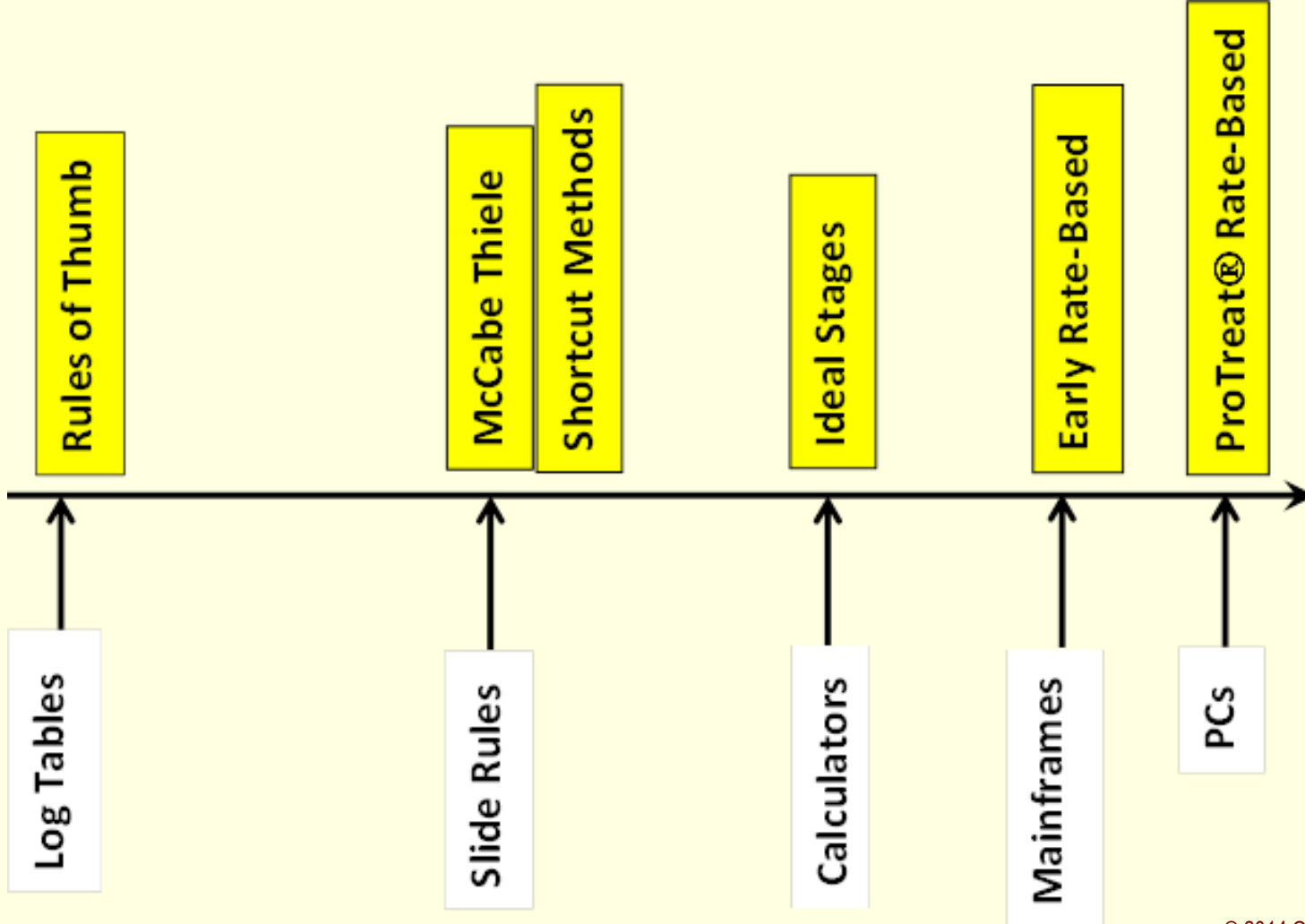
- Survey.....
- Process simulations are:
 - Physical and chemical mathematical models for processes taking place in process equipment
- Equations are either:
 - Empirical or Physically based

Brute force curve fits

Chemistry
Material & Energy balances
Vapor Liquid Equilibrium (VLE)
Mass & Heat Transport



Process Simulation Paleontology





Process Simulation

- Advantages over Hand Calculations
 - Speed of Computation
 - More Realistic Models
 - Better represent reality
 - Predictive and more confident extrapolation
- Match the Model to Needs



About ProTreat®

Mid 60s to Mid 80s	Dr. Ralph Weiland's university research on mass transfer rate modeling for mainframe computers (supported by Dow Chemical) led to the development of mass transfer rate models of AspenTech and SimSci
Late 80s	Engineering computations migrate from mainframes to PCs with Microsoft's launch of Windows®
1992	OGT, Inc. founded by Weiland & Dingman specifically to develop a rate-based simulator for Windows
2003	Commercial introduction of ProTreat®

What can *ProTreat*® simulate?

- All amines plus 2- & 3-amine blends
- Physical solvents: DMPEG, MEG, DEG, TEG
- Specialty solvents
- Hydrocarbon, BTEX solubility
- Rate-based mercaptans, HCN, Phenol
- Heat Stable Salts (ionic contaminants)
- Ammonia & Sour Water Stripping
- Caustic treating with NaOH and KOH
- H₂S / CO₂ corrosion in amine and sour water



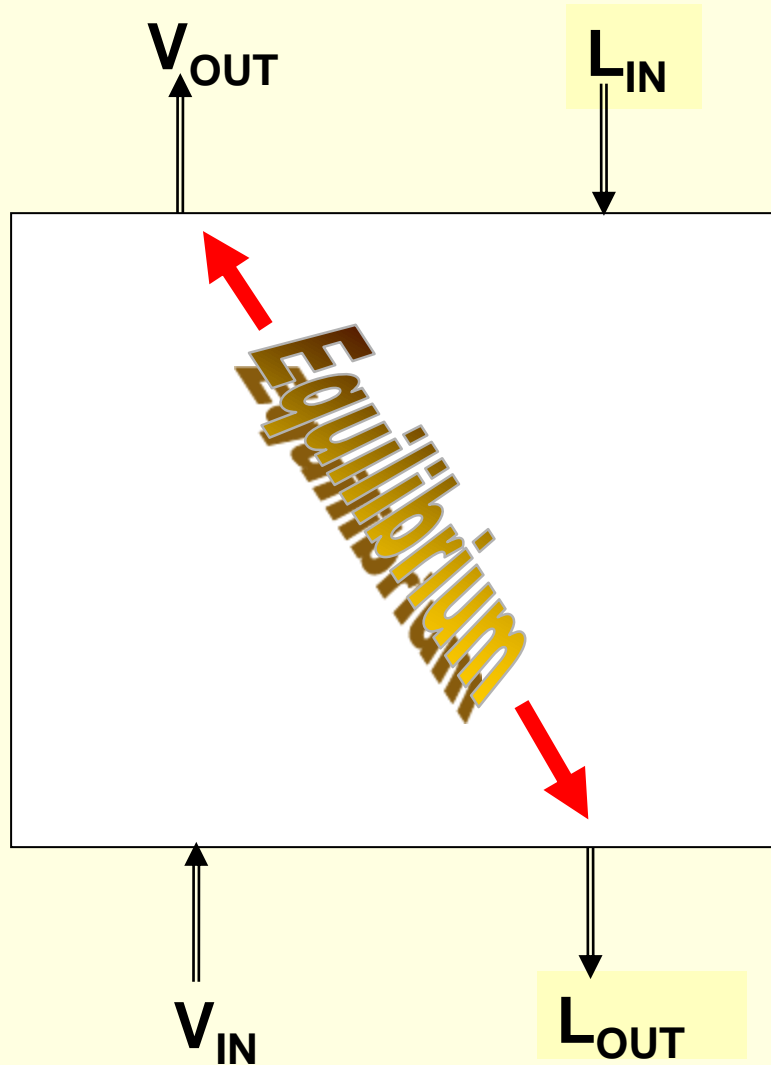


True MTR Distillation

- **Directly calculates tray-by-tray & packed segment-by-segment performance**
- **No translation from ideal stages to real tower internals**
- **Real trays, random packing, structured packing — hydraulics & mass transfer**
- **Chemical reactions modeled and accounted for enhancement to mass transfer**
- **Flows/T/P/Composition impact separation through mass transfer as well as VLE**

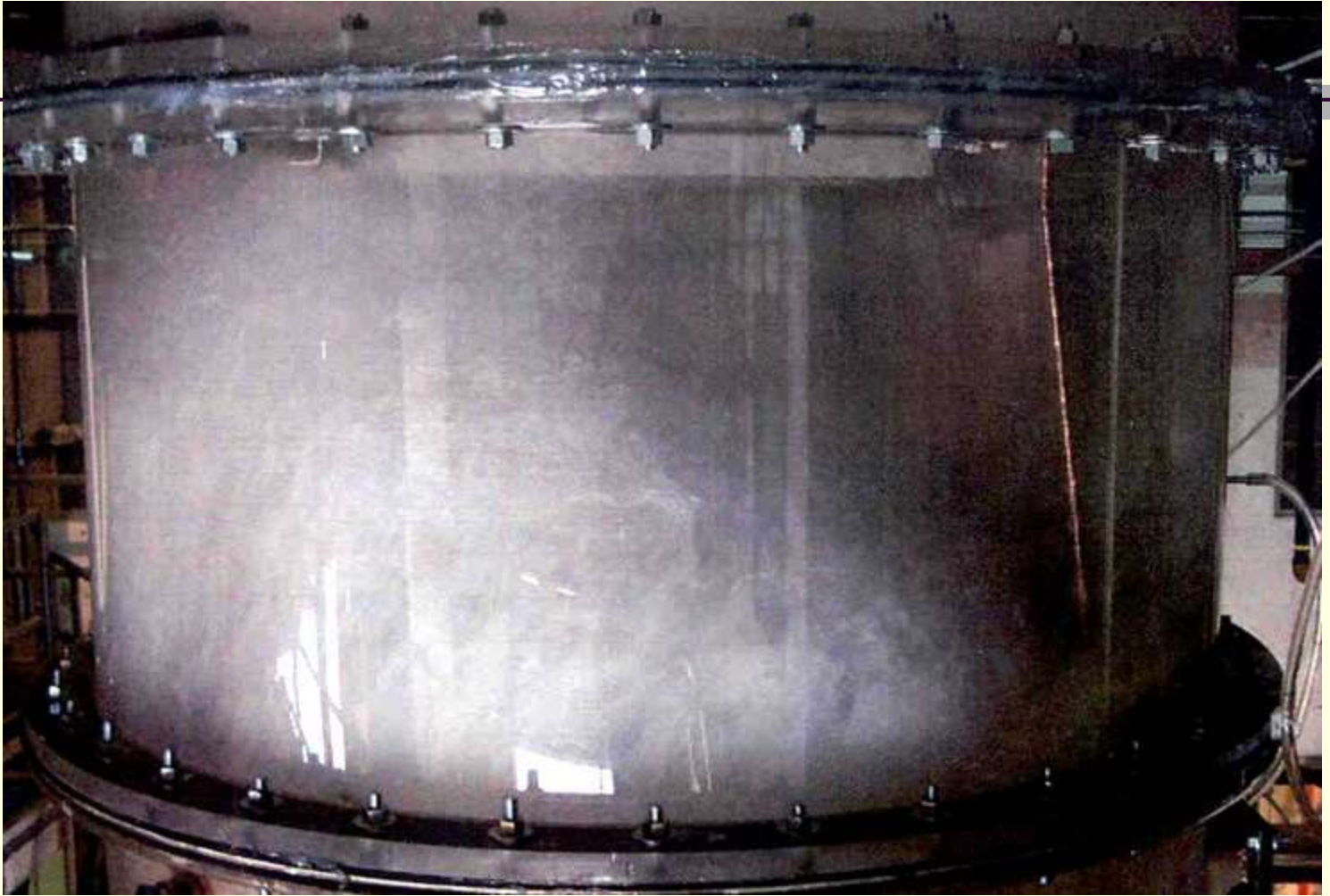


The Ideal Stage





Low Gas Flow



Medium Gas Flow



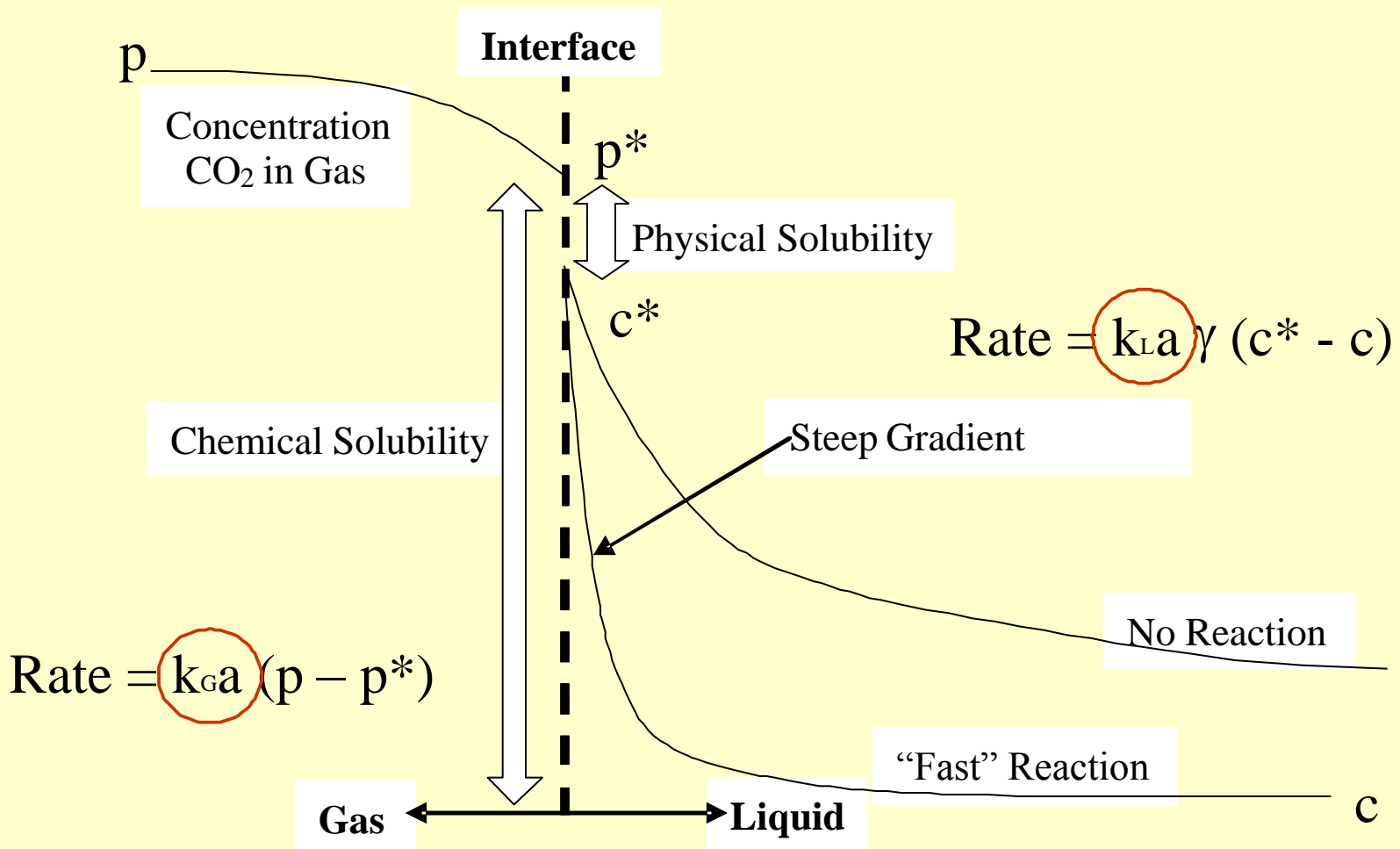
High Gas Flow



Onset of Flood in Structured Packing

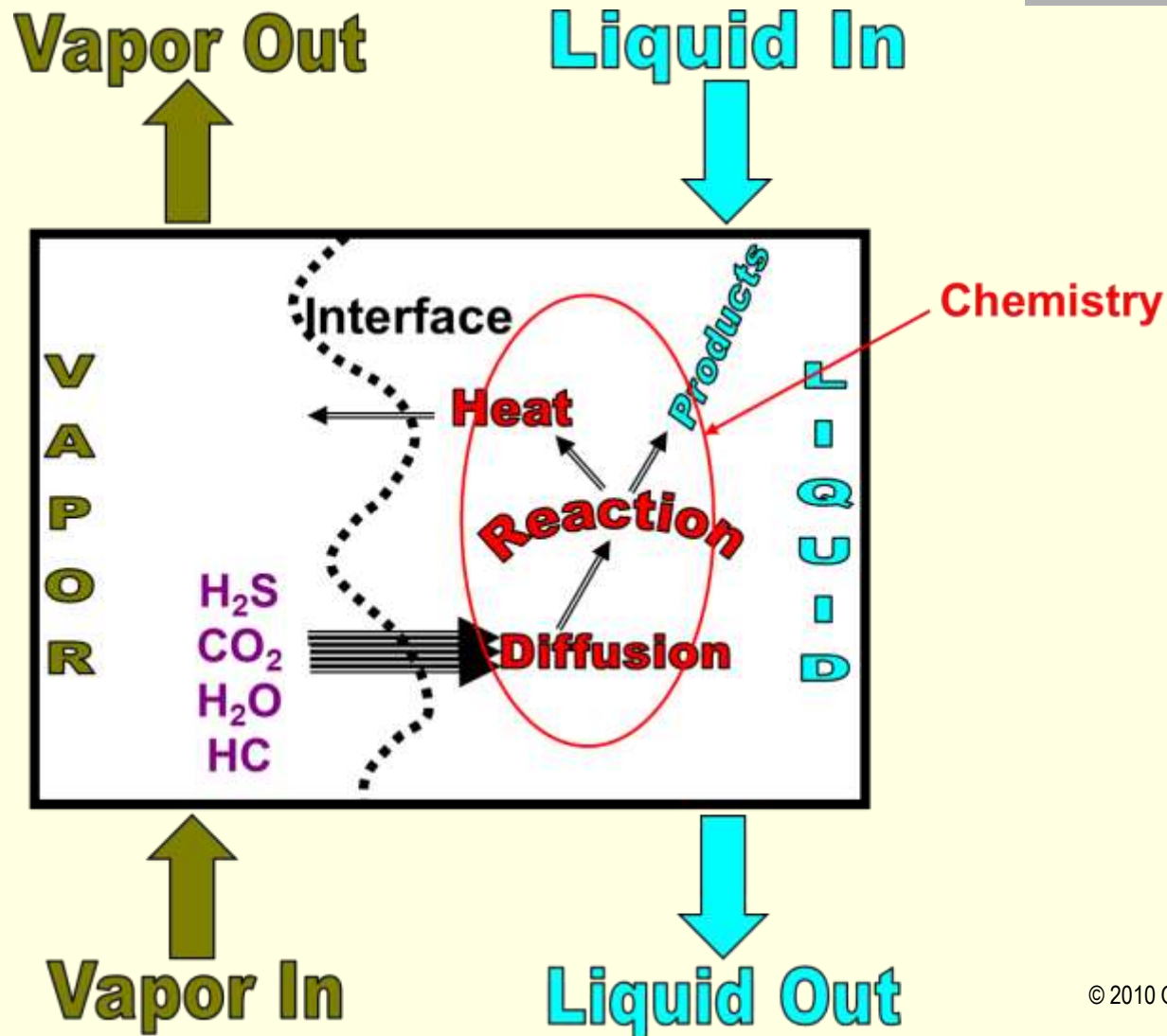


Mass Transfer – Gas Absorption





MTR Segment



Transfer Rate to Liquid From Interface

Mass transfer coefficient

- Depends on equipment
- Fluid properties
- Hydraulics

Free Acid Gas Concentration at Interface

- Henry's Law

Free Acid Gas Concentration in bulk liquid

- VLE

$$N_L = E k_L^o a (y^{Interface} - y^{Bulk})$$

Enhancement Factor

- Accounts for reaction with diffusion
- Depends on kinetics

Interfacial Area

- Depends on equipment hydraulics



Mass Transfer Rate

Depends on...

- Area available for mass/heat transfer
- Phase resistances
 - Gas & liquid loads
 - Hydraulics (specific tower internals)
 - Physical properties (density, viscosity, diffusion)
- Driving force (extent that phases are **not** in equilibrium)



Mass Transfer Rate

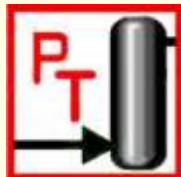
Results...

- Learn how much CO₂ and H₂S are actually removed on each individual REAL tray and in each segment of REAL packing
- You are not asked for
 - Number of theoretical stages
 - Liquid holdup per theoretical stage
 - Tray efficiency or packing HETP
- You are asked for
 - Tray details (as per tray drawings)
 - Column details (as per PFDs)
 - Packing type & size by Vendor designations (as per PFDs)

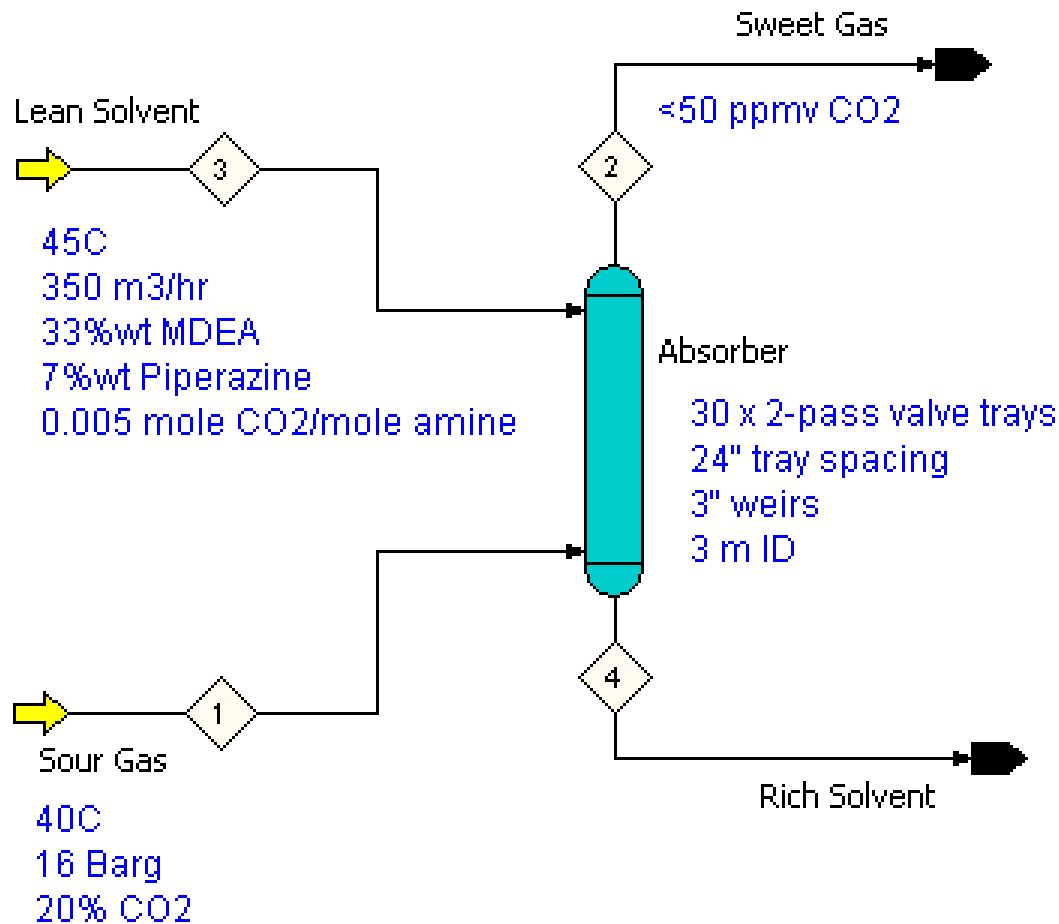


Phase Equilibrium

- Just as important as in ideal stage models
- But not the whole story
- If the VLE is wrong, the rate model will follow suit



Case Study



Ideal Stage “Tuning”

Match CO₂ performance at 350 m³/hr solvent

Ideal Stages	CO ₂ Out, ppmv
3	745
4	1.14
5	0.150
6	0.146

← Closest representation

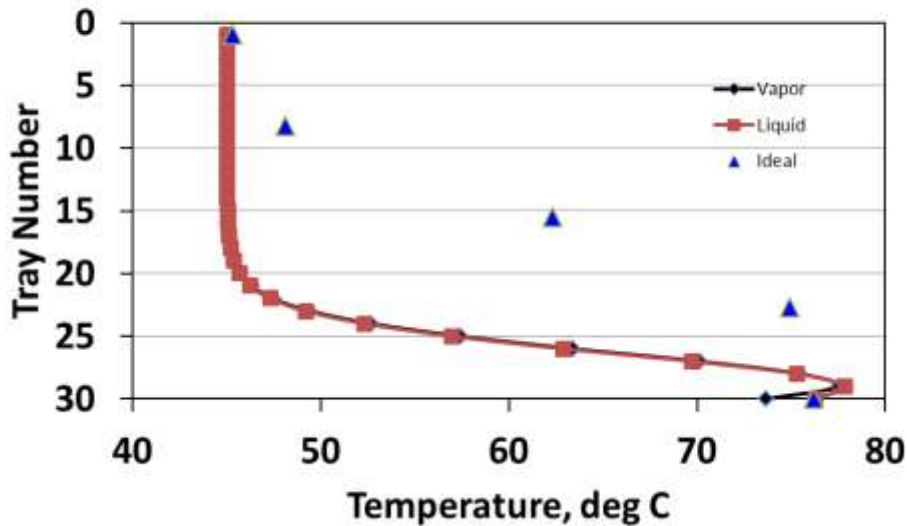
ProTreat Rate Model Outlet CO₂: 0.156 ppmv



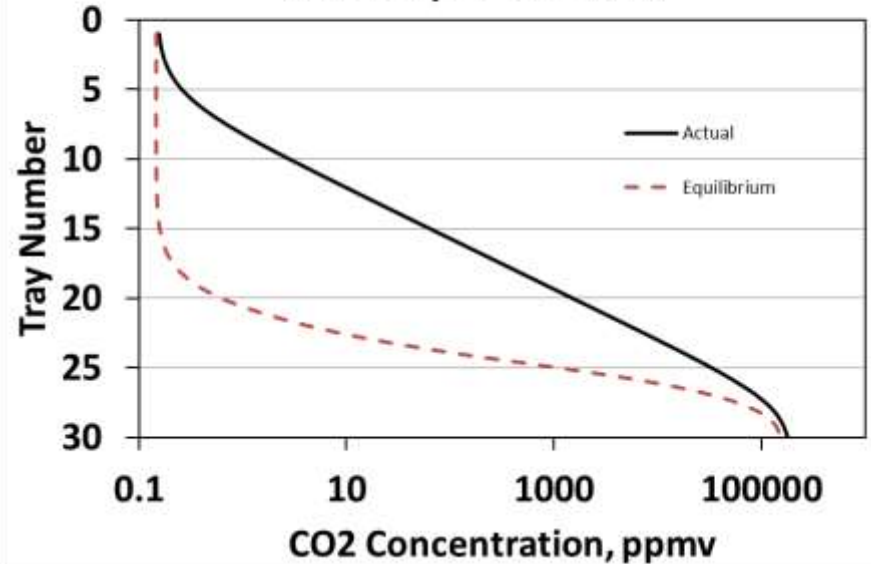
Column Profiles

350 m³/hr Solvent Rate

LNG Absorber Temperature Profile
350 m³/hr Solvent



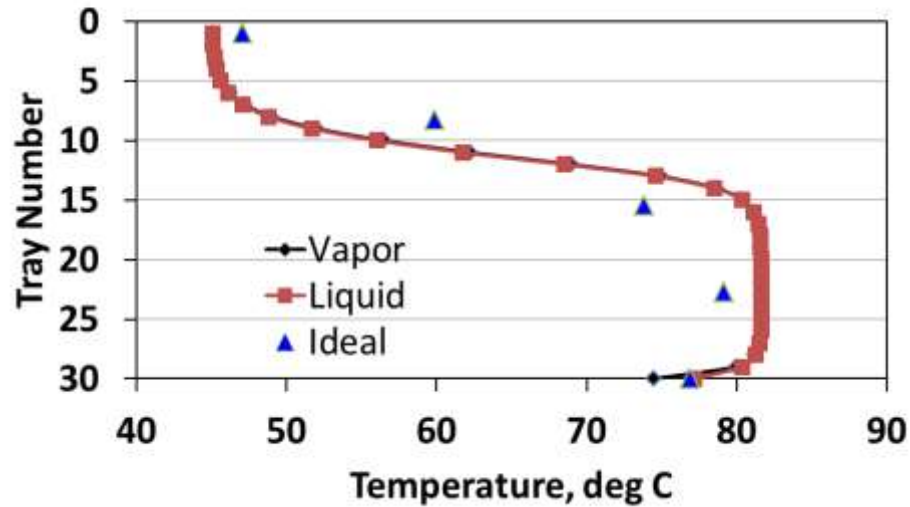
LNG Absorber CO₂ Profile in Vapor
350 m³/hr Solvent



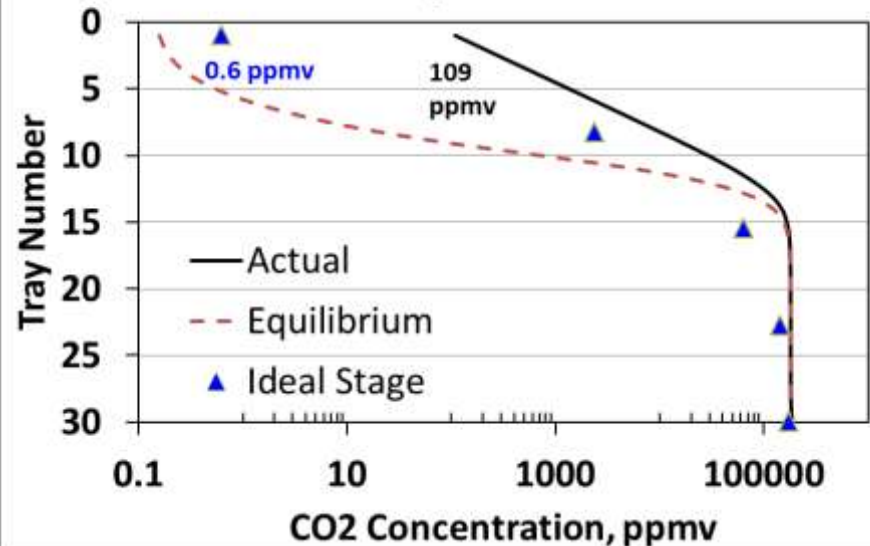
Column Profiles

340 m³/hr Solvent Rate

Temperature Profile
340 m³/hr Solvent



CO₂ Profile in Vapor
340 m³/hr Solvent



Mass Transfer Rate Models

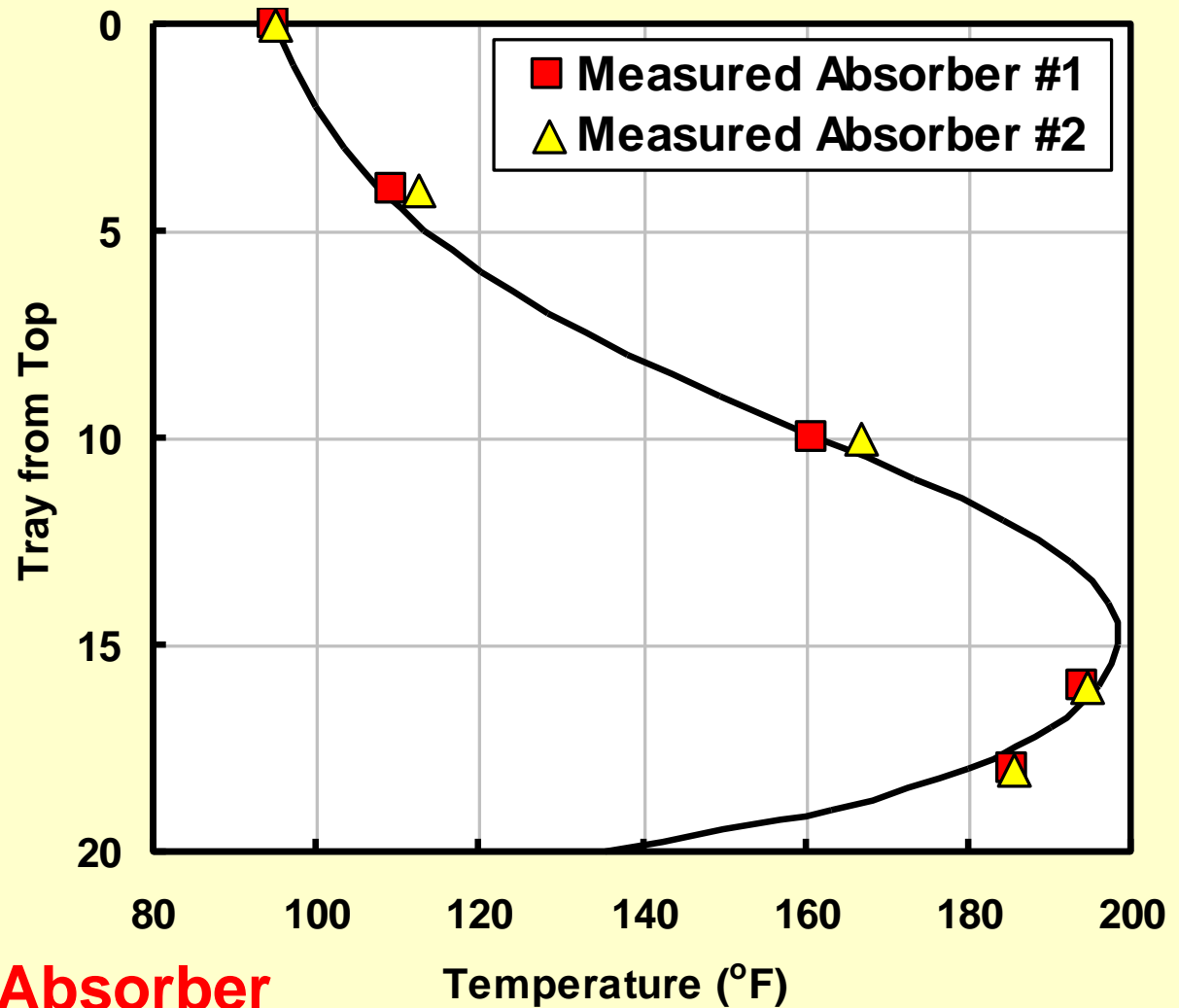
- Answers don't depend on how well you can play the “guess the efficiencies” and “guess a residence time” game. They depend on what the tower internals can really do!
- A mass transfer rate model sets up a **virtual plant** based on REAL WORLD REALITY and sound engineering science
- You don't pick parameter values to match the data — the simulation matches good data or you go looking for what's wrong with the plant



Why a Rate Model?

- Predictive
 - Tower internals do matter, packing characteristics (type, size, structured, random, etc.) enter directly into calculations
- Highly reliable for selective gas treating
 - Selectivity is a competition between CO₂ and H₂S absorption rates.
- Works correctly with mixed amines
 - Mixed amine performance depends on altering mass transfer rates, and **mass transfer rates are the very basis of a rate model**





Gas Treating Absorber Temperature Profile

Summary

- Directly tied to internals type, detail, & operating conditions via hydraulics & quality of contact
- Separation depends on physical & transport properties (c_p , μ , σ , ρ) — so does the rate model
- A truly predictive tool—needs no operating experience to get answers
- Relates to actual hardware
- Tells you what a plant *should* be doing





ProTreat[®]

Taking the
Guesswork
Out of Process
Simulation

